

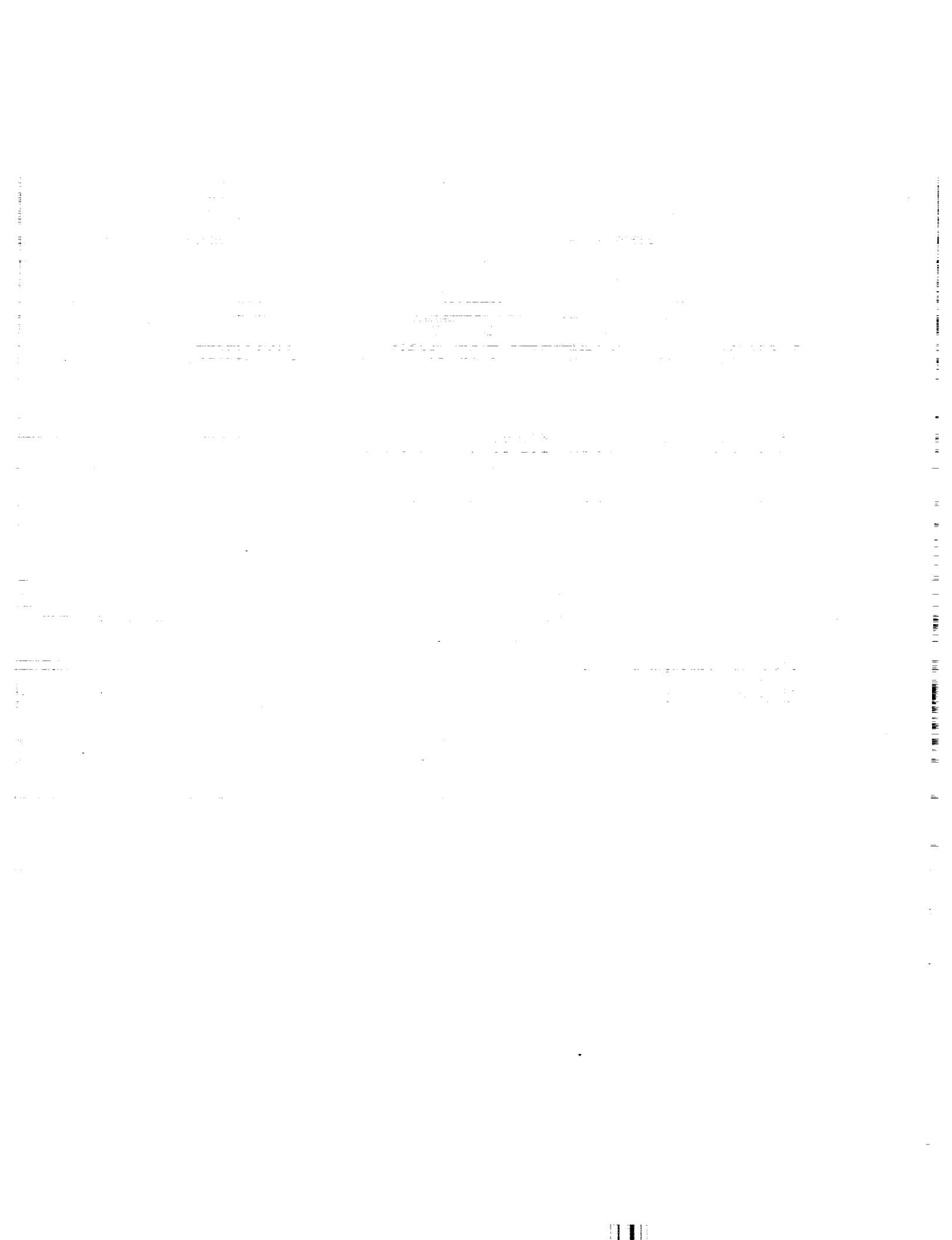
**Computer Program for Solving Laminar,  
Transitional, or Turbulent Compressible  
Boundary-Layer Equations for  
Two-Dimensional and Axisymmetric Flow**

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#### SUMMARY

A numerical algorithm and computer program are presented for solving the laminar, transitional, or turbulent two-dimensional or axisymmetric compressible boundary-layer equations for perfect-gas flows. The governing equations are solved by an iterative three-point implicit finite-difference procedure. The software, program VGBLP, is a modification of the approach presented in NASA TR R-368 and NASA TM X-2458, respectively. The major modifications are: (1) replacement of the fourth-order Runge-Kutta integration technique with a finite-difference procedure for numerically solving the equations required to initiate the parabolic marching procedure; (2) introduction of the Blottner variable-grid scheme; (3) implementation of an iteration scheme allowing the coupled system of equations to be converged to a specified accuracy level; and (4) inclusion of an iteration scheme for variable-entropy calculations. These modifications to the approach presented in NASA TR R-368 and NASA TM X-2458 yield a software package with high computational efficiency and flexibility. Turbulence-closure options include either two-layer eddy-viscosity or mixing-length models. Eddy conductivity is modeled as a function of eddy viscosity through a static turbulent Prandtl number formulation. Several options are provided for specifying the static turbulent Prandtl number. The transitional boundary layer is treated through a streamwise intermittency function which modifies the turbulence-closure model. This model is based on the probability distribution of turbulent spots and ranges from zero to unity for laminar and turbulent flow, respectively. Several test cases are presented as guides for potential users of the software.

#### INTRODUCTION

A number of finite-difference and integral methods are currently available for numerically solving the two-dimensional, or axisymmetric, compressible boundary-layer equations. No attempt is made in the present paper to present a literature review of either solution techniques (ref. 1) or turbulence closure (ref. 2). Reference 2 includes a tabular summary of 34 additional two-dimensional programs available as of 1975. The purpose of the present paper is to present modifications of the algorithm and software presented in references 3 and 4 that render the approach more accurate, more efficient, and easier to implement.

In the present approach, a coupled, iterative implicit finite-difference procedure, similar in many respects to that presented in references 5 and 6 for laminar flows, is used to solve the system of equations for laminar, transitional, or turbulent boundary-layer flows. The major modifications presented in the present approach as compared with references 3 and 4 are as follows: (1) replacement of the fourth-order Runge-Kutta integration technique used in reference 4 with a finite-difference procedure for numerically solving the equations required to initiate the parabolic marching procedure; (2) introduction of the variable-grid scheme proposed by Blottner in reference 7; (3) implementation of an iteration scheme allowing the coupled system of equations to be converged to a specified accuracy level; and (4) implementation of an iteration scheme for variable-entropy calculations. For most applications, because of the quasilinearization technique, the iteration cycle for constant-entropy calculations can be omitted if a sufficiently fine grid distribution is chosen for the coordinate normal to the wall boundary. (See ref. 8.) The present program can be easily applied to any attached, compressible, perfect-gas (two-dimensional or axisymmetric),

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boundary-layer flow. Transverse-curvature terms are retained in the system of equations with the option of being neglected if the user so desires. The program is also structured to allow the user the option of obtaining locally similar solutions.

Options are provided for either two-layer eddy-viscosity or mixing-length turbulence-closure models. No attempt has been made to generalize the closure models to empirically include the effects of streamwise pressure gradient, wall curvature, wall roughness, wall mass transfer, and low Reynolds number. (See ref. 2.) The models are structured in subroutine TURBLNT such that the user can easily modify the formulation to best represent the specific type of flow under investigation. The static turbulent Prandtl number can be specified in one of three ways: (1) as a constant; (2) as an analytic function of the coordinate normal to the wall boundary; or (3) as tabular input from experimental data.

The transitional region of the boundary layer is modeled through the streamwise intermittency function (ref. 9), which modifies the turbulence-closure model. Boundary-layer transition location and the extent of the transition (length of transition region) can either be specified from experimental data or computed from empirical correlation equations. The laminar boundary-layer equations are recovered by equating the streamwise intermittency function to zero.

Five test cases are presented in the present paper. These cases cover external and internal flows, including flows with wall mass transfer, transverse-curvature, and variable-entropy effects. The cases are designed to serve as guides for assisting potential users as they become familiar with program VGBLP prior to applying the program to their specific problems.

SYMBOLS

A damping function,  $26v/u_T$

$A^+$  damping constant,  $Au_T/v$

$A_{1n}, B_{1n}, C_{1n}, D_{1n}$   
 $E_{1n}, F_{1n}, G_{1n}$ } coefficients in difference equation (45a) and defined by  
equations (B3)

$A_{2n}, B_{2n}, C_{2n}, D_{2n}$   
 $E_{2n}, F_{2n}, G_{2n}$ } coefficients in difference equation (45b) and defined by  
equations (B4)

a speed of sound

$a_1, a_2, a_3, a_4$  coefficients in molecular viscosity relations (see eqs. (7))

$C_f$  skin-friction coefficient

$c_p$  specific heat at constant pressure

D damping term (eq. (17a))

F velocity ratio,  $u/u_e$

$h$	heat-transfer coefficient
$i$	index used in grid-point notation (see eq. (41))
$k$	geometric progression constant, $\Delta\eta_{i+1}/\Delta\eta_i$
$k_\ell$	thermal conductivity
$k_T$	eddy conductivity (see eq. (2c))
$k_1$	constant in eddy-viscosity model (see eq. (16a))
$k_2$	constant in eddy-viscosity model (see eq. (16b))
$k_3$	constant in intermittency function (see eq. (17c))
$k_4$	constant in intermittency function (see eq. (17c))
$k_5$	constant in mixing-length model (see eq. (20b))
$L_r$	reference length
$l$	defined in equation (30)
$\bar{\lambda}$	mixing length (see eq. (20a))
$M$	Mach number
$m$	grid-point index in S-direction
$N$	number of grid points normal to wall boundary
$N_O$	reference number of grid points normal to wall boundary (see eq. (42))
$N_{Pr}$	Prandtl number, $c_p\mu/k_\ell$
$N_{Pr,t}$	static turbulent Prandtl number (see eqs. (3))
$N_{Re}$	unit Reynolds number, $u_e/\nu_e$
$N_{Re,r}$	reference Reynolds number, $\rho_r u_r L_r / \mu_r$
$N_{Re,s}$	Reynolds number based on $s$ , $u_e s / \nu_e$
$N_{Re,s_{t,i}}$	Reynolds number at transition, $u_e s_{t,i} / \nu_e$
$N_{Re,\delta^*}$	Reynolds number based on displacement thickness, $u_e \delta^* / \nu_e$
$N_{Re,\theta}$	Reynolds number based on momentum thickness, $u_e \theta / \nu_e$
$N_{Re,\infty}$	free-stream unit Reynolds number, $u_\infty / \nu_\infty$
$N_{St}$	Stanton number, $h / (c_p \rho u)$

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n	grid-point index in Y-direction (see fig. 1)
$p^{(1)}, p^{(2)}, p^{(3)}$	defined in equations (50)
p	pressure
$Q^{(1)}, Q^{(2)}, Q^{(3)}$	defined in equations (50)
q	heat-transfer rate
R, Z	body axis system with origin at stagnation point, where Z is positive downstream and R is positive radially outward (see fig. 2)
$R_g$	gas constant (see eq. (6))
r	radial body coordinate measured normal to Z-axis (see fig. 2)
$r_o$	body radius (see fig. 2)
$r_s$	radial coordinate of shock wave (see fig. 2)
S, Y	orthogonal boundary-layer coordinate system with origin at stagnation point, where S lies along the body surface and is positive downstream and Y is normal to the body surface and positive outward (see fig. 2)
s	boundary-layer coordinate along S-axis (see fig. 2)
$s_{t,f}$	end of transition (see fig. 2)
$s_{t,i}$	beginning of transition (see fig. 2)
T	static temperature
t	transverse-curvature term (see eqs. (23))
u	velocity component in S-direction (fig. 2)
$u_t$	friction velocity, $\sqrt{\tau_w/\rho}$
v	transformed normal-velocity component (see eq. (26))
v	velocity component in Y-direction
$\tilde{v}$	velocity component, $v + \frac{\rho' v'}{\rho}$
$v^+$	velocity component, $\tilde{v} \sqrt{N_{Re,r}}$
$x_1, x_2, \dots, x_5$	functions of grid-point distribution (see eqs. (A4) to (A8))
$y_1, y_2, \dots, y_6$	functions of grid-point distributions (see eqs. (A12) to (A17))
y	boundary-layer coordinate along Y-axis (see fig. 2)
$\tilde{y}$	stretched y-coordinate (see eq. (15))

$y_m$	match point for two-layer eddy-viscosity model
$z$	axial body coordinate (see fig. 2)
$\alpha$	defined in equation (30)
$\beta$	defined in equation (30)
$\Gamma$	streamwise intermittency distribution (see eq. (38))
$\gamma$	ratio of specific heats
$\bar{\gamma}$	transverse intermittency distribution (see eq. (17c))
$\Delta s, \Delta y$	grid-point spacing, physical plane
$\Delta s_t$	transition extent, $s_{t,f} - s_{t,i}$
$\Delta \xi, \Delta n$	grid-point spacing, transformed plane (see fig. 1)
$\Delta^*$	defined in equation (50g)
$\delta$	boundary-layer thickness
$\delta^*$	displacement thickness
$\delta_{inc}^*$	incompressible displacement thickness, $\int_0^\infty (1 - F) dy$
$\varepsilon$	eddy viscosity, $-\rho \frac{\overline{u'v'}}{\partial u / \partial y}$
$\bar{\varepsilon}$	defined in equation (5a)
$\tilde{\varepsilon}$	defined in equation (5b)
$\theta$	static-temperature ratio, $T/T_e$
$\theta$	momentum thickness
$\theta_s$	shock-wave angle (see fig. 2)
$\lambda$	defined in equation (40)
$\mu$	molecular viscosity
$\nu$	kinematic viscosity, $\mu/\rho$
$\xi, \eta$	transformed boundary-layer coordinates (see fig. 1 and eqs. (22))
$\bar{\xi}$	defined in equation (39)
$\rho$	density
$\tau$	shear stress

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$\phi$  local surface angle (see fig. 2)

$\chi$  vorticity Reynolds number,  $\frac{y^2}{v} \left( \frac{\partial u}{\partial y} \right)$

$\chi_{max}$  maximum value of  $(\chi)_{m+1}$

$\psi$  stream function (see fig. 2)

Subscripts:

$aw$  adiabatic wall

$e$  based on boundary-layer edge conditions

$i$  inner region of turbulent layer

$m$  mesh point in  $\xi$ -direction (see fig. 1)

$max$  maximum value

$n$  mesh point in  $\eta$ -direction (see fig. 1)

$o$  outer region of turbulent layer

$r$  reference quantity

$s$  shock

$t$  total condition

$w$  wall value

$\infty$  free stream

Superscript:

$j$  flow index;  $j = 0$  for planar flow,  $j = 1$  for axisymmetric flow

An asterisk (\*) on a symbol denotes a dimensional quantity.

A prime on a symbol denotes a fluctuating component.

A bar over a symbol denotes the time average value.

A coordinate used as a subscript denotes the partial differential with respect to the coordinate. (See eqs. (A1).)

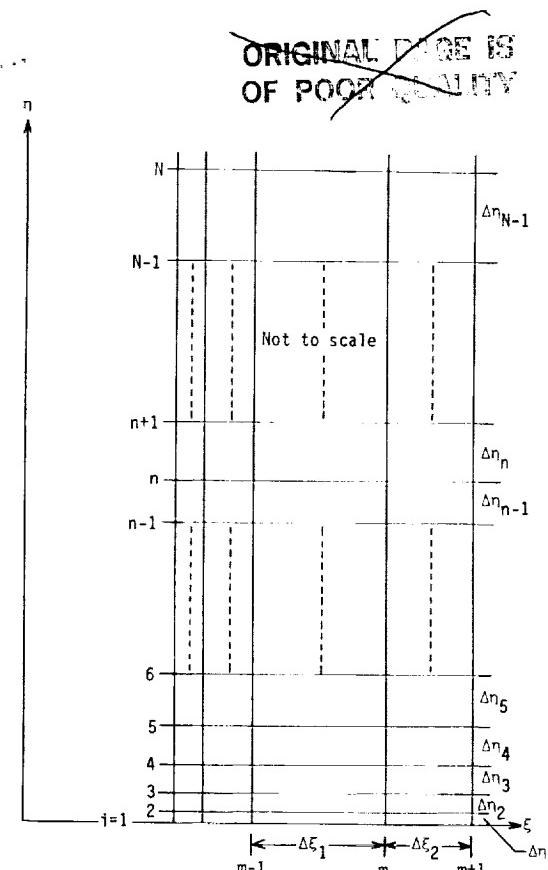


Figure 1.- Finite-difference grid model.

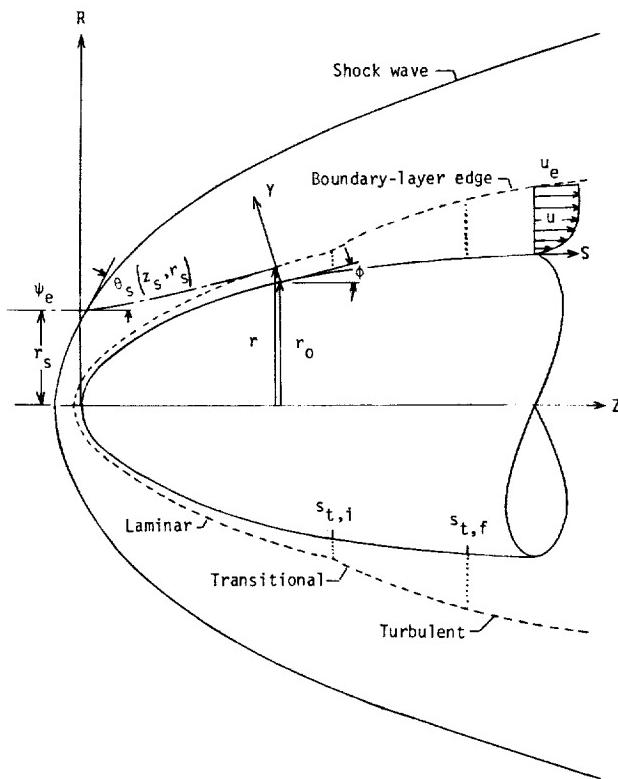


Figure 2.- Coordinate system and notation.

#### PROBLEM DESCRIPTION

This section presents the governing equations for compressible laminar, transitional, or turbulent boundary-layer flows together with the required boundary conditions. It should be noted that the system of equations can be found in numerous references (e.g., see refs. 2 and 3); however, for completeness, the equation set is presented in order to allow the user to modify the software if required. The algebraic turbulence closure, transition location and extent, and transitional-flow-structure models are presented and briefly discussed; however, the reader interested in a detailed discussion of these models is referred to references 2, 3, and 8.

#### Basic Partial Differential Equations

Dimensional governing equations.- The mean turbulent boundary-layer equations can be written as follows:

##### Continuity

$$\frac{\partial}{\partial s^*} \left( r^* j \rho^* u^* \right) + \frac{\partial}{\partial y^*} \left[ r^* j \rho^* \left( v^* + \frac{\overline{v'v'}}{\rho^*} \right) \right] = 0 \quad (1a)$$

##### Momentum

$$\rho^* \left[ u^* \frac{\partial u^*}{\partial s^*} + \left( v^* + \frac{\overline{v'v'}}{\rho^*} \right) \frac{\partial u^*}{\partial y^*} \right] = - \frac{dp^*}{ds^*} + \frac{1}{r^* j} \frac{\partial}{\partial y^*} \left[ r^* j \left( u^* \frac{\partial u^*}{\partial y^*} - \rho^* \overline{u'v'} \right) \right] \quad (1b)$$

##### Energy

$$\begin{aligned} \rho^* \left[ u^* \frac{\partial}{\partial s^*} (c_p^* T^*) + \left( v^* + \frac{\overline{v'v'}}{\rho^*} \right) \frac{\partial}{\partial y^*} (c_p^* T^*) \right] &= u^* \frac{dp^*}{ds^*} + \frac{1}{r^* j} \frac{\partial}{\partial y^*} \left[ r^* j \frac{k_l^*}{c_p^*} \frac{\partial}{\partial y^*} (c_p^* T^*) \right] \\ &\quad + \mu^* \left( \frac{\partial u^*}{\partial y^*} \right)^2 + \frac{1}{r^* j} \frac{\partial}{\partial y^*} \left[ r^* j \left( -c_p^* \rho^* \overline{v'T'} \right) \right] \\ &\quad - \rho^* \overline{u'v'} \frac{\partial u^*}{\partial y^*} \end{aligned} \quad (1c)$$

The mean turbulent equations are identical to those for laminar flow with the exception of the correlations of turbulent fluctuating quantities. These correlations must be related to the mean flow in order to obtain a closed system of equations. In the present analysis, the apparent mass-flux term  $\overline{\rho^* v'}$ , the apparent stress term  $\overline{\rho^* u' v'}$  (Reynolds stress), and the apparent heat-flux term  $\overline{c_p^* \rho^* v' T'}$  are modeled or represented by a new velocity component  $\tilde{v}^*$ , an eddy viscosity  $\epsilon^*$ , and an eddy conductivity  $k_l^*$ , respectively, as follows:

$$\tilde{v}^* = v^* + \frac{\overline{\rho^* v^*}}{\rho^*} \quad (2a)$$

$$\epsilon^* = -\rho^* \frac{\overline{u^* v^*}}{\partial u^*/\partial y^*} \quad (2b)$$

$$k_T^* = -c_p^* \rho^* \frac{\overline{v^* T^*}}{\partial T^*/\partial y^*} \quad (2c)$$

The static turbulent Prandtl number is defined as follows:

$$N_{Pr,t} = \frac{\overline{u^* v^*}}{\overline{v^* T^*}} \left( \frac{\partial T^*/\partial y^*}{\partial u^*/\partial y^*} \right) \quad (3a)$$

Equation (3a) can then be rewritten in terms of equations (2b) and (2c) as

$$N_{Pr,t} = \frac{c^* \epsilon^*}{k_T^*} \quad (3b)$$

In terms of equations (2) and (3), the governing differential equations can be written as follows:

#### Continuity

$$\frac{\partial}{\partial s^*} (r^* j \rho^* u^*) + \frac{\partial}{\partial y^*} (r^* j \rho^* \tilde{v}^*) = 0 \quad (4a)$$

#### Momentum

$$\rho^* \left( u^* \frac{\partial u^*}{\partial s^*} + \tilde{v}^* \frac{\partial u^*}{\partial y^*} \right) = - \frac{dp^*}{ds^*} + \frac{1}{r^* j} \frac{\partial}{\partial y^*} \left( r^* j \bar{\epsilon}^* \frac{\partial u^*}{\partial y^*} \right) \quad (4b)$$

#### Energy

$$\begin{aligned} \rho^* \left[ u^* \frac{\partial}{\partial s^*} (c_p^* T^*) + \tilde{v}^* \frac{\partial}{\partial y^*} (c_p^* T^*) \right] &= u^* \frac{dp^*}{ds^*} + \bar{\epsilon}^* \left( \frac{\partial u^*}{\partial y^*} \right)^2 \\ &+ \frac{1}{r^* j} \frac{\partial}{\partial y^*} \left[ r^* j \tilde{\epsilon}^* \frac{\partial}{\partial y^*} (c_p^* T^*) \right] \end{aligned} \quad (4c)$$

The terms  $\overline{\varepsilon^*}$  and  $\tilde{\varepsilon}^*$  appearing in equations (4) are defined as follows:

$$\overline{\varepsilon^*} = \mu^* \left( 1 + \frac{\varepsilon^*}{\mu^*} \Gamma \right) \quad (5a)$$

$$\tilde{\varepsilon}^* = \frac{\mu^*}{N_{Pr}} \left( 1 + \frac{\varepsilon^*}{\mu^*} \frac{N_{Pr}}{N_{Pr,t}} \Gamma \right) \quad (5b)$$

The function  $\Gamma$  appearing in equations (5) represents the streamwise intermittency distribution for the transitional-flow region. The  $\Gamma$  distribution assumes a value of zero for laminar flows, a value of unity for fully turbulent flows, and a range of 0 to 1 for the transitional region of flow. The variation of  $\Gamma$  in the transitional region depends upon the statistical growth and distribution of turbulent spots. The model used to represent  $\Gamma$  is discussed in a subsequent section of the present paper.

The system of equations is closed by the addition of the perfect-gas law and a viscosity-temperature relation. The perfect-gas law is written as

$$p^* = \rho^* R_g T^* \quad (6)$$

Two viscosity-temperature relations are provided: (1) the Sutherland law

$$\mu^* = \frac{a_1^* (T^*)^{3/2}}{T^* + a_2^*} \quad (7a)$$

and (2) the power law

$$\mu^* = a_3^* (T^*)^{a_4} \quad (7b)$$

The pressure-gradient term in equations (4) is replaced by the Bernoulli relation

$$\frac{dp^*}{ds^*} = -\rho_e^* u_e^* \frac{du_e^*}{ds^*} \quad (8)$$

for constant entropy flows; however, for variable entropy flows the value of  $dp^*/ds^*$  is explicitly retained in the equation system.

The equations are rewritten in nondimensional form where the nondimensional variables are as follows:

$$\left. \begin{array}{l} u = u^*/u_r^* \\ v = v^*/u_r^* \\ p = p^*/(\rho_r^* u_r^{2*}) \\ \rho = \rho^*/\rho_r^* \\ T = T^*/T_r^* \\ \mu = \mu^*/\mu_r^* \end{array} \right\} \quad (9)$$

where all dimensional lengths are nondimensionalized by a reference length  $L_r^*$ . The reference values of density and velocity are taken to be those of the free stream, the reference temperature is taken to be  $u_r^{2*}/c_p^*$ , and the reference viscosity is the viscosity obtained from either equation (7a) or (7b) evaluated at the reference temperature.

Nondimensional governing equations.- The nondimensional equations are as follows:

#### Continuity

$$\frac{\partial}{\partial s}(r^j \rho u) + \frac{\partial}{\partial \tilde{y}}(r^j \rho v^+) = 0 \quad (10)$$

#### Momentum

$$\rho \left( u \frac{\partial u}{\partial s} + v^+ \frac{\partial u}{\partial \tilde{y}} \right) = - \frac{dp^*}{ds} + \frac{1}{r^j} \frac{\partial}{\partial \tilde{y}} \left( r^j \bar{\epsilon} \frac{\partial u}{\partial \tilde{y}} \right) \quad (11)$$

#### Energy

$$\rho \left( u \frac{\partial T}{\partial s} + v^+ \frac{\partial T}{\partial \tilde{y}} \right) = u \frac{dp}{ds} + \frac{1}{r^j} \frac{\partial}{\partial \tilde{y}} \left( r^j \bar{\epsilon} \frac{\partial T}{\partial \tilde{y}} \right) + \bar{\epsilon} \left( \frac{\partial u}{\partial \tilde{y}} \right)^2 \quad (12)$$

#### Equation of State

$$p = \left( \frac{\gamma - 1}{\gamma} \right) \rho T \quad (13)$$

Viscosity-Temperature

$$\left. \begin{aligned} \mu &= T^{3/2} \left( \frac{1 + a_2}{T + a_2} \right) \\ \text{or} \\ \mu &= T^{a_4} \end{aligned} \right\} \quad (14)$$

where

$$\left. \begin{aligned} \tilde{y} &= y \sqrt{N_{Re,r}} \\ v^+ &= \tilde{v} \sqrt{N_{Re,r}} \\ a_2 &= a_2^*/T_r^* \end{aligned} \right\} \quad (15)$$

Turbulence closure.- Algebraic models are used to close the system of equations. Two options are provided: (1) a two-layer eddy-viscosity model (KODVIS = 2), and (2) a mixing-length model (KODVIS = 1).

Two-layer model

The equations describing the two-layer model are as follows (see ref. 8):

$$\left( \frac{\varepsilon}{\mu} \right)_i = \frac{\rho^*}{\mu^*} (k_1 y^* D)^2 \left| \frac{\partial u^*}{\partial y^*} \right| \quad (0 \leq y^* \leq y_m^*) \quad (16a)$$

$$\left( \frac{\varepsilon}{\mu} \right)_o = \frac{\rho^*}{\mu^*} k_2 u_e^* (\delta_{inc}^*)^* \bar{\gamma} \quad (y_m^* < y^*) \quad (16b)$$

where

$$D = 1 - \exp(-y^*/A^*) \quad (17a)$$

$$(\delta_{inc}^*)^* = \int_0^\infty \left( 1 - \frac{u}{u_e} \right) dy^* \quad (17b)$$

and

$$\bar{\gamma} = \frac{1 - \operatorname{erf} \left[ k_3 \left( \frac{y}{\delta} - k_4 \right) \right]}{2} \quad (17c)$$

The boundary-layer thickness  $\delta$  in equation (17c) is defined as the distance normal to the wall boundary where  $u/u_e = 0.995$ . The empirical constants  $k_1$  to  $k_4$  are assigned values of 0.4, 0.0168, 5.0, and 0.78, respectively.

The location of the boundary separating the two layers  $y_m^*$  is defined from the continuity of eddy viscosity; that is, where

$$\left( \frac{\varepsilon}{\mu} \right)_i = \left( \frac{\varepsilon}{\mu} \right)_o \quad (18)$$

#### Mixing-length model

A mixing-length option (KODVIS = 1) is provided for those interested in utilizing experimental mixing-length data. The eddy-viscosity distribution across the boundary layer can be written as follows:

$$\frac{\varepsilon}{\mu} = \frac{\rho^*}{\mu^*} \bar{\lambda}^{*2} \left| \frac{\partial u^*}{\partial y^*} \right| \quad (19)$$

where the mixing length  $\bar{\lambda}^*$  can be expressed as

$$\frac{\bar{\lambda}}{\delta} = D \bar{\gamma} f \left( \frac{y}{\delta} \right) \quad (20a)$$

An analytic formulation is provided in subroutine TURBLNT for  $f \left( \frac{y}{\delta} \right)$  as follows (see ref. 10):

$$f \left( \frac{y}{\delta} \right) = k_5 \tan h \left( \frac{k_1}{k_5} \frac{y}{\delta} \right) \quad (20b)$$

where  $k_5$  is assigned the value of 0.108. It should be noted that the assigned values of  $k_1, k_2, \dots, k_5$  and the definition of  $\delta$  can be modified through input to program VGBLP.

### Eddy conductivity

The eddy conductivity (eq. (2c)) is modeled as a static turbulent Prandtl number (eq. (3a)). Three options are provided in subroutines TURBLNT for  $N_{Pr,t}$ : (1) a constant, for example  $N_{Pr,t} = 0.95$  (KODPRT = 1); (2) the Rotta (ref. 11) distribution (KODPRT = 2)

$$N_{Pr,t} = \frac{(N_{Pr,t})_w}{2} \left[ 2 - \left( \frac{y}{\delta} \right)^2 \right] \quad (21)$$

and (3) a distribution  $N_{Pr,t} = g\left(\frac{y}{\delta}\right)$  specified in tabular form from experimental data (KODPRT = 3).

Transformed plane.- The system of governing equations is singular at  $s = 0$ . The Probstein-Elliott (ref. 12) and Levy-Lees (ref. 13) transformation is used to remove this singularity as well as to reduce the growth of the boundary layer as the solution proceeds downstream. This transformation can be written as follows:

$$\xi(s) = \int_0^s \rho_e u_e \mu_e r_o^{2j} ds \quad (22a)$$

$$\eta(s, \tilde{y}) = \frac{\rho_e u_e r_o^j}{\sqrt{2\xi}} \int_0^{\tilde{y}} t^j \left( \frac{\rho}{\rho_e} \right) d\tilde{y} \quad (22b)$$

where the parameter  $t$  appearing in equation (22b) is the transverse-curvature term, defined as

$$t = \frac{x}{r_o} \quad (23a)$$

or, in terms of the  $y$ -coordinate, as

$$t = 1 + \frac{y}{r_o} \cos \phi \quad (23b)$$

The relation between derivatives in the stretched physical  $(s, \tilde{y})$  and transformed  $(\xi, \eta)$  coordinate system is as follows:

$$\left( \frac{\partial}{\partial s} \right)_{\tilde{y}} = \rho_e u_e \mu_e r_o^{2j} \left( \frac{\partial}{\partial \xi} \right)_{\eta} + \left( \frac{\partial \eta}{\partial s} \right) \left( \frac{\partial}{\partial \eta} \right)_{\xi} \quad (24a)$$

$$\left( \frac{\partial}{\partial \tilde{y}} \right)_s = \frac{\rho_e u_e r_o^{j+1}}{\sqrt{2\xi}} \left( \frac{\rho}{\rho_e} \right) \left( \frac{\partial}{\partial \eta} \right)_{\xi} \quad (24b)$$

Two parameters  $F$  and  $\Theta$  are introduced and defined as

$$\left. \begin{aligned} F &= \frac{u}{u_e} \\ \Theta &= \frac{T}{T_e} \end{aligned} \right\} \quad (25)$$

together with a transformed normal velocity

$$v = \frac{2\xi}{\rho_e u_e \mu_e r_o^2 j} \left[ F \left( \frac{\partial \eta}{\partial s} \right) + \frac{\rho \tilde{v} r_o^j t^j}{\sqrt{2\xi}} \right] \quad (26)$$

The governing equations in the transformed plane can then be written as follows:

#### Continuity

$$\frac{\partial v}{\partial \eta} + 2\xi \frac{\partial F}{\partial \xi} + F = 0 \quad (27)$$

#### Momentum

$$2\xi F \frac{\partial F}{\partial \xi} + v \frac{\partial F}{\partial \eta} - \frac{\partial}{\partial \eta} \left( t^{2j} l \tilde{\epsilon} \frac{\partial F}{\partial \eta} \right) + \beta (F^2 - \Theta) = 0 \quad (28)$$

#### Energy

$$2\xi F \frac{\partial \Theta}{\partial \xi} + v \frac{\partial \Theta}{\partial \eta} - \frac{\partial}{\partial \eta} \left( t^{2j} l \tilde{\epsilon} \frac{\partial \Theta}{\partial \eta} \right) - \alpha l t^{2j} \tilde{\epsilon} \left( \frac{\partial F}{\partial \eta} \right)^2 = 0 \quad (29)$$

where

$$\left. \begin{aligned} l &= \frac{\rho u}{(\rho \mu)_e} \\ \alpha &= (\gamma - 1) M_e^2 \\ \beta &= \frac{2\xi}{u_e} \left( \frac{du_e}{d\xi} \right) \end{aligned} \right\} \quad (30)$$

By using the viscosity relations (eqs. (14)) and the equation of state (eq. (13)), the parameter  $\lambda$  can be written as follows:

Sutherland law

$$\lambda = \sqrt{\Theta} \left( \frac{1 + a_2/T_e}{\Theta + a_2/T_e} \right) \quad (31a)$$

Power law

$$\lambda = (\Theta)^{a_4 - 1} \quad (31b)$$

The transverse-curvature term can be written in terms of the transformed variables as

$$t = \left( 1 + \frac{2\sqrt{2\xi} \cos \phi}{\rho_e u_e r_o^{2j} \sqrt{N_{Re,r}}} \int_0^\eta \Theta d\eta \right)^{1/2} \quad (32)$$

The physical coordinate normal to the wall is obtained from the inverse transformation; namely,

$$y = \frac{r_o}{\cos \phi} \left[ -1 + \left( 1 + \frac{2\sqrt{2\xi} \cos \phi}{\rho_e u_e r_o^{2j} \sqrt{N_{Re,r}}} \int_0^\eta \Theta d\eta \right)^{1/2} \right] \quad (33)$$

The boundary conditions in the transformed plane are as follows:

Wall boundary

$$\left. \begin{array}{l} F(\xi, 0) = 0 \\ V(\xi, 0) = V_w(\xi) \\ \Theta(\xi, 0) = \Theta_w(\xi) \end{array} \right\} \quad (34a)$$

or

$$\left. \left( \frac{\partial \Theta}{\partial \eta} \right)_{\xi, 0} = \left( \frac{\partial \Theta}{\partial \eta} \right)_w \right\}$$

Edge boundary

$$\left. \begin{array}{l} F(\xi, n_e) = 1 \\ \theta(\xi, n_e) = 1 \end{array} \right\} \quad (34b)$$

The boundary condition at the wall for the transformed  $V$  component can be related to the physical plane as (see eq. (26))

$$v_w = \frac{\sqrt{2\xi}}{\mu_e r_o} \left( \frac{\rho_w v_w}{\rho_e u_e} \right) \quad (35)$$

Transition

Transition location. - Because of the large parameter space influencing transition to turbulence (refs. 14 to 17), it is not possible to predict with assurance the location of transition for general flows. However, for certain classes of geometry (e.g., flat plate, cone, etc.), empirical correlations are available. These empirical correlations can be used with confidence provided one realizes that a probable range of transition locations is being predicted. In program VGBLP either the transition location (SST) or the stability index at transition (SMXTR; see ref. 8) must be specified; however, any correlation can be directly incorporated into the program.

Transition extent. - The assumption of a universal intermittency distribution implies that the transition-zone length (transition extent) can be expressed as a function of the Reynolds number at transition  $u_{est,i}/v_e$ . In reference 9 it is shown, for the transition data considered, that the data are represented on the average by the equation

$$N_{Re,\Delta s_t} = 5(N_{Re,s_{t,i}})^{0.8} \quad (36)$$

where  $N_{Re,\Delta s_t} = \frac{u_e}{v_e}(s_{t,f} - s_{t,i})$ . The location of the end of transition  $s_{t,f}$  can then be obtained directly from equation (36) as follows:

$$s_{t,f} = s_{t,i} + 5N_{Re,\Delta s_t}^{-1} (N_{Re,s_{t,i}})^{0.8} \quad (37)$$

where  $N_{Re}$  is the local unit Reynolds number,  $u_e/v_e$ .

In program VGBLP the extent of the transition region ( $s_{t,f} - s_{t,i}$ ) can be specified in one of two ways: (1) from equation (37) (KTCOD = 1); or (2) from the specification of  $s_{t,f}/s_{t,i}$  obtained from experimental data (KTCOD = 2). It should be noted that the program can be easily modified to include any desired correlation or equation in place of equation (37).

Transition-flow structure.- The parameter  $\Gamma$  (eqs. (5)) is the streamwise intermittency function which models the turbulent spot distribution in the transitional region. The parameter is a function of the s-coordinate only and is defined (see ref. 9) as follows:

$$\Gamma(\bar{\xi}) = 1 - \exp(-0.412\bar{\xi}^2) \quad (38)$$

where

$$\bar{\xi} = \frac{s - s_{t,i}}{\lambda} \quad (39)$$

and

$$\lambda = (s)_{\Gamma=\frac{3}{4}} - (s)_{\Gamma=\frac{1}{4}} \quad (40)$$

It should be noted that  $\Gamma = 0$  for laminar flow,  $\Gamma = 1$  for fully turbulent flow, and  $\Gamma$  ranges from 0 to 1 for the transitional-flow region. Equations (27) to (29) reduce to the classical laminar boundary-layer equations when  $\Gamma$  is set to zero.

#### SOLUTION TECHNIQUE

The system of governing equations (eqs. (27) to (29)) is parabolic and, therefore, can be numerically integrated by a marching procedure in the streamwise direction. In order to cast the equations into a form in which the marching procedure can be implemented, the derivatives with respect to  $\xi$  and  $\eta$  are replaced by finite-difference quotients. The method of linearization and solution used in the analysis closely parallels that of references 5 and 6.

#### Finite-Difference Mesh

Because of the magnitude and variation of the gradients of the dependent variables ( $\partial F / \partial y$ ;  $\partial \theta / \partial y$ ) near the wall boundary for turbulent flow, it is computationally inefficient to use equally spaced mesh points in the y-coordinate. This problem can be alleviated by selecting a variable mesh-point distribution such that  $\Delta n_{i+1} / \Delta n_i > 1$  where the distribution in the wall region is chosen sufficiently small to resolve all gradients. One approach to grid specification is to use a geometric progression

$$\Delta n_i = (k)^{i-1} \Delta n_1 \quad (i = 2, 3, 4, \dots, N) \quad (41)$$

where  $k$  is defined as the geometric progression constant  $\Delta n_{i+1} / \Delta n_i$ . A schematic of such a grid is presented (not to scale) in figure 1.

Blottner (ref. 7) introduced a variable-grid scheme that is more computationally efficient than the differencing scheme and mesh distribution used in references 3 and 4. The Blottner variable-grid scheme (ref. 7) and the Cebeci-Keller box scheme

(ref. 18) appear to be two of the most promising schemes currently available in the literature for solving the boundary-layer equations. The Cebeci-Keller box scheme, although efficient for two-dimensional flow, yields block-tridiagonal matrices and requires greater computational effort than the simple-tridiagonal matrices of the Blottner variable-grid scheme. Blottner has shown (ref. 7) that the variable-grid scheme is as accurate as the box scheme for the two-dimensional boundary-layer equations and, furthermore, that large values of the geometric progression constant can be used for the normal mesh-point distribution, provided the variable grid is interpreted as a coordinate transformation. In reference 8 it was shown that  $k$  values on the order of 1.04 could be used for turbulent flows. In reference 19 it was shown that an accuracy requirement on  $\tau_w$  of 1 percent required approximately 220 mesh points normal to the wall with  $k \approx 1.04$ . In order to increase the computational efficiency of such schemes one can reduce the number of mesh points while simultaneously increasing the value of  $k$ ; however, this approach generally results in unacceptable levels of accuracy. Blottner (ref. 7) demonstrated that with the variable-grid scheme satisfactory results could be obtained with approximately 20 mesh points for  $k = 1.82$ . Vatsa and Goglia (ref. 20), using the method of reference 4, showed that the variable-grid scheme proposed by Blottner (ref. 7) could reduce the number of grid points from approximately 201 to 61 for a specified 1-percent accuracy in wall shear stress. They also showed that for most applications one could obtain reasonably accurate solutions for turbulent boundary layers with as few as 25 to 30 mesh points, as compared to approximately 200 mesh points for the method of reference 3.

Blottner (ref. 7) introduced a modified definition for the geometric progression constant such that

$$\bar{k} = (k)^{\frac{N-1}{N_0-1}} \quad (42)$$

where  $\bar{k}$  is now defined as the conventional geometric progression constant for  $N_0$  mesh points normal to the wall. Using equation (41), one obtains

$$\eta_i = \eta_e \left( \frac{k^{i-1} - 1}{k^{N-1} - 1} \right) \quad (43)$$

which when combined with equation (42) yields the following for the  $\eta$ -mesh distribution:

$$\eta_i = \eta_e \left[ \frac{(\bar{k})^{(i-1)(N_0-1)/(N-1)} - 1}{(\bar{k})^{N_0-1} - 1} \right] \quad (44)$$

Two options are provided in program VGBLP: (1) specify  $\eta_{max}$ ,  $N$ , and  $k$  (IGEOM = 1); or (2) specify  $\eta_{max}$ ,  $N$ , and  $\Delta\eta_1$  (IGEOM = 2). Of these two options, it is recommended that the user select the first option (IGEOM = 1) where the value of  $k$  is computed from equation (42) for specified values of  $\bar{k}$  and  $N_0$ . Typical values for  $\bar{k}$  and  $N_0$  are 1.5 and 25, respectively, for  $N \geq 41$ . (See ref. 20.) It is obvious that the larger the selected value of  $N$  and the smaller the value

of  $k - 1$  ( $k \geq 1$ ), the more accurate the solution. Since program VGBLP is very efficient in terms of computer resources, it is suggested that potential users of the program perform a series of numerical experiments over a range of  $k$  and  $N$  values in order to gain experience with the procedure. If the second option (IGEOM = 2) is selected (specify  $\eta_{\max}$ ,  $N$ , and  $\Delta\eta_1$ ), the user is cautioned to exercise care in selecting the number of grid points. If transitional or turbulent flow occurs in a given problem, the laminar region of the boundary layer is calculated with the value of  $k$  used for the turbulent region; that is, for a given solution,  $k$  is invariant.

### Difference Equations

Three-point implicit difference relations (see appendices A and B) are used to reduce the transformed momentum and energy equations (eqs. (28) and (29), respectively) to finite-difference form. The difference quotients produce linear difference equations when substituted into the momentum and energy equations provided truncation terms of the order  $\Delta\xi_{m-1} \Delta\xi_m$  and  $\Delta\eta_{n-1} \Delta\eta_n$  are neglected. (It should be noted that the truncation term for  $\partial^2 F / \partial \eta^2$  is of the order  $(\Delta\eta_{n-1} - \Delta\eta_n)$ .) The resulting difference equations may be written as follows:

#### Momentum equation

$$\begin{aligned} A_{1n} F_{m+1,n-1} + B_{1n} F_{m+1,n} + C_{1n} F_{m+1,n+1} + D_{1n} \theta_{m+1,n-1} \\ + E_{1n} \theta_{m+1,n} + F_{1n} \theta_{m+1,n+1} = G_{1n} \end{aligned} \quad (45a)$$

#### Energy equation

$$\begin{aligned} A_{2n} F_{m+1,n-1} + B_{2n} F_{m+1,n} + C_{2n} F_{m+1,n+1} + D_{2n} \theta_{m+1,n-1} \\ + E_{2n} \theta_{m+1,n} + F_{2n} \theta_{m+1,n+1} = G_{2n} \end{aligned} \quad (45b)$$

The coefficients  $A_{1n}$ ,  $B_{1n}$ , ...,  $G_{1n}$  and  $A_{2n}$ ,  $B_{2n}$ , ...,  $G_{2n}$  (see appendix B) are functions of known quantities at stations  $m$  and  $m-1$ . It is important to note that equations (45) are coupled through the dependent variables  $F$  and  $\theta$ ; however, the dependent variable  $V$  does not appear explicitly as an unknown at station  $m+1$ . The variable  $V$  is uncoupled from the system because of the particular way that the non-linear terms  $V \frac{\partial F}{\partial \eta}$  and  $V \frac{\partial \theta}{\partial \eta}$  are linearized. (See eq. (A23).)

### Solution of Difference Equations

The system of difference equations (eqs. (45)) represents a set of  $2(N - 1)$  linear algebraic equations for  $2(N - 1)$  unknowns. The boundary conditions to be used with the difference equations are specified in equations (34). The  $2(N - 1)$  linear algebraic equations may be written in tridiagonal matrix form; consequently, an efficient algorithm (Thomas algorithm) is available for simultaneous solution.

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The simultaneous or coupled-solution technique is presented in appendix B of reference 5; however, because of differences between the present work and that presented in reference 5, the solution technique is discussed here in some detail.

Because of the special form of equations (45), the following relations exist (see ref. 21):

$$F_{m+1,n-1} = P_{m+1,n-1}^{(1)} + P_{m+1,n-1}^{(2)} F_{m+1,n} + P_{m+1,n-1}^{(3)} \theta_{m+1,n} \quad (46a)$$

$$\theta_{m+1,n-1} = Q_{m+1,n-1}^{(1)} + Q_{m+1,n-1}^{(2)} F_{m+1,n} + Q_{m+1,n-1}^{(3)} \theta_{m+1,n} \quad (46b)$$

Next, equations (46) are substituted into equations (45) to obtain the following relations:

$$\begin{aligned} B1_{m+1,n}^* F_{m+1,n} + E1_{m+1,n}^* \theta_{m+1,n} &= G1_{m+1,n}^* - C1_{m+1,n} F_{m+1,n+1} \\ &\quad - F1_{m+1,n} \theta_{m+1,n+1} \end{aligned} \quad (47a)$$

$$\begin{aligned} B2_{m+1,n}^* F_{m+1,n} + E2_{m+1,n}^* \theta_{m+1,n} &= G2_{m+1,n}^* - C2_{m+1,n} F_{m+1,n+1} \\ &\quad - F2_{m+1,n} \theta_{m+1,n+1} \end{aligned} \quad (47b)$$

where

$$B1_{m+1,n}^* = B1_{m+1,n} + A1_{m+1,n} P_{m+1,n-1}^{(2)} + D1_{m+1,n} Q_{m+1,n-1}^{(2)} \quad (48a)$$

$$E1_{m+1,n}^* = E1_{m+1,n} + A1_{m+1,n} P_{m+1,n-1}^{(3)} + D1_{m+1,n} Q_{m+1,n-1}^{(3)} \quad (48b)$$

$$G1_{m+1,n}^* = G1_{m+1,n} - A1_{m+1,n} P_{m+1,n-1}^{(1)} - D1_{m+1,n} Q_{m+1,n-1}^{(1)} \quad (48c)$$

$$B2_{m+1,n}^* = B2_{m+1,n} + A2_{m+1,n} P_{m+1,n-1}^{(2)} + D2_{m+1,n} Q_{m+1,n-1}^{(2)} \quad (48d)$$

$$E2_{m+1,n}^* = E2_{m+1,n} + A2_{m+1,n} P_{m+1,n-1}^{(3)} + D2_{m+1,n} Q_{m+1,n-1}^{(3)} \quad (48e)$$

and

$$G2_{m+1,n}^* = G2_{m+1,n} - A2_{m+1,n} P_{m+1,n-1}^{(1)} - D2_{m+1,n} Q_{m+1,n-1}^{(1)} \quad (48f)$$

The unknown values of  $F$  and  $\theta$  at station  $m+1, n$  are obtained from equations (47) as follows:

$$F_{m+1,n} = P_{m+1,n}^{(1)} + P_{m+1,n}^{(2)} F_{m+1,n+1} + P_{m+1,n}^{(3)} \theta_{m+1,n+1} \quad (49a)$$

$$\theta_{m+1,n} = Q_{m+1,n}^{(1)} + Q_{m+1,n}^{(2)} F_{m+1,n+1} + Q_{m+1,n}^{(3)} \theta_{m+1,n+1} \quad (49b)$$

where

$$P_{m+1,n}^{(1)} = (E2_{m+1,n}^* G1_{m+1,n}^* - E1_{m+1,n}^* G2_{m+1,n}^*) \Delta_{m+1,n}^* \quad (50a)$$

$$P_{m+1,n}^{(2)} = (E1_{m+1,n}^* C2_{m+1,n}^* - E2_{m+1,n}^* C1_{m+1,n}^*) \Delta_{m+1,n}^* \quad (50b)$$

$$P_{m+1,n}^{(3)} = (E1_{m+1,n}^* F2_{m+1,n}^* - E2_{m+1,n}^* F1_{m+1,n}^*) \Delta_{m+1,n}^* \quad (50c)$$

$$Q_{m+1,n}^{(1)} = (B1_{m+1,n}^* G2_{m+1,n}^* - B2_{m+1,n}^* G1_{m+1,n}^*) \Delta_{m+1,n}^* \quad (50d)$$

$$Q_{m+1,n}^{(2)} = (B2_{m+1,n}^* C1_{m+1,n}^* - B1_{m+1,n}^* C2_{m+1,n}^*) \Delta_{m+1,n}^* \quad (50e)$$

$$Q_{m+1,n}^{(3)} = (B2_{m+1,n}^* F1_{m+1,n}^* - B1_{m+1,n}^* F2_{m+1,n}^*) \Delta_{m+1,n}^* \quad (50f)$$

and

$$\Delta_{m+1,n}^* = \frac{1}{(B1_{m+1,n}^* E2_{m+1,n}^* - B2_{m+1,n}^* E1_{m+1,n}^*)} \quad (50g)$$

Next, equations (46) are rewritten as follows (where  $n = n + 1$ ):

$$F_{m+1,n} = P_{m+1,n}^{(1)} + P_{m+1,n}^{(2)} F_{m+1,n+1} + P_{m+1,n}^{(3)} \theta_{m+1,n+1} \quad (51a)$$

$$\theta_{m+1,n} = Q_{m+1,n}^{(1)} + Q_{m+1,n}^{(2)} F_{m+1,n+1} + Q_{m+1,n}^{(3)} \theta_{m+1,n+1} \quad (51b)$$

The "no-slip" boundary condition ( $F_{m+1,1} = 0$ ) is applied at the wall boundary to obtain the values of  $P_{m+1,1}^{(i)}$  where  $i = 1, 2, 3$ ; that is,

$$P_{m+1,1}^{(1)} = P_{m+1,1}^{(2)} = P_{m+1,1}^{(3)} = 0 \quad (52)$$

The thermal condition at the wall boundary can be specified in one of two ways: (1) specified wall-temperature distribution ( $KODWAL = 1$ ); or (2) specified heat-transfer distribution ( $KODWAL = 2$ ). For a specified wall-temperature distribution it can be seen directly from equation (51b) that

$$\left. \begin{array}{l} Q_{m+1,1}^{(1)} = \theta_{m+1,1} \\ Q_{m+1,1}^{(2)} = Q_{m+1,1}^{(3)} = 0 \end{array} \right\} \quad (53)$$

The case in which a heat-transfer distribution is specified presents a somewhat more difficult problem; however, this class of flows is often of interest; for example, adiabatic flows where  $q_w^* = 0$ .

The heat transfer at the wall boundary can be written in the transformed plane as follows (see ref. 3):

$$q_{m+1,1}^* = -\frac{\mu_r^* u_r^* 2 \sqrt{N_{Re,r}}}{L_r^*} \left( \frac{\rho_e u_e T_e \mu_e r_o^j}{N_{Pr} \sqrt{2\xi}} \right)_{m+1,N} l_{m+1,1} \left( \frac{\partial \theta}{\partial \eta} \right)_{m+1,1} \quad (54)$$

Then, for a specified value of  $q_{m+1,1}^*$ , the gradient of  $\theta$  can be obtained directly as follows:

$$\left( \frac{\partial \theta}{\partial \eta} \right)_{m+1,1} = -q_{m+1,1}^* \frac{L_r^*}{\mu_r^* u_r^* 2 \sqrt{N_{Re,r}}} \left( \frac{N_{Pr} \sqrt{2\xi}}{\rho_e u_e T_e \mu_e r_o^j} \right)_{m+1,N} \left( \frac{1}{l} \right)_{m+1,1} \quad (55)$$

For the grid-point spacing used in program VGBLP, the gradient of  $\theta$  evaluated at the wall, by using a three-point relation, is as follows:

$$\left( \frac{\partial \theta}{\partial \eta} \right)_{m+1,1} = \frac{[1 - (1 + k)^2] \theta_{m+1,1} + (1 + k)^2 \theta_{m+1,2} - \theta_{m+1,3}}{k(1 + k) \Delta \eta_1} \quad (56)$$

Equations (55) and (56) then yield the following expression for  $\theta_{m+1,1}$ :

$$\theta_{m+1,1} = \frac{k(1 + 1) \Delta \eta_1}{1 - (1 + k)^2} \left( \frac{\partial \theta}{\partial \eta} \right)_{m+1,1} - \frac{(1 + k)^2}{1 - (1 + k)^2} \theta_{m+1,2} + \frac{1}{1 - (1 + k)^2} \theta_{m+1,3} \quad (57)$$

where  $\left( \frac{\partial \theta}{\partial \eta} \right)_{m+1,1}$  is evaluated from equation (55). Equations (45) are next written at the  $m+1,2$  point to obtain two equations in terms of  $F_{m+1,n}$  and  $\theta_{m+1,n}$  where

$n = 1, 2, 3$ . (Note that  $F_{m+1,1} = 0$ .) The quantity  $F_{m+1,3}$  is then eliminated from these two equations to obtain one equation in terms of  $F_{m+1,2}$  and  $\theta_{m+1,n}$  where  $n = 1, 2, 3$ . The quantity  $\theta_{m+1,3}$  is next eliminated through use of equation (57) to obtain the relation

$$\theta_{m+1,1} = \bar{Q}_{m+1,1}^{(1)} + \bar{Q}_{m+1,1}^{(2)} F_{m+1,2} + \bar{Q}_{m+1,1}^{(3)} \theta_{m+1,2} \quad (58)$$

where

$$\bar{Q}_{m+1,1}^{(1)} = \frac{[(C2)(G1) - (C1)(G2)]_{m+1,2} + [(C2)(F1) - (C1)(F2)]_{m+1,2} [k(1+k)\Delta n_1] \left(\frac{\partial \theta}{\partial n}\right)_{m+1,1}}{\Delta_{m+1,2}} \quad (59a)$$

$$\bar{Q}_{m+1,1}^{(2)} = \frac{[(C1)(B2) - (C2)(B1)]_{m+1,2}}{\Delta_{m+1,2}} \quad (59b)$$

$$\bar{Q}_{m+1,1}^{(3)} = \frac{[(C1)(E2) - (C2)(E1)]_{m+1,2} + [(C1)(F2) - (C2)(F1)]_{m+1,2} (1+k)^2}{\Delta_{m+1,2}} \quad (59c)$$

and

$$\Delta_{m+1,2} = \left\{ [(C2)(D1) - (C1)(D2)] + [(C2)(F1) - (C1)(F2)] [1 - (1+k)^2] \right\}_{m+1,2} \quad (59d)$$

By comparing equations (51b) and (58), it is observed that

$$Q_{m+1,1}^{(i)} = \bar{Q}_{m+1,1}^{(i)} \quad (i = 1, 2, 3) \quad (60)$$

which completes the desired boundary condition for the case of a specified heat-transfer distribution along the wall boundary. The temperature at the wall is obtained from equation (57) once  $\theta_{m+1,2}$  and  $\theta_{m+1,3}$  are known.

The quantities  $P_{m+1,n}^{(i)}$  and  $Q_{m+1,n}^{(i)}$  where  $i = 1, 2, 3$  (see eqs. (51)) must first be determined across the boundary layer at the  $m+1$  station where  $n = 1, 2, \dots, N$ . These quantities are calculated by the following procedure:

- (1) Perform the following steps at the first grid point away from the wall ( $n = 2$ ):

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- (a) Calculate  $A_{12}, B_{12}, \dots, G_{12}$  from equations (B3)
- (b) Calculate  $A_{22}, B_{22}, \dots, G_{22}$  from equations (B4)
- (c) Using the results from steps (a) and (b) and the boundary conditions (eqs. (52) and (53) or (59)), calculate  $B_{12}^*, B_{22}^*, E_{12}^*, E_{22}^*, G_{12}^*$ , and  $G_{22}^*$  from equations (48)
- (d) Using the results from steps (a) to (c), calculate  $P_2^{(i)}$  and  $Q_2^{(i)}$  where  $i = 1, 2, 3$  from equations (50)

(2) The procedure outlined in step (1) is now repeated at the second grid point off the wall ( $n = 3$ ) by using the results obtained at  $n = 2$ . This procedure is repeated until the entire boundary layer is traversed ( $n = N$ ) and all values of  $P_{m+1,n}^{(i)}$  and  $Q_{m+1,n}^{(i)}$  are determined where  $i = 1, 2, 3$  and  $n = 2, 3, 4, \dots, N$ .

(3) Using the values of  $P_{m+1,n}^{(i)}$  and  $Q_{m+1,n}^{(i)}$  where  $i = 1, 2, 3$  and  $n = 2, 3, 4, \dots, N$ , the values of  $F_{m+1,n}$  and  $\theta_{m+1,n}$  where  $n = N-1, N-2, \dots, 2$  are calculated from equations (49). It should be noted that  $F_{m+1,N}$  and  $\theta_{m+1,N}$  are specified edge boundary conditions (eqs. (34b)). The wall-boundary values of  $F$  and  $\theta$  are obtained from equations (34a), or from equation (57) for the case of a specified wall-boundary heat-transfer distribution. At this point in the procedure, the values of  $F_{m+1,n}$  and  $\theta_{m+1,n}$  are known for  $n = 1, 2, \dots, N$ , and it remains only to determine  $V_{m+1,n}$  for all values of  $n$  to complete the first iteration.

(4) The continuity equation (eq. (27)) is solved numerically for the  $N - 1$  unknown values of  $V_{m+1,n}$  as follows:

$$V_{m+1,n} = V_{m+1,1} - \int_0^{\eta_n} \left( 2\xi \frac{\partial F}{\partial \xi} + F \right)_{m+1} d\xi \quad (61)$$

where  $V_{m+1,1}$  represents the wall-boundary condition  $V_w$ . (See eq. (35).) The trapezoidal rule of integration is used to numerically solve equation (61).

(5) The solution is now checked for convergence where the convergence criterion is as follows ( $q$  is iteration index):

$$DIF = \left| 1 - \frac{(\partial F / \partial \eta)^q}{(\partial F / \partial \eta)^{q-1}} \right|_{m+1,1} \quad (62)$$

If  $DIF \leq CONV$ , station  $m+1$  is declared converged and  $m$  is incremented by 1. During the development of program VGBLP, a global convergence check was initially applied to each of the three dependent variables over all values of  $n$ . Global convergence was declared once all three variables were converged over all values of  $n$ ; however, it was observed numerically that a local check on the gradient of  $F$  at the wall was a sufficiently accurate criterion. Consequently, the logic and storage requirements for the global check were removed from the software.

### Initial Profiles

A major change in the present approach compared with that of references 3 and 4 is the technique for numerically generating the initial profiles at  $\xi = 0$ . These initial values are required to initiate the three-point implicit marching procedure. In references 3 and 4, the equations at the initial station ( $\xi = 0$ ) were numerically solved using a fourth-order Runge-Kutta scheme for an equally spaced grid ( $\Delta\eta = \eta_{\max}/(N - 1)$ ) in the  $\eta$ -direction. The converged solution on the equally spaced grid was then interpolated onto the variably spaced grid ( $\Delta\eta_i = k \Delta\eta_{i-1}$ ). This procedure introduced some interpolation error into the initial profiles which, although decaying in  $\xi$ , could cause oscillations in the neighborhood of the stagnation point for blunt-body flows. These oscillations, if they occurred, made it difficult to accurately determine parameters such as  $\lim_{s \rightarrow 0} q_w$  and  $\lim_{s \rightarrow 0} T_w$ . Another problem sometimes encountered by users of the approach presented in reference 4 was the sensitivity of the convergence of the initial solution to the selected initial values

for  $\frac{\partial F}{\partial \eta}\Big|_{\eta=0}$  and  $\frac{\partial \Theta}{\partial \eta}\Big|_{\eta=0}$  required to initiate the Runge-Kutta integration. To ensure convergence, the user would often have to make several trial runs before the initial guesses were sufficiently close to the converged values.

In the present approach these two problems (interpolation and convergence) are completely eliminated. The locally similar form of the momentum and energy equations is numerically solved in finite-difference form for the variable grid used in the marching procedure. Initial value guesses and interpolation procedures are not required. The momentum and energy equations are of tridiagonal form and are easily solved. The continuity equation is uncoupled from the system and solved using the trapezoidal rule of integration. The initial profiles are generated in subroutine SIMILAR.

The marching procedure requires evaluation of the  $\xi$ -derivatives at two backward points; consequently, the first solution station SS(1) + SS(2) in the  $\xi$ -coordinate requires special attention to assure local accuracy in the neighborhood of the stagnation point. For flows with a stagnation point (IBODY = 1), the profiles at  $\xi = \Delta\xi_1$  are reflected about the stagnation point to impose symmetry. For flows without a stagnation point (IBODY = 2), it is assumed that the solution at  $\xi = \Delta\xi_1$  is identical to that at  $\xi = 0$  ( $s = 0$ ). As a result of this approach, the solutions are physically correct and merge smoothly with the downstream marching solution ( $\xi > \Delta\xi_1$ ). The quantity  $\Delta\xi_1$  is evaluated using Simpson's rule for stagnation-point flows.

### Evaluation of Wall Derivatives

The shear stress and heat transfer at the wall are directly proportional to the gradient of  $F$  and  $\Theta$  evaluated at the wall, respectively. By using  $G$  to represent a general quantity, where  $G_{m+1,1}$  is the value of  $G$  at  $m+1$  evaluated at the wall, the four-point difference scheme used to evaluate derivatives at the wall is given as

$$\left(\frac{\partial G}{\partial \eta}\right)_{m+1,1} = Y_7 G_{m+1,1} + Y_8 G_{m+1,2} + Y_9 G_{m+1,3} + Y_{10} G_{m+1,4} \quad (63)$$

where the coefficients are defined by the following relations:

$$Y_7 = -\frac{(1 + k + k^2)^2 [k(1 + k) - 1] + (1 + k)}{(1 + k)(1 + k + k^2)k^3 \Delta\eta_1} \quad (64a)$$

$$Y_8 = \frac{(1 + k + k^2)}{k^2 \Delta\eta_1} \quad (64b)$$

$$Y_9 = -\frac{(1 + k + k^2)}{(1 + k)k^3 \Delta\eta_1} \quad (64c)$$

and

$$Y_{10} = \frac{1}{(1 + k + k^2)k^3 \Delta\eta_1} \quad (64d)$$

For the case of equally spaced grid points in the  $\eta$ -direction ( $k = 1$ ), equation (63) reduces to the familiar four-point relation:

$$\left(\frac{\partial G}{\partial \eta}\right)_{m+1,1} = -\frac{1}{6 \Delta\eta} (11G_{m+1,1} - 18G_{m+1,2} + 9G_{m+1,3} - 2G_{m+1,4}) \quad (65)$$

#### PROGRAM DESCRIPTION

Program VGBLP is run on the Control Data CYBER 170 series computers under the NOS 1.4 operating system at the Langley Research Center.

#### Array Dimensions

Program VGBLP and subroutines TABLE, VARENT, TURBLNT, MESH, SIMILAR, and SOLVE use the variable-dimension capability of the preprocessor at the Langley Research Center. This capability allows the user to designate the minimum storage requirements for a given problem. If the preprocessor capability is not available at the user's installation, the dimension statements can be modified by inserting the required dimensions in place of their equivalent designations (UPDATE, MODIFY, etc.) in accordance with the following definitions for program VGBLP and its subroutines.

#### Program VGBLP

##### Variable dimension

##### Assigned value

JI

1 - (KODPRT  $\neq$  3); NUMBL - (KODPRT = 3)

JK

IE + 2

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JL	1 - (constant entropy); IEND1 - (variable entropy)
JM	INTEGER ( $s_{max}/PRNTINC + IPRNT$ )
JN	INTEGER ( $s_{max}/PROINC + IPRO$ )
JH	IEND1 + 1

Subroutine TABLE

JH	See definition in VGBLP
JJ	NUMBER

Subroutine VARENT

JL	See definition in VGBLP
----	-------------------------

Subroutine TURBLNT

JI	See definition in VGBLP
JK	See definition in VGBLP

Subroutines MESH, SIMILAR, SOLVE

JK	See definition in VGBLP
----	-------------------------

Input Description

Standard CDC NAMELIST is used for all data input. Program VGBLP reads input under \$NAM1. Subroutine TABLE reads input under \$NAM2. For cases where the variable entropy option is required (IENTRO = 2), subroutine VARENT reads input under \$NAM3.

Input/output flexibility is provided to the user wherein either the International System of Units (SI, KODUNIT = 1) or the U.S. Customary Units (U.S., KODUNIT = 0) can be used. The required input and resulting output data are listed in the following sections with appropriate dimensional units. The SI Units are listed first, followed by U.S. Units in parentheses. If no units are listed, the quantity is nondimensional.

Input data for \$NAM1.-

<u>Variable name</u>	<u>Variable description</u>
CONV	Convergence criterion for boundary-layer solution; DEFAULT = $1 \times 10^{-4}$
CONVE	Convergence criterion for variable entropy iteration; DEFAULT = $1 \times 10^{-2}$
DETA1	$\Delta\eta_1$ (see fig. 1)

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FT	1.0 - nonsimilar solution; 0.0 - locally similar solution; DEFAULT = 1.0
G	$\gamma$ ; DEFAULT = 1.4
GLAR	$y/\delta$ array corresponding to PRTAR array, used only if KODPRT = 3; NUMBL values
IBODY	1 - flows with stagnation point; 2 - flows without stagnation point
IE	Number of mesh points in $\eta$ -coordinate
IEND1	Number of steps in S-direction $S_{\max} = \sum_{m=1}^{IEND1} SS(m) \text{ where } SS(1) = 0$
IENTRO	1 - constant entropy; 2 - variable entropy; DEFAULT = 1
IGAS	1 - Sutherland's viscosity (see eq. (7a)); 2 - power-law viscosity (see eq. (7b)); DEFAULT = 1
IGEOM	1 - specify XEND, IE, XK; 2 - specify XEND, IE, DETA1
IPRNT	Number of specified wall-value printouts desired other than those determined by PRNTINC; DEFAULT = 0
IPRO	Number of specified profile printouts desired other than those determined by PROINC; DEFAULT = 0
ITMAX	Maximum number of iteration cycles, $1 \leq m \leq IEND1$ , for variable-entropy calculations; DEFAULT = 3
IYINT	1 - normal intermittency function, $\bar{\gamma}$ set to 1.0; 2 - normal intermittency function, $\bar{\gamma}$ calculated from equation (17c); DEFAULT = 1
J	j; 0 - two-dimensional; 1 - axisymmetric
KODAMP	1 - local values used in equation (5b) for damping; 2 - wall values used in equation (5b) for damping; DEFAULT = 2
KODE	1 - both laminar and turbulent profile prints are desired for diagnostic reasons once flow is turbulent; 0 - otherwise; DEFAULT = 0
KODPRT	1 - constant $N_{Pr,t}$ ; 2 - Rotta distribution (see eq. (21)); 3 - tabular, $N_{Pr,t} = f(y/\delta)$ ; DEFAULT = 1

KODUNIT	0 - all dimensional input and output in U.S. Units; 1 - all dimensional input and output in SI Units; DEFAULT = 0
KODVIS	1 - mixing-length model; 2 - two-layer eddy-viscosity model; DEFAULT = 2
KODWAL	1 - specified wall temperature distribution; 2 - specified wall heat-transfer distribution; DEFAULT = 1
KTCOD	1 - transition extent calculated from equation (37); 2 - transition extent specified as TLNGTH; DEFAULT = 2.0
NAUXPRO	1 - auxiliary profile prints are desired (see output description); 2 - otherwise; DEFAULT = 2.0
NITMAX	Maximum number of iterations allowed at any given station; DEFAULT = 1
NUMBL	Number of values read into PRTAR and GLAR arrays if KODPRT = 3
PHII	Opening angle of body at $s = 0$ , $\tan^{-1} \left( \frac{ds}{dz} \right)_{s=0}$ , deg
PR	$N_{Pr}$ ; DEFAULT = 0.72
PRNTINC	Incremental $s^*$ -value for which wall-value printouts will be made, m (ft); DEFAULT = 0.1
PRNTVAL	Array of IPRNT specified $s^*$ -values for which wall-value printouts are desired, m (ft)
PROINC	Incremental $s^*$ -value for which profile printouts will be made, m (ft); DEFAULT = 1.0
PROVAL	Array of IPRO specified $s^*$ -values for which profile printouts are desired, m (ft)
PRT	$N_{Pr,t}$ ; DEFAULT = 0.95
PRTAR	$N_{Pr,t}$ array, used only if KODPRT = 3; NUMBL values
PT1	$P_{t,\infty}^*$ , Pa ( $lb/ft^2$ )
R	$R_g^*$ , gas constant (eq. (6)), $m^2/(s^2-K)$ ( $ft^2/(s^2-O_R)$ ); DEFAULT = $1716\ ft^2/(s^2-O_R)$
SMXTR	Critical-vorticity Reynolds number; DEFAULT = $1 \times 10^8$

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SST	$s^*$ -location of transition, $s_{t,i}$ , m (ft); DEFAULT = $1 \times 10^8$
TLNGTH	$s_{t,f}/s_{t,i}$ , transition extent (see fig. 2); DEFAULT = 2.0
TTL	$T_{t,\infty}^*$ , K ( $^{\circ}$ R)
VELEDG	Value of F to be used in defining edge of boundary layer; DEFAULT = 0.995
VIS1C1	$a_1^*$ (see eq. (7a)), Pa-s ( $\text{lb}\cdot\text{s}/\text{ft}^2$ ); DEFAULT = $2.27 \times 10^{-8}$ $\text{lb}\cdot\text{s}/\text{ft}^2$
VIS1C2	$a_2^*$ (see eq. (7a)), K ( $^{\circ}$ R); DEFAULT = 198.6 $^{\circ}$ R
VIS2C1	$a_3^*$ (see eq. (7b)), Pa-s ( $\text{lb}\cdot\text{s}/\text{ft}^2$ )
VIS2C2	$a_4$ (see eq. (7b))
W	0 - neglect transverse curvature; 1 - include transverse curvature; DEFAULT = 0
WAVE	$\theta_s^* _{s=0}$ , shock-wave angle at $s = 0$ (see fig. 2), deg
XEND	$n_{\max}$ (see fig. 1)
XK	k, constant in geometric progression (see eq. (42))
XMA	$M_{\infty}$
XT1	$k_1$ (see eq. (16a)); DEFAULT = 0.4
XT2	$k_2$ (see eq. (16b)); DEFAULT = 0.0168
XT3	$k_3$ (see eq. (17c)); DEFAULT = 5.0
XT4	$k_4$ (see eq. (17c)); DEFAULT = 0.78
XT5	$k_5$ (see eq. (20b)); DEFAULT = 0.108
XT6	$A^+$ , damping function; DEFAULT = 26.0

Input data for \$NAM2.-

<u>Variable name</u>	<u>Variable description</u>
L	Order of interpolation to be used for \$NAM2 tables; DEFAULT = 1
NUMBER	Number of values read into \$NAM2 tables

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PE	Edge pressure-distribution array (NUMBER values), Pa (lb/ft <sup>2</sup> )
QW	Wall heat-transfer-distribution array (NUMBER values); KODWAL = 2, W/m <sup>2</sup> (Btu/ft <sup>2</sup> -s)
RMI	Body radial-coordinate array $r_o$ (NUMBER values), m (ft)
RVWALD	Wall mass-flux array $V_w$ (NUMBER values); DEFAULT = 0, Pa-s/m (lb-s/ft <sup>3</sup> )
S	S-station array (NUMBER values); independent variable for tabular input, m (ft)
SS	Array of incremental values between adjacent solu- tion stations ( $s_1^*$ , $s_2^*$ , ..., $s_{IEND1}^*$ ); step size can be arbitrary and not directly associated with the S-station array other than $IEND1$ $\sum_{m=1}^{IEND1} SS(I) = s_{max}^*$ ; the first two members of the array must be equal ( $SS(2) = SS(1)$ )
TW	Wall-temperature-distribution array (NUMBER values); KODWAL = 1, K (°R)
Z	Axial-coordinate array (NUMBER values), m (ft)

Input data for \$NAM3.-

<u>Variable name</u>	<u>Variable description</u>
NUMBER	Number of values read into \$NAM3 tables
RRS	Array of radial coordinates of shock wave (NUMBER values), m (ft)
ZZS	Array of axial coordinates of shock wave (NUMBER values), m (ft)

A unique relationship exists between the print control parameters (PROINC; PRNTINC; IPRO; IPRNT; PROVAL; PRNTVAL) and IEND1 in \$NAM1 and the SS array in \$NAM2. The potential user of program VGBLP should note that there are exactly IEND1 values in the SS array and that these values specify the solution-station locations along the s-coordinate. Also, a solution station must be located at the s-coordinate locations designated as print (profile or wall) stations. A failure to understand this relationship generally results in a computer run with no output. Consider the following input where the program user wishes to march the solution to  $s_{max} = 1.0$ :

```
SS = 10*.001, 99*.01  
IEND1 = 75  
  
PRNTINC = 0.201, PROINC = 0.501  
  
IPRO = 1, IPRNT = 1  
  
PROVAL = 0.751, PRNTVAL = 0.751
```

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Two errors have been made in the preceding input that will result in the program stopping at  $s = 0.66$  (instead of  $s = 1.0$ ) without any output (wall print or profile print). The two errors are as follows: (1) IEND1 is not equal to the number of values in the SS array; (2) the designated print locations do not agree with the solution stations designated by the SS array. An example of correct input is as follows:

```
SS = 10*.001, 99*.01  
IEND = 109  
  
PRNTINC = 0.2, PROINC = 0.5,  
  
IPRO = 1, IPRNT = 1,  
  
PROVAL = 0.75, PRNTVAL = 0.75
```

The program would now have a normal STOP at  $s = 1.0$  with wall prints at  $s = 0.2, 0.4, 0.6, 0.75, 0.8,$  and  $1.0$  and profile prints at  $s = 0.5, 0.75,$  and  $1.0.$  Finally, it should be noted that the SS array can be composed of completely arbitrary  $\Delta s$  values with the restriction  $SS(1) = SS(2),$  but to obtain output the user must specify print-control input corresponding to the location of the solution stations.

#### Intermediate Data Storage

The output ( $S, PE, RMI, TW, Z, DPEDS, RVWALD, DRDZ, QW$ ) required at station  $m+1$  generated in subroutine TABLE is written on TAPE 4. Program VGBLP reads this output just prior to obtaining the boundary-layer solution at station  $m+1.$  For cases where variable entropy is included ( $IENTRO = 2$ ), TAPE 4 is rewound at the end of the last computed station  $s_{max}$  to enable restart for the next variable-entropy iteration.

#### Output Description

Program VGBLP first prints namelist data for \$NAM1. Next, subroutine TABLE prints \$NAM2. If the case includes the effect of variable entropy ( $IENTRO = 2$ ), subroutine VARENT then prints \$NAM3 input. It should be noted that for many cases the user can take advantage of many of the DEFAULT values for \$NAM1 and \$NAM2.

Following the input data prints, the similar-solution profiles at the initial station ( $\xi = 0$ ) are printed as follows:

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<u>Variable name</u>	<u>Variable (see "Symbols")</u>
ETA	$\eta$
FZ	$\partial F / \partial n$
T/TE	$\Theta$
TZ	$\partial \Theta / \partial n$
U/UE	$F$
V	$V$
XL	$(\rho \mu) / (\rho \mu)_e$

The initial station parameters are then printed.

MUE	$\mu_e^*, \text{ Pa-s (lb-s/ft}^2)$
PE	$p_e^*, \text{ Pa (lb/ft}^2)$
QSD	$q_w^*, \text{ W/m}^2 \text{ (Btu/ft}^2\text{-s)}$
TE	$T_e^*, \text{ K (}^\circ\text{R)}$
UE	$u_e^*, \text{ m/s (ft/s)}$

The units used in input and expected as output for dimensional quantities are next declared as either SI or U.S. Customary.

Free-stream and reference variables are then printed.

AA1	$a_\infty^*, \text{ m/s (ft/s)}$
PREF	$\rho_r^* u_r^{*2}, \text{ Pa (lb/ft}^2)$
PTR	$p_{t,\infty}^* / (\rho_\infty u_\infty^2)$
PTI	$p_{t,\infty}^*, \text{ Pa (lb/ft}^2)$
P1	$p_\infty^*, \text{ Pa (lb/ft}^2)$
REY	$N_{Re,\infty}, \text{ m}^{-1} \text{ (ft}^{-1})$
RREF	$\rho_r^*, \text{ kg/m}^3 \text{ (lb-s}^2/\text{ft}^4)$
RT1	$\rho_{t,\infty}^*, \text{ kg/m}^3 \text{ (lb-s}^2/\text{ft}^4)$
R1	$\rho_\infty^*, \text{ kg/m}^3 \text{ (lb-s}^2/\text{ft}^4)$
TREF	$u_r^{*2} / c_p^*, \text{ K (}^\circ\text{R)}$
TTL	$T_{t,\infty}^*, \text{ K (}^\circ\text{R)}$

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T1	$T_{\infty}^*, \text{ K } (^{\circ}\text{R})$
UREF	$u_r^*, \text{ m/s } (\text{ft/s})$
U1	$u_{\infty}^*, \text{ m/s } (\text{ft/s})$
VISREF	$\mu_r^*, \text{ Pa-s } (\text{lb-s/ft}^2)$
XMA	$M_{\infty}$

The profile-print and wall-print stations are next printed in accordance with input specified in \$NAM1.

Laminar-profile

CROCCO	$\frac{T_t - T_w}{T_{t,e} - T_w}$
ETA	$\eta$
FZ	$\left( \frac{\partial F}{\partial \eta} \right)_{m+1,n}$
M/ME	$M/M_e$ , Mach number ratio
PT/PTR	$p_t/p_{t,r}$ , total pressure ratio
T/TE	$\Theta$
TT/TTE	$T_t/T_{t,e}$
TZ	$\left( \frac{\partial \Theta}{\partial \eta} \right)_{m+1,n}$
U/UE	$F$
VORTREY	$\chi_{m+1,n} = \left[ \frac{y^2}{v} \left( \frac{\partial \mu}{\partial y} \right) \right]_{m+1,n}$ , vorticity Reynolds number
XLM11	$\frac{(\rho \mu)_{m+1,n}}{(\rho \mu)_e}$
Y/YE	$y/y_e$

Additional values for transitional and turbulent profiles

UDEF	$\frac{u_e - u}{u_T}$
UPLUS	$\frac{u}{u_T}$
VISEFF	$1 + \frac{\epsilon}{\mu} \Gamma$ , effective viscosity parameter
YPLUS	$\frac{yu_T}{v}$

Auxiliary-profile values (NAUXPRO = 1)

DAMP	C	$\left[ 1 - \exp\left(-\frac{y}{A}\right) \right]_{m+1,n}$
EP		$\left(\frac{\varepsilon}{\mu}\right)_{m+1,n}$
EPl		$\left[\left(\frac{\varepsilon}{\mu}\right)_i\right]_{m+1,n}$ (see eq. (16a))
EP2		$\left[\left(\frac{\varepsilon}{\mu}\right)_o\right]_{m+1,n}$ (see eq. (16b))
FCl		$\left(\frac{\rho}{\mu} \left  \frac{\partial u}{\partial y} \right  \right)_{m+1,n}$
GRAD (U/UE)		$\frac{\partial F}{\partial \eta}$
GRAD (T/TE)		$\frac{\partial \Theta}{\partial \eta}$
MIXDEL		$\left(\frac{\zeta}{\delta}\right)_{m+1,n}$
V		V (see eq. (26))

Wall print

BETA	$\beta$ , pressure-gradient parameter (see eqs. (30))
CFE	$\frac{\tau_w}{\frac{1}{2} \rho_e u_e^2}$ , skin-friction coefficient based on edge condition
CFW	$\frac{\tau_w}{\frac{1}{2} \rho_w u_e^2}$ , skin-friction coefficient based on wall density
DLTAST	$\delta^*$ , displacement thickness, m (ft)
DPEDS	$\frac{dp_e}{ds}$ , pressure gradient
DSMXO	$\left( \frac{\partial X_{max}}{\partial s} \right)_{m+1}$
DTEDS	$\frac{dT_e}{ds}$ , temperature gradient

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DUEDS	$\frac{du_e}{ds}$ , velocity gradient
ERROR	value of DIF at convergence (see eq. (62))
FORM	$\frac{\delta^*}{\theta}$
HD	$\frac{q_w}{T_w - T_{aw}}$ , heat-transfer coefficient, $\text{W/m}^2\text{-K}$ (Btu/ft <sup>2</sup> -s-°R)
ITRO	number of iterations performed for variable entropy
ME	$M_e$ , edge Mach number
MUE	$\mu_e$ , Pa-s (lb-s/ft <sup>2</sup> )
NOITER	number of iterations required for convergence
NSTE	$\frac{h}{c_p(\rho u)_e}$ , Stanton number based on edge condition
NSTW	$\frac{h}{c_p \rho_w u_e}$ , Stanton number based on wall condition
NUE	Nusselt number based on edge condition
NUW	Nusselt number based on wall condition
OMEGA	$\left( \frac{\rho_r u_r L_r}{\mu_r} \right)^{-1/2}$
PE	$p_e$ , edge pressure, Pa (lb/ft <sup>2</sup> )
P20	$\frac{p_{t,e}}{\rho_r u_r^2}$
QSD	$q_w$ , heat transfer, $\text{W/m}^2$ (Btu/ft <sup>2</sup> -s)
RE	$\rho_e$ , edge density, $\text{kg/m}^3$ (lb-s <sup>2</sup> /ft <sup>4</sup> )
REDELT	$\frac{\rho_e u_e \delta^*}{\mu_e}$ , Reynolds number based on local displacement thickness
RES	$\frac{\rho_e u_e s}{\mu_e}$ , local Reynolds number

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RETHET	$\frac{\rho_e u_e \theta}{\mu_e}$ , Reynolds number based on local momentum thickness
RFTRUE	$\frac{T_{aw} - T_e}{T_t - T_e}$ , recovery factor
RMI	$r_o$ , body radius (see fig. 2), m (ft)
ROUSE	$\chi_{max} = \left[ \left( \frac{y^2}{v} \frac{\partial u}{\partial y} \right)_{m+1, n} \right]_{max}$
RSHK	local radius of shock wave, m (ft)
RVWAL	$(\rho v)_w / (\rho u)_e$
RVWALD	$(\rho v)_w$ , dimensional mass flux at wall, Pa-s/m (lb-s/ft <sup>3</sup> )
S	s, boundary-layer coordinate (see fig. 2), m (ft)
SWANG	local shock-wave angle, deg
TAUD	$\tau_w$ , wall shear stress, Pa (lb/ft <sup>2</sup> )
TE	$T_e$ , edge temperature, K ( $^oR$ )
THETA	$\theta$ , momentum thickness, m (ft)
TRFCT	$\Gamma$ , intermittency distribution (see eq. (38))
TW/TTL	$\frac{T_w}{T_{t,\infty}}$
UE	$u_e$ , edge velocity, m/s (ft/s)
UTAU	$u_T = \sqrt{\frac{T_w}{\rho}}$ , m/s (ft/s)
VW	$v_{m+1, l}$
XAL	$(\gamma - 1) M_e^2$
XI	$\xi$
YE	$\delta_e$ , boundary-layer thickness, m (ft)
YMP	n-value at $y_m$
Z	z, axial coordinate of body (see fig. 2), m (ft)
ZSHK	axial coordinate of shock wave, m (ft)

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Flow charts and listings for program VGBLP and its subroutines are presented in appendix C.

SAMPLE CASES

A range of test cases is presented as guides for assisting users of program VGBLP in their own specific applications. Five major test cases are presented that include external and internal flows, flows with wall-mass transfer, flows where transverse-curvature effects are important, and flows where variable-entropy effects must be included. For each test case presented, the following information is given: (1) schematic of geometry; (2) boundary conditions; (3) all input data including variable dimension specification; (4) samples of output (see appendix D); and (5) plots of selected results. It is suggested that users compute two or more of the test cases prior to applying program VGBLP to their own particular problem. This approach is beneficial in that it (1) confirms that the software has been correctly implemented on the user's computer system and (2) provides experience in using the program and specifying the correct input data; however, the user need not understand the algorithm in order to successfully apply program VGBLP. The first test case, flat-plate flows, is especially useful in developing experience with the grid specification and control.

Test Case No. 1

This case represents the simplest class of flow that is usually encountered. The flat-plate boundary layer need not be similar; for example, turbulent flow, arbitrarily distributed wall-mass transfer, arbitrary heat transfer, or externally imposed pressure gradients result in nonsimilar boundary-layer development.

For the present case, the test conditions of reference 22 are selected. A schematic of the model, including flow conditions and numerical results, is presented in figure 3. The input and sample output are presented in appendix D. Comparisons

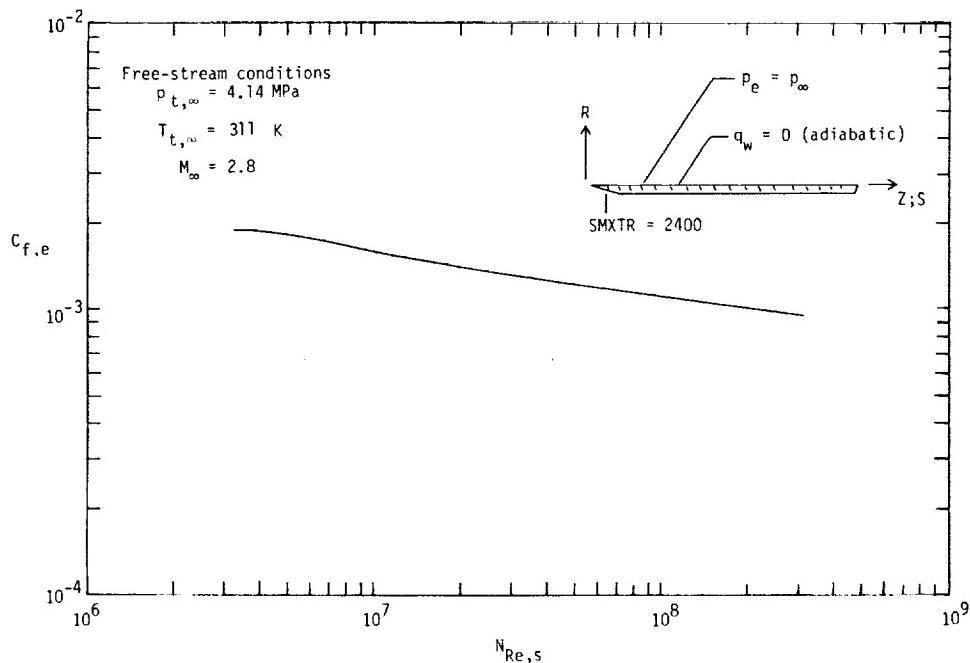


Figure 3.- Test case no. 1.

of numerical results with the experimental data of reference 22 are presented in reference 3. A grid refinement study showing the order of accuracy of the numerical approach is presented in reference 20.

#### Test Case No. 2

This test case is for the flow past a waisted-afterbody configuration (ref. 23). Transverse-curvature terms must be included; also, the flow is supersonic with an attached shock wave. A schematic of the model, flow conditions, and typical numerical results are presented in figure 4. The input and sample output are presented in appendix D. Comparisons of the numerical results with experimental data are presented in reference 3.

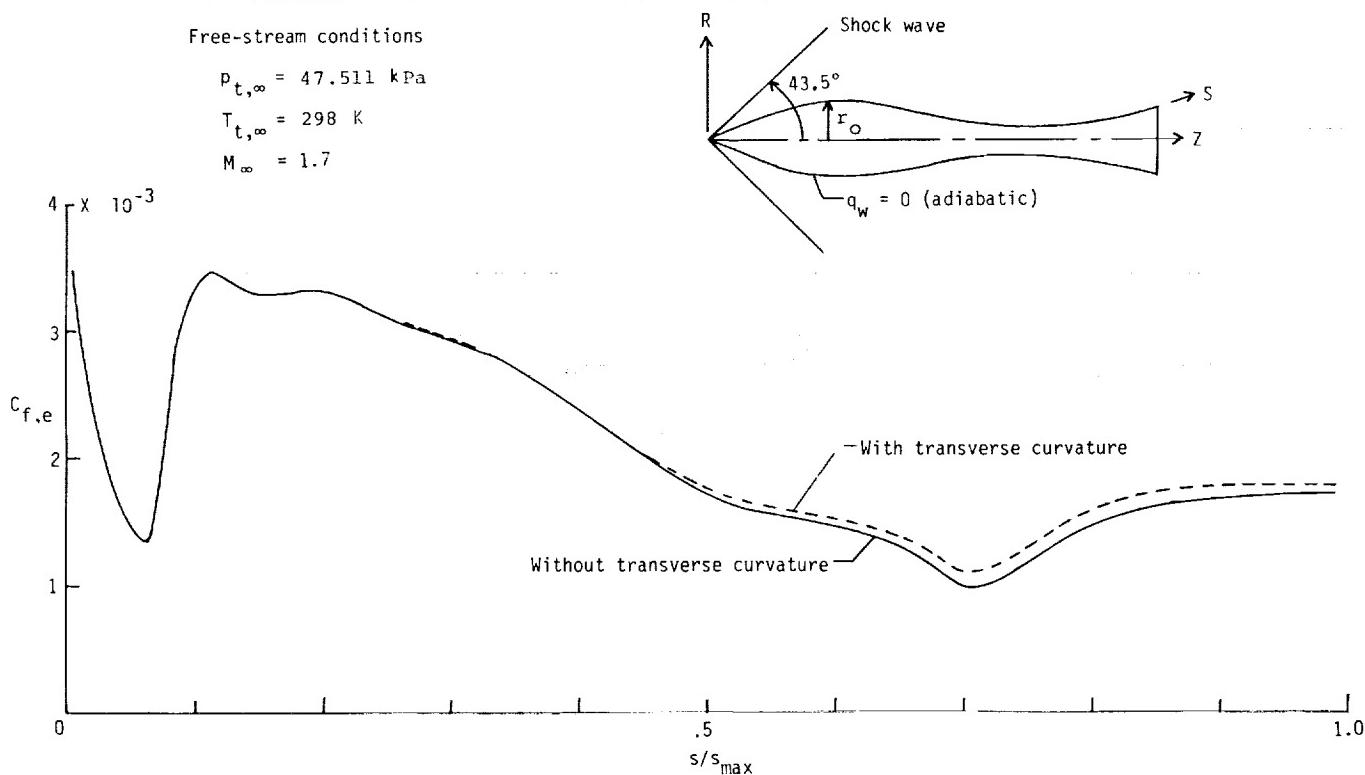


Figure 4.- Test case no. 2; skin-friction coefficient.

The pressure distribution was taken directly from the experimental data (ref. 23). Results for two calculations are presented: (1) without transverse-curvature (TVC) terms; (2) with TVC terms. This particular configuration is an example of a body where the boundary-layer coordinate  $s$  cannot be expressed as an explicit function of the body-coordinate system  $R, Z$ , and as such must be obtained by numerical integration. In the previous example for flat-plate flow, this presented no difficulty since  $S$  and  $Z$  were congruent. It is suggested that the user of program VGBLP develop software to numerically generate the  $s$ -coordinate from a specified body-coordinate system and to interpolate edge-pressure and wall-boundary data, often specified as a function of the body-coordinate system, to the  $S, R$ -coordinate system.

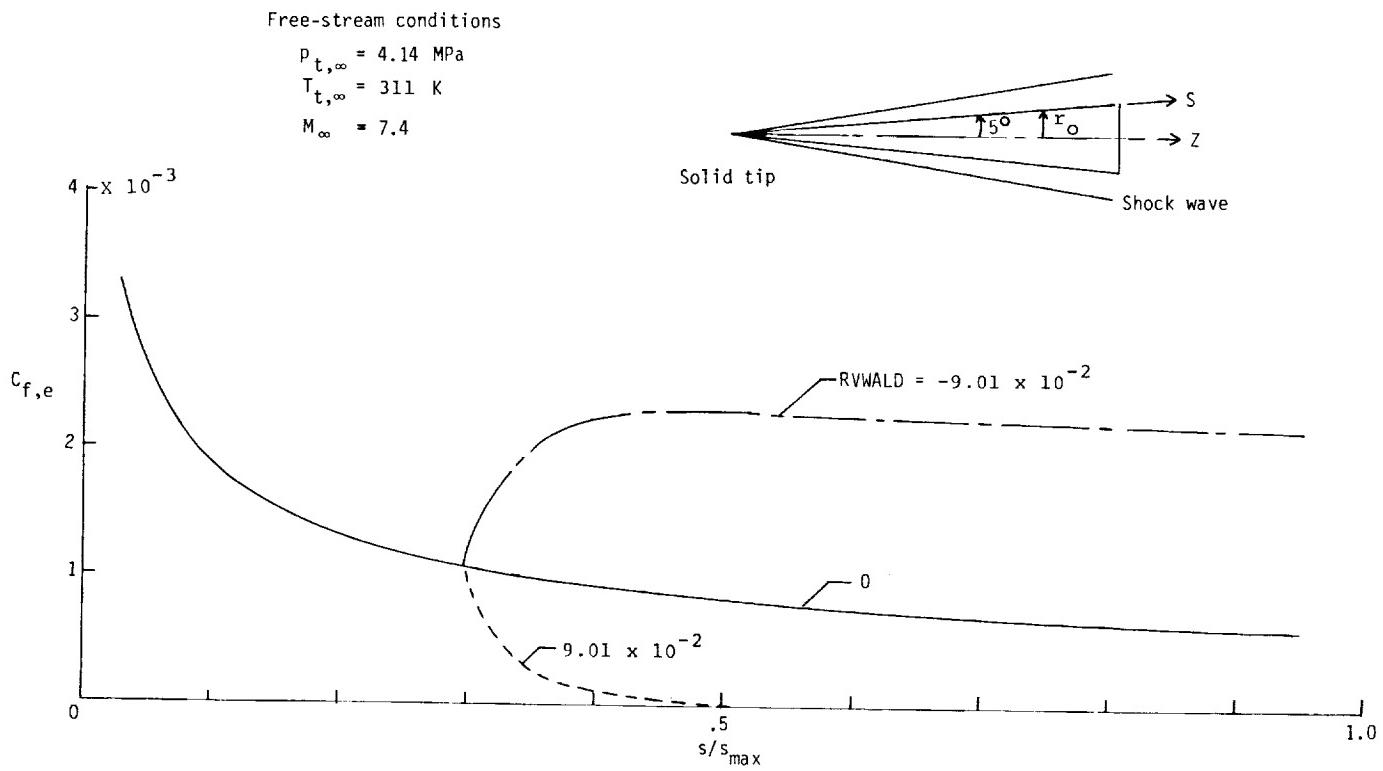
The trapezoidal rule is sufficiently accurate and can be easily implemented to integrate the following relationship:

$$s = s_0 + \int_0^z \sqrt{1 + \left(\frac{dr_o}{dz}\right)^2} dz \quad (66)$$

#### Test Case No. 3

Flows with wall-mass transfer are often encountered and can be efficiently solved by program VGBLP. The sample case selected is that of reference 24 for laminar boundary-layer flow. A schematic of the model, including flow conditions and numerical results, is presented in figure 5. The required input and sample output are presented in appendix D. It should be noted that program VGBLP can be applied to turbulent flow with wall-mass transfer if the user modifies the  $A^+$  definition in subroutine TURBLNT. (See ref. 2.)

The numerical results for three wall-mass transfer boundary conditions are presented in figure 5: (1)  $(\rho v)_w < 0$  (suction); (2)  $(\rho v)_w = 0$  (solid wall); and (3)  $(\rho v)_w > 0$  (transpiration). The input and sample output are presented in appendix D. Comparisons of the numerical results with experimental data are presented in reference 3. It should be noted that program VGBLP is not limited to fixed values of  $(\rho v)_w^*$ ; that is,  $(\rho v)_w^* = g(s)$  can be input in \$NAM2 if required.



(a) Skin-friction coefficient.

Figure 5.- Test case no. 3.

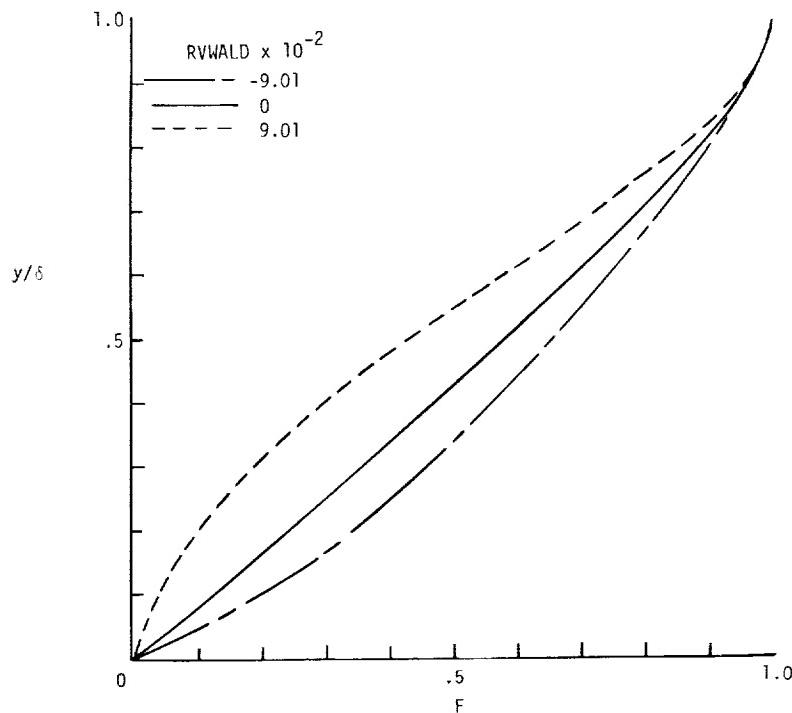
(b) Velocity profiles;  $s = 0.100$  m.

Figure 5.- Concluded.

## Test Case No. 4

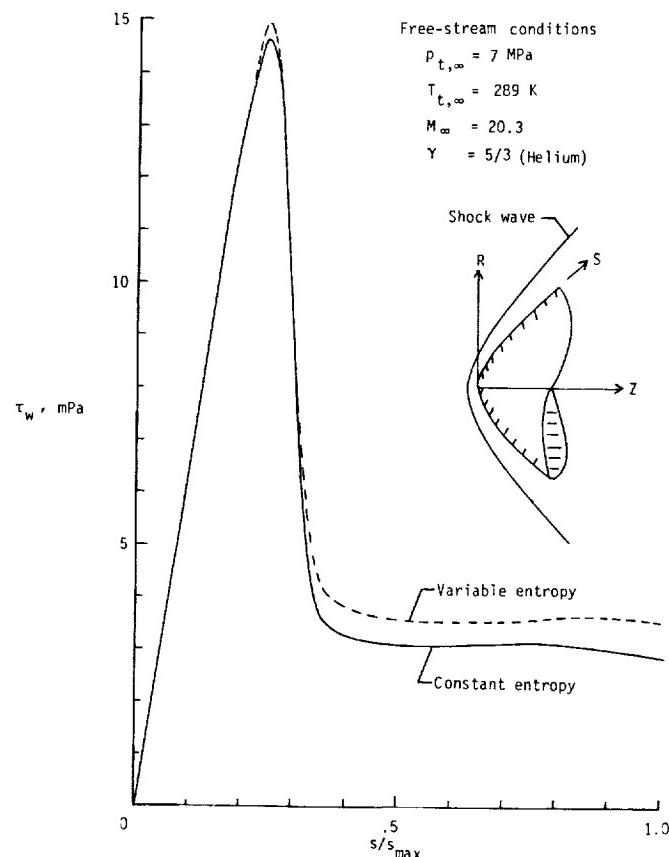
For hypersonic, blunt-body flows, the effect of variable entropy introduced by the bow shock wave can significantly affect the boundary-layer development. As an example, the flow over a  $45^\circ$  spherically blunted cone in helium flow is considered. (See ref. 25.) A schematic of the model, including flow conditions and numerical results, is presented in figure 6. Experimental pressure data, supplied by the authors of reference 25, were used as input. The shock-wave data were obtained from figure 7(d) of reference 25. The input and sample output are presented in appendix D.

## Test Case No. 5

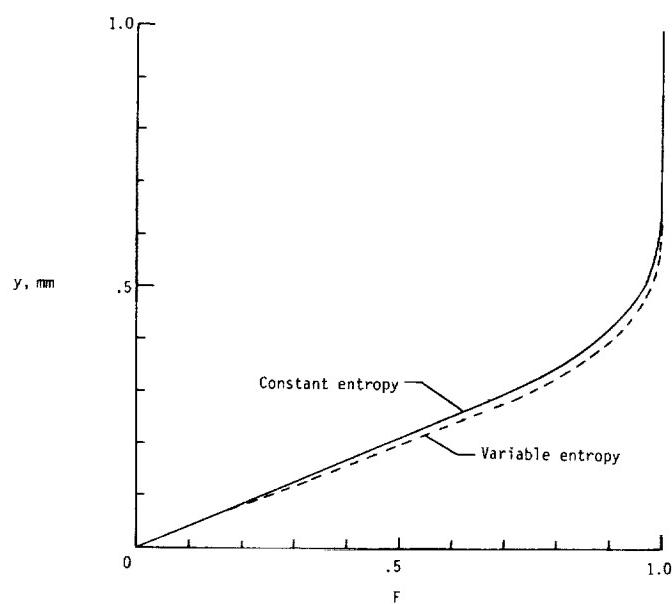
Boundary-layer solutions are usually required for the design and analysis of nozzle flows. A typical wind-tunnel design case (see ref. 26) is presented in figure 7. It should be noted that the solution for this case is initiated in the stagnation chamber and marched downstream to the nozzle exit. The input and sample output are presented in appendix D. Extensive comparisons of the numerical results with experimental data are presented in reference 26.

Nozzle flows are typical of the more difficult applications of boundary-layer theory because of the large variation of pressure gradient  $dP_e/ds$  as the solution proceeds from the settling chamber through the sonic throat and into the supersonic region of the nozzle. The thinning effect of the pressure gradient on the boundary-layer thickness in the throat region of the nozzle necessitates care in selecting the grid distribution in the normal-coordinate as well as the marching-coordinate direction.

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(a) Shear stress.



(b) Velocity profiles;  $s = 0.0495 \text{ m}$ .

Figure 6.- Test case no. 4.

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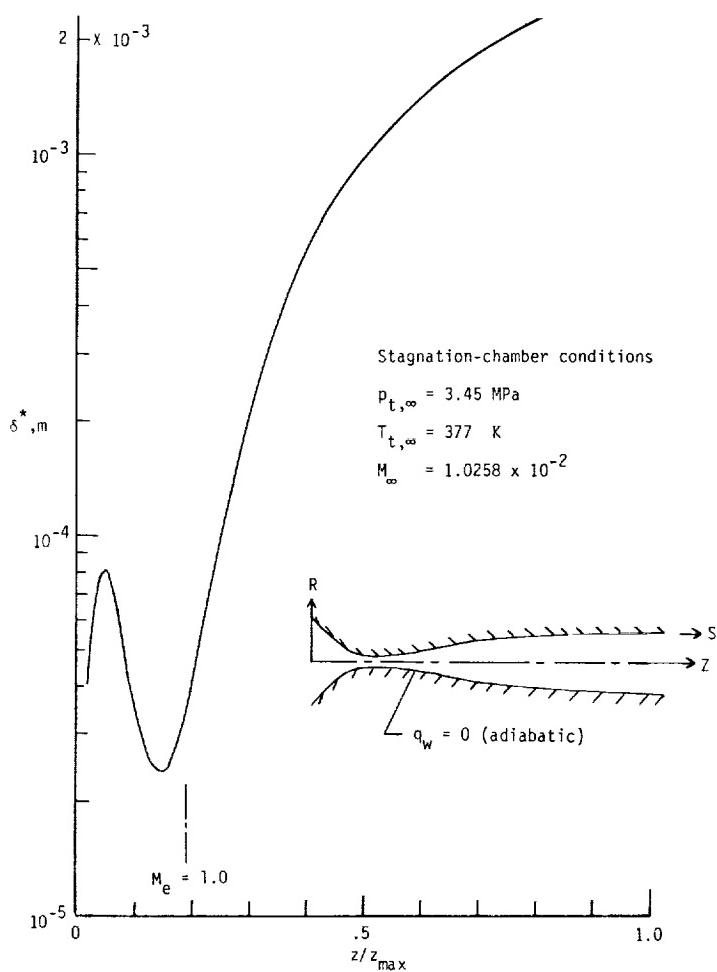


Figure 7.- Test case no. 5; displacement thickness.

A common problem often encountered in large pressure-gradient flows is oscillations in  $\delta^*$  caused by the specification of  $p_e = g(s)$  and/or step size in the s-coordinate. For many applications (e.g., rocket nozzle design), these oscillations may be acceptable, but for facility design, where the design goal is usually to achieve a shock-free flow that meets the design test-section flow conditions, caution and judgment must be exercised in specifying the inviscid pressure distribution and step-size distribution in the s-coordinate. For example, if a relatively coarse distribution of  $p_e = g(s)$  and a fine distribution of  $\Delta s$  were specified, the resulting pressure-gradient distribution  $\frac{dp_e}{ds} = \frac{d[g(s)]}{ds}$  would be a series of step functions for linear interpolation. Spline functions or higher-order interpolation could be used to obtain  $p_e$  and  $dp_e/ds$  at the solution stations from the specified input values; however, care must be exercised since higher-order interpolation can introduce oscillations resulting in changes in the sign of the pressure gradient. Splines with tension represent the optimum technique for generating  $p_e$  and  $dp_e/ds$  at the solution stations from the input data; however, experience has indicated that it is more efficient to input a sufficiently dense distribution of  $p_e = g(s)$  and use linear interpolation. It is suggested that the user of program VGBLP work several problems with large pressure variations in order to gain experience in specifying pressure input and step-size distributions.

#### **CONCLUDING REMARKS**

A computer program, VGBLP, has been presented for solving the compressible laminar, transitional, or turbulent boundary-layer equations for planar or axisymmetric perfect-gas attached flows. A three-point implicit, variable-grid finite-difference procedure is used to solve the governing equations. The algorithm and software are modifications of the procedures presented in NASA TR R-368 and NASA TM X-2458, respectively. The modifications render the approach easier to implement while increasing the efficiency (computer resources) and accuracy as compared with the original approach presented in NASA TR R-368.

Test cases have been presented and should serve as guides for potential users of the software. These cases cover external and internal flows including flows with wall-mass transfer effects, transverse-curvature effects, and variable-entropy effects.

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Hampton, VA 23665  
November 6, 1981

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## APPENDIX A

## DIFFERENCE RELATIONS

Three-point implicit difference relations are used in references 3 and 4 to reduce the transformed momentum and energy equations (eqs. (28) and (29)) to finite-difference form. The differencing scheme proposed by Blottner (ref. 7) is used in program VGBLP. For completeness, both differencing techniques are presented.

It is assumed that all data are known at the solution stations  $m-1$  and  $m$ . (See fig. 1.) Then, it is possible to obtain the unknown quantities at the grid points for the  $m+1$  station. In the subsequent development the notations  $G$  and  $H$  are utilized to represent any typical variable.

Taylor-series expansions are first written about the unknown grid point  $(m+1, n)$  in the  $\xi$ -direction as follows:

$$G_{m,n} = G_{m+1,n} - \Delta\xi_2 (G_\xi)_{m+1,n} + \frac{\Delta\xi_2^2}{2} (G_{\xi\xi})_{m+1,n} - \frac{\Delta\xi_2^3}{6} (G_{\xi\xi\xi})_{m+1,n} + \dots \quad (\text{Ala})$$

and

$$\begin{aligned} G_{m-1,n} &= G_{m+1,n} - (\Delta\xi_1 + \Delta\xi_2) (G_\xi)_{m+1,n} + \frac{(\Delta\xi_1 + \Delta\xi_2)^2}{2} (G_{\xi\xi})_{m+1,n} \\ &\quad - \frac{(\Delta\xi_1 + \Delta\xi_2)^3}{6} (G_{\xi\xi\xi})_{m+1,n} + \dots \end{aligned} \quad (\text{Alb})$$

where subscript notation has been utilized to denote differentiation; for example,  $G_\xi \equiv \partial G / \partial \xi$ .

Equations (Ala) and (Alb) can be solved to yield

$$\left( \frac{\partial G}{\partial \xi} \right)_{m+1,n} = \frac{x_1 G_{m+1,n} - x_2 G_{m,n} + x_3 G_{m-1,n}}{2 \Delta\xi_2} + \frac{\Delta\xi_2 (\Delta\xi_1 + \Delta\xi_2)}{6} G_{\xi\xi\xi} + \dots \quad (\text{A2})$$

and

$$G_{m+1,n} = x_4 G_{m,n} - x_5 G_{m-1,n} + \frac{\Delta\xi_1 \Delta\xi_2}{2} \left( 1 + \frac{\Delta\xi_2}{\Delta\xi_1} \right) G_{\xi\xi} + \dots \quad (\text{A3})$$

Terms of the order of  $\Delta\xi_1 \Delta\xi_2$ , or smaller, are neglected. This produces truncation errors of the order of  $\Delta\xi_1 \Delta\xi_2$  instead of  $\Delta\xi_2$  as in reference 5 where two-point difference relations are used. The  $x_1, x_2, \dots, x_5$  coefficients appearing in equations (A2) and (A3) are defined as follows:

$$x_1 = 2 \frac{\Delta\xi_1 + 2\Delta\xi_2}{\Delta\xi_1 + \Delta\xi_2} \quad (A4)$$

$$x_2 = 2 \frac{\Delta\xi_1 + \Delta\xi_2}{\Delta\xi_1} \quad (A5)$$

$$x_3 = 2 \frac{\Delta\xi_2^2}{\Delta\xi_1(\Delta\xi_1 + \Delta\xi_2)} \quad (A6)$$

$$x_4 = \frac{\Delta\xi_1 + \Delta\xi_2}{\Delta\xi_1} \quad (A7)$$

and

$$x_5 = \frac{\Delta\xi_2}{\Delta\xi_1} \quad (A8)$$

Taylor-series expansions are next written about the unknown grid point  $(m+1, n)$  in the  $\eta$ -direction as follows:

$$\begin{aligned} G_{m+1,n+1} &= G_{m+1,n} + \Delta\eta_n (G_\eta)_{m+1,n} + \frac{\Delta\eta_n^2}{2} (G_{\eta\eta})_{m+1,n} \\ &\quad + \frac{\Delta\eta_n^3}{6} (G_{\eta\eta\eta})_{m+1,n} + \dots \end{aligned} \quad (A9a)$$

and

$$\begin{aligned} G_{m+1,n-1} &= G_{m+1,n} - \Delta\eta_{n-1} (G_\eta)_{m+1,n} + \frac{\Delta\eta_{n-1}^2}{2} (G_{\eta\eta})_{m+1,n} \\ &\quad - \frac{\Delta\eta_{n-1}^3}{6} (G_{\eta\eta\eta})_{m+1,n} + \dots \end{aligned} \quad (A9b)$$

Equations (A9a) and (A9b) can be solved to yield

$$\begin{aligned} \left( \frac{\partial^2 G}{\partial \eta^2} \right)_{m+1,n} &= Y_1 G_{m+1,n+1} - Y_2 G_{m+1,n} + Y_3 G_{m+1,n-1} \\ &\quad + \frac{(\Delta\eta_{n-1} - \Delta\eta_n)}{3} G_{\eta\eta\eta} + \dots \end{aligned} \quad (A10)$$

and

$$\left(\frac{\partial G}{\partial \eta}\right)_{m+1,n} = Y_4 G_{m+1,n+1} - Y_5 G_{m+1,n} - Y_6 G_{m+1,n-1} - \frac{\Delta \eta_n \Delta \eta_{n-1}}{6} G_{m+1,n} + \dots \quad (\text{A11})$$

The  $Y_1, Y_2, \dots, Y_6$  coefficients appearing in equations (A10) and (A11) are defined as follows:

$$Y_1 = \frac{2}{\Delta \eta_n (\Delta \eta_n + \Delta \eta_{n-1})} \quad (\text{A12})$$

$$Y_2 = \frac{2}{\Delta \eta_n \Delta \eta_{n-1}} \quad (\text{A13})$$

$$Y_3 = \frac{2}{\Delta \eta_{n-1} (\Delta \eta_n + \Delta \eta_{n-1})} \quad (\text{A14})$$

$$Y_4 = \frac{\Delta \eta_{n-1}}{\Delta \eta_n (\Delta \eta_n + \Delta \eta_{n-1})} \quad (\text{A15})$$

$$Y_5 = \frac{\Delta \eta_{n-1} - \Delta \eta_n}{\Delta \eta_n \Delta \eta_{n-1}} \quad (\text{A16})$$

and

$$Y_6 = \frac{\Delta \eta_n}{\Delta \eta_{n-1} (\Delta \eta_n + \Delta \eta_{n-1})} \quad (\text{A17})$$

For the case of equally spaced grid points in the  $\xi$ - and  $\eta$ -coordinates, equations (A4) to (A8) and (A12) to (A17) reduce to the following relations:

$$\left. \begin{array}{l} x_1 = 3 \\ x_2 = 4 \\ x_3 = 1 \\ x_4 = 2 \\ x_5 = 1 \end{array} \right\} \quad (\text{A18a})$$

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and

$$\left. \begin{array}{l} Y_1 = \frac{1}{\Delta\eta^2} \\ Y_2 = 2Y_1 \\ Y_3 = Y_1 \\ Y_4 = \frac{1}{2\Delta\eta} \\ Y_5 = 0 \\ Y_6 = Y_4 \end{array} \right\} \quad \begin{array}{l} \text{ORIGINAL PAGE IS} \\ \text{OF POOR QUALITY} \end{array} \quad (A18b)$$

where  $\Delta\xi$  and  $\Delta\eta$  represent the spacing between the grid points in the  $\xi$ - and  $\eta$ -coordinates, respectively.

Equations (A2), (A3), (A10), and (A11) can then be written for constant grid-point spacing as follows:

$$\left( \frac{\partial G}{\partial \xi} \right)_{m+1,n} = \frac{3G_{m+1,n} - 4G_{m,n} + G_{m-1,n}}{2\Delta\xi} + \frac{\Delta\xi^2}{3} G_{\xi\xi\xi} + \dots \quad (A19)$$

$$G_{m+1,n} = 2G_{m,n} - G_{m-1,n} + \Delta\xi^2 G_{\xi\xi} + \dots \quad (A20)$$

$$\left( \frac{\partial^2 G}{\partial \eta^2} \right)_{m+1,n} = \frac{G_{m+1,n+1} - 2G_{m+1,n} + G_{m+1,n-1}}{\Delta\eta^2} - \frac{\Delta\eta^2}{12} G_{\eta\eta\eta\eta} + \dots \quad (A21)$$

and

$$\left( \frac{\partial G}{\partial \eta} \right)_{m+1,n} = \frac{G_{m+1,n+1} - G_{m+1,n-1}}{2\Delta\eta} - \frac{\Delta\eta^2}{6} G_{\eta\eta\eta} + \dots \quad (A22)$$

Quantities of the form  $\left( G \frac{\partial H}{\partial \xi} \right)$  that appear in the governing equations must be linearized in order to obtain a system of linear-difference equations. Quantities of this type are obtained from equations (A2) and (A3).

## APPENDIX A

The procedure used to linearize nonlinear products such as  $\left(\frac{\partial G}{\partial \eta}\right)\left(\frac{\partial H}{\partial \eta}\right)$  is the same as that used by Flügge-Lotz and Blottner (ref. 5) and is as follows:

$$\begin{aligned} \left[ \left( \frac{\partial G}{\partial \eta} \right) \left( \frac{\partial H}{\partial \eta} \right) \right]_{m+1,n} &= \left( \frac{\partial G}{\partial \eta} \right)_{m,n} \left( \frac{\partial H}{\partial \eta} \right)_{m+1,n} - \left( \frac{\partial G}{\partial \eta} \right)_{m,n} \left( \frac{\partial H}{\partial \eta} \right)_{m,n} \\ &\quad + \left( \frac{\partial H}{\partial \eta} \right)_{m,n} \left( \frac{\partial G}{\partial \eta} \right)_{m+1,n} + O(\Delta \xi_2)^2 \end{aligned} \quad (A23)$$

where the terms  $\left( \frac{\partial G}{\partial \eta} \right)_{m,n}$  and  $\left( \frac{\partial H}{\partial \eta} \right)_{m,n}$  are evaluated from equation (A11), but at the known station  $m$ . By equating  $G$  to  $H$  in equation (A23), the linearized form for quantities of the type  $\left( \frac{\partial G}{\partial \eta} \right)^2$  is obtained; that is,

$$\left( \frac{\partial G}{\partial \eta} \right)_{m+1,n}^2 = \left( \frac{\partial G}{\partial \eta} \right)_{m,n} \left[ 2 \left( \frac{\partial G}{\partial \eta} \right)_{m+1,n} - \left( \frac{\partial G}{\partial \eta} \right)_{m,n} \right] + O(\Delta \xi_2)^2 \quad (A24)$$

where  $\left( \frac{\partial G}{\partial \eta} \right)_{m+1,n}$  is obtained from equation (A11).

The preceding relations for the difference quotients produce linear-difference equations when substituted into the governing differential equations (eqs. (45)). In references 3 and 4 it is noted that in practice the nonlinearities do not require iteration provided a sufficiently fine mesh-point distribution is chosen. However, if one wishes to increase the computational speed by reducing the number of grid points to a minimum, then iteration may become necessary.

Blottner (ref. 7) proposed a variable grid scheme that in principle is only first-order accurate in the normal step size  $\Delta \eta_n$ , but approaches second-order accuracy when the grid defined by equations (42) to (43) is used. In the variable grid scheme, the following difference relations are used:

$$\left( \frac{\partial G}{\partial \eta} \right)_{m+1,n} = \frac{G_{m+1,n+1} - G_{m+1,n-1}}{\Delta \eta_{n-1} + \Delta \eta_n} - \frac{(\Delta \eta_n - \Delta \eta_{n-1})}{2} G_{\eta \eta} + \dots \quad (A25)$$

$$\left( \frac{\partial^2 G}{\partial \eta^2} \right)_{m+1,n} = \text{Equation (A10)}$$

The nonlinear term is evaluated as follows:

$$\begin{aligned} \left[ \frac{\partial}{\partial n} \left( \zeta \frac{\partial G}{\partial n} \right) \right]_{m+1,n} &= \frac{2}{\Delta n_n + \Delta n_{n-1}} \left[ \zeta_{m+1,n+1} \frac{1}{2} \left( \frac{G_{m+1,n+1} - G_{m+1,n}}{\Delta n_n} \right) \right. \\ &\quad \left. - \zeta_{m+1,n-1} \frac{1}{2} \left( \frac{G_{m+1,n} - G_{m+1,n-1}}{\Delta n_{n-1}} \right) \right] \\ &\quad - \frac{1}{12} \left[ \zeta_{G_{nnn}} + 3(\zeta_{G_{\eta}})_{nn} \right]_{m+1,n} (\Delta n_n - \Delta n_{n-1}) \end{aligned} \quad (A26)$$

where

$$\zeta_{m+1,n+\frac{1}{2}} = \frac{\zeta_{m+1,n+1} + \zeta_{m+1,n}}{2} \quad (A27)$$

## APPENDIX B

### COEFFICIENTS FOR DIFFERENCE EQUATIONS

Equations (45) are the difference equations used to represent the partial differential equations for the conservation of momentum and energy, respectively. These equations are repeated for convenience as follows:

#### Momentum equation

$$\begin{aligned} A_{1n} F_{m+1,n-1} + B_{1n} F_{m+1,n} + C_{1n} F_{m+1,n+1} + D_{1n} \theta_{m+1,n-1} \\ + E_{1n} \theta_{m+1,n} + F_{1n} \theta_{m+1,n+1} = G_{1n} \end{aligned} \quad (B1)$$

#### Energy equation

$$\begin{aligned} A_{2n} F_{m+1,n-1} + B_{2n} F_{m+1,n} + C_{2n} F_{m+1,n+1} + D_{2n} \theta_{m+1,n-1} \\ + E_{2n} \theta_{m+1,n} + F_{2n} \theta_{m+1,n+1} = G_{2n} \end{aligned} \quad (B2)$$

These equations are obtained from equations (28) and (29) and the difference quotients presented in appendix A. The coefficients  $A_{1n}$ ,  $B_{1n}$ , and so forth, in equations (B1) and (B2) are functions of known quantities evaluated at stations  $m$  and  $m-1$ . (See fig. 1.) Therefore, equations (B1) and (B2) can be solved simultaneously. In references 3 and 4, equations (B1) and (B2) were solved simultaneously without iteration. The reader interested in the coefficients for the noniterative simultaneous solution is referred to appendix B of reference 4. In the present approach, using the Blottner variable grid scheme (ref. 7), the coefficients are written as follows:

#### Momentum equation

$$A_{1n} = -\frac{(v_{m+1,n})_g}{\Delta \eta_{n-1} + \Delta \eta_n} - \left[ \frac{(t^2 j \bar{\epsilon})_{m+1,n} + (t^2 j \bar{\epsilon})_{m+1,n-1}}{2} \right] Y_{3n} \quad (B3a)$$

$$\begin{aligned} B_{1n} = & \left[ \frac{\xi (F_{m+1,n})_g}{\Delta \xi_2} \right] X_1 + \left[ \frac{(t^2 j \bar{\epsilon})_{m+1,n} + (t^2 j \bar{\epsilon})_{m+1,n+1}}{2} \right] Y_{1n} \\ & + \left[ \frac{(t^2 j \bar{\epsilon})_{m+1,n} + (t^2 j \bar{\epsilon})_{m+1,n-1}}{2} \right] Y_{3n} + 2\beta (F_{m+1,n})_g \end{aligned} \quad (B3b)$$

$$C_{1n} = \frac{(v_{m+1,n})_g}{\Delta \eta_{n-1} + \Delta \eta_n} - \left[ \frac{(t^2 j \bar{\epsilon})_{m+1,n} + (t^2 j \bar{\epsilon})_{m+1,n+1}}{2} \right] Y_{1n} \quad (B3c)$$

APPENDIX B

$$Dl_n = 0 \quad (B3d)$$

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$$El_n = -\beta \quad (B3e)$$

$$Fl_n = 0 \quad (B3f)$$

$$Gl_n = \frac{\xi(F_{m+1,n})_g}{\Delta\xi_2} \left[ (x2)F_{m,n} - (x3)F_{m-1,n} \right] - \beta(F_{m+1,n})_g^2 \quad (B3g)$$

Energy equation

$$A2_n = \frac{2(\alpha\ell t^2 j\bar{\varepsilon})_{m+1,n} \left[ \left( \frac{\partial F}{\partial n} \right)_{m+1,n} \right]_g}{\Delta n_{n-1} + \Delta n_n} \quad (B4a)$$

$$B2_n = 0 \quad (B4b)$$

$$C2_n = - \frac{2(\alpha\ell t^2 j\bar{\varepsilon})_{m+1,n} \left[ \left( \frac{\partial F}{\partial n} \right)_{m+1,n} \right]_g}{\Delta n_{n-1} + \Delta n_n} \quad (B4c)$$

$$D2_n = - \frac{(v_{m+1,n})_g}{\Delta n_{n-1} + \Delta n_n} - \left[ \frac{(t^2 j \ell \tilde{\varepsilon})_{m+1,n} + (t^2 j \ell \tilde{\varepsilon})_{m+1,n-1}}{2} \right] Y3_n \quad (B4d)$$

$$E2_n = \left[ \frac{\xi(F_{m+1,n})}{\Delta\xi_2} \right] X1 + \left[ \frac{(t^2 j \ell \tilde{\varepsilon})_{m+1,n} + (t^2 j \ell \tilde{\varepsilon})_{m+1,n-1}}{2} \right] Y1_n \\ + \left[ \frac{(t^2 j \ell \tilde{\varepsilon})_{m+1,n} + (t^2 j \ell \tilde{\varepsilon})_{m+1,n-1}}{2} \right] Y3_n \quad (B4e)$$

$$F2_n = \frac{(v_{m+1,n})_g}{\Delta n_{n-1} + \Delta n_n} - \left[ \frac{(t^2 j \ell \tilde{\varepsilon})_{m+1,n} + (t^2 j \ell \tilde{\varepsilon})_{m+1,n+1}}{2} \right] Y1_n \quad (B4f)$$

$$G2_n = \frac{\xi(F_{m+1,n})_g}{\Delta\xi_2} \left[ (x2)\Theta_{m,n} - (x3)\Theta_{m-1,n} \right] - (\alpha\ell t^2 j\bar{\varepsilon})_{m+1,n} \left[ \left( \frac{\partial F}{\partial n} \right)_{m+1,n}^2 \right]_g \quad (B4g)$$

These equations are solved using the coupled solution technique presented in references 3 and 4. A major difference between the present approach (program VGBLP) and that of reference 4 is that the system of equations can be iterated in the present

## APPENDIX B

approach as opposed to no iteration in reference 4. The iteration cycle is as follows: (1) the  $g$  subscripted quantities are first obtained from known values at stations  $m-1$  and  $m$  using equation (A3) for the initial solution of the system at station  $m+1$  (note that the continuity equation is integrated using the trapezoidal rule of integration); (2) for the remaining iterations the  $g$  subscripted quantities assume their value at the previous iteration at station  $m+1$ . The eddy viscosity is updated after each iteration.

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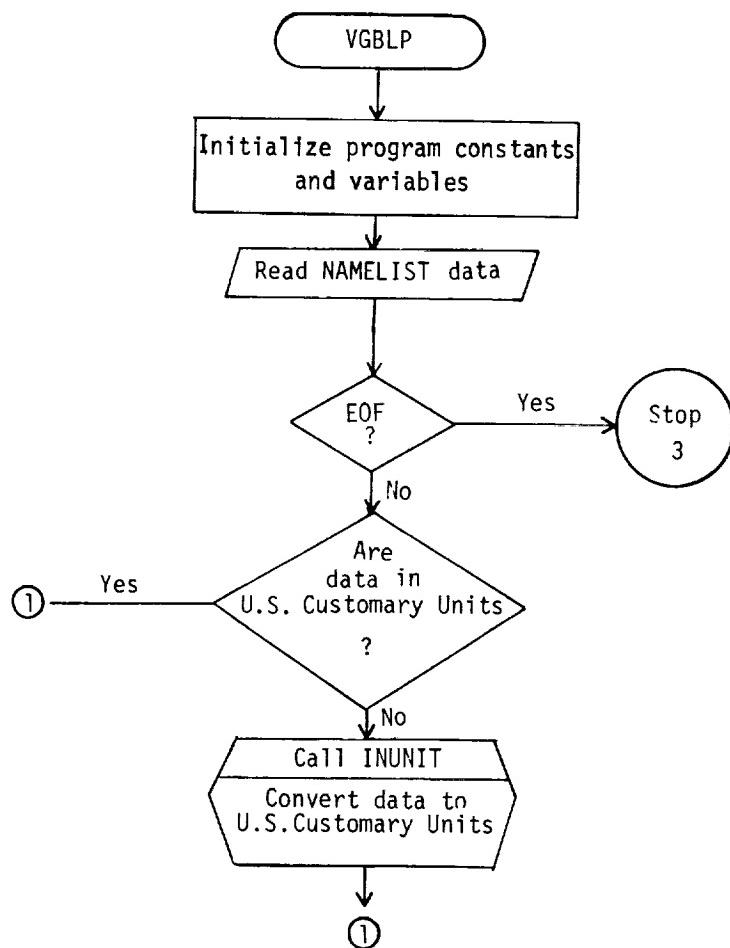
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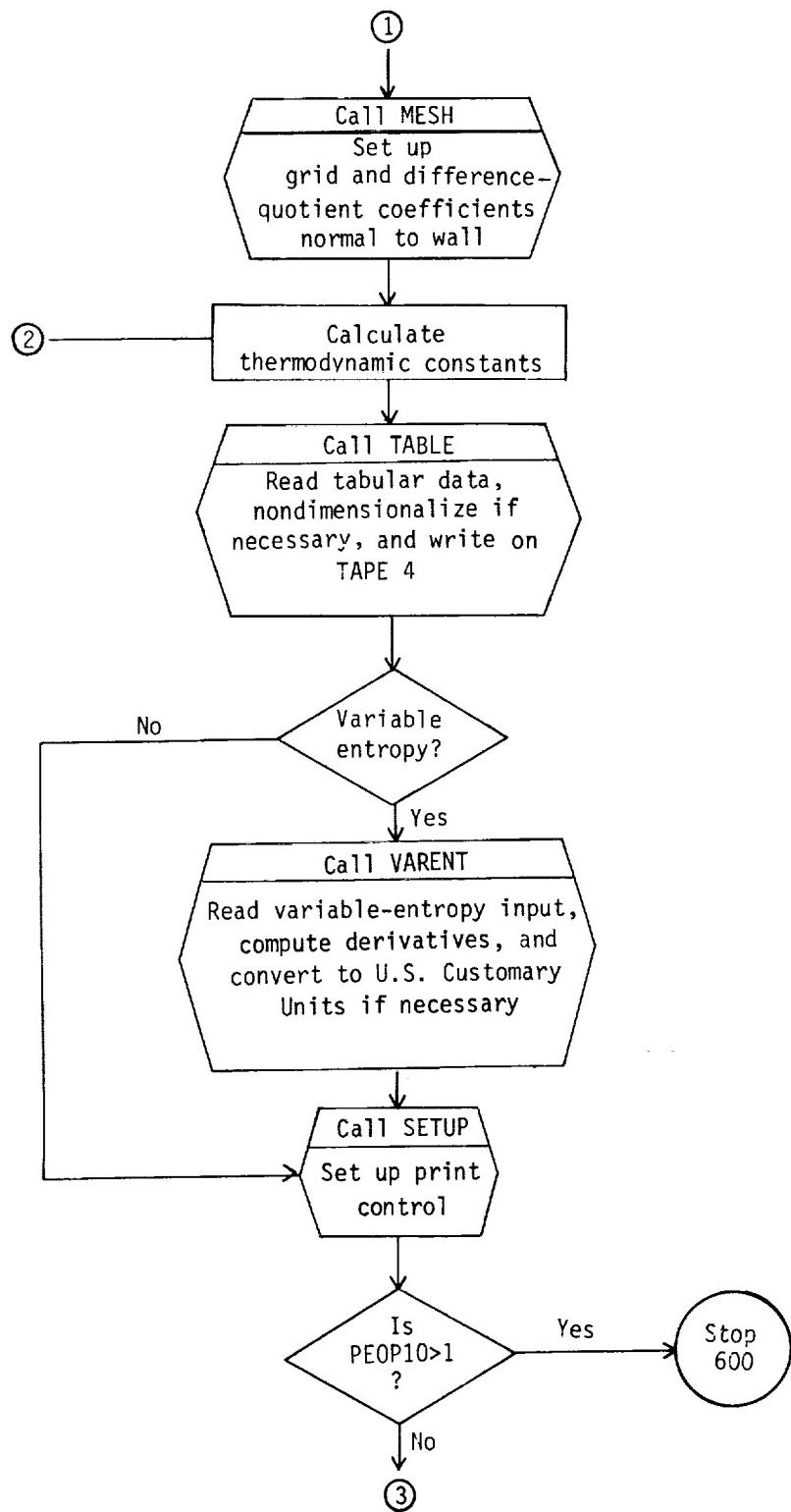
APPENDIX C

FLOW CHARTS AND PROGRAM LISTING

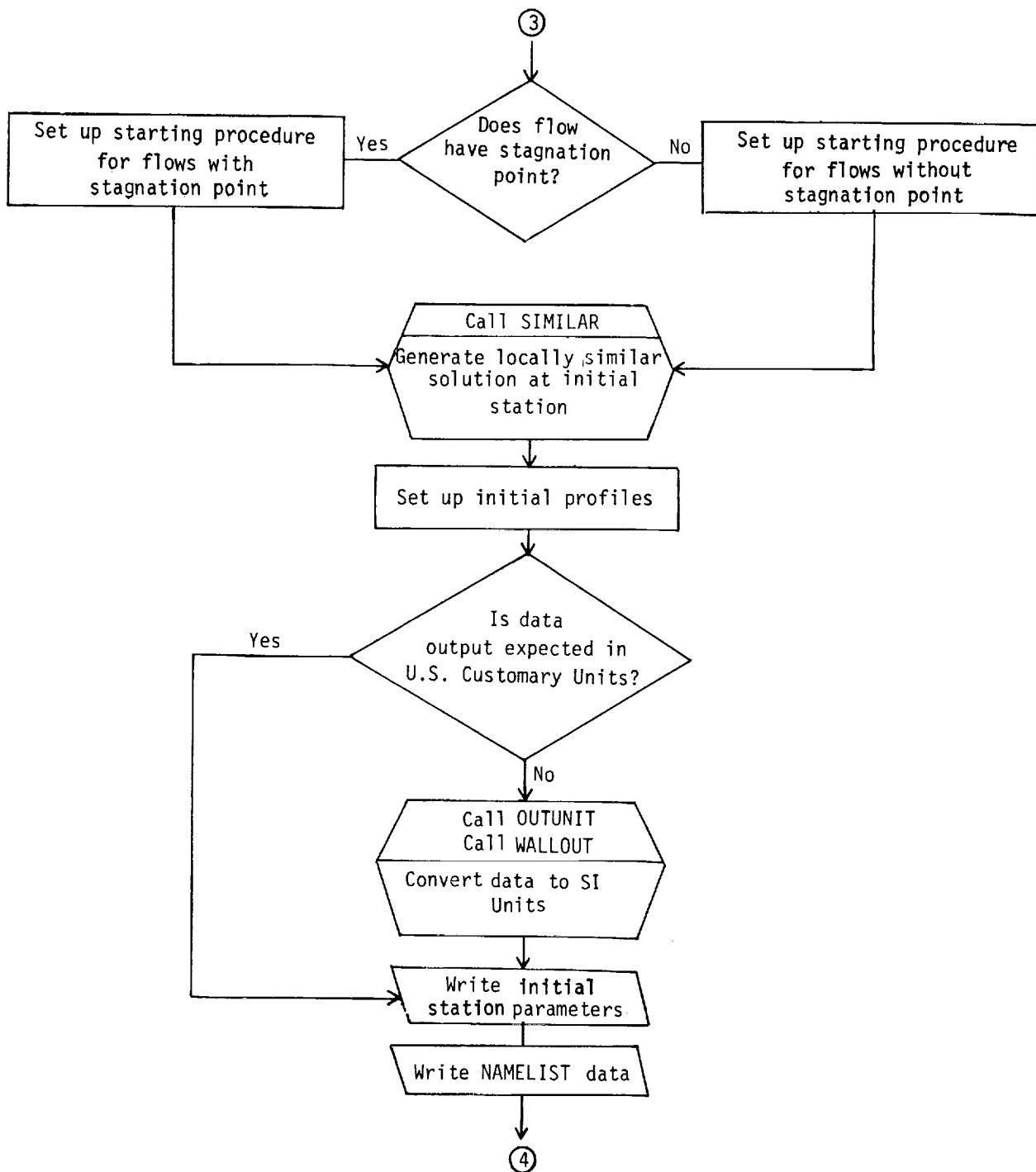
Main Program VGBLP

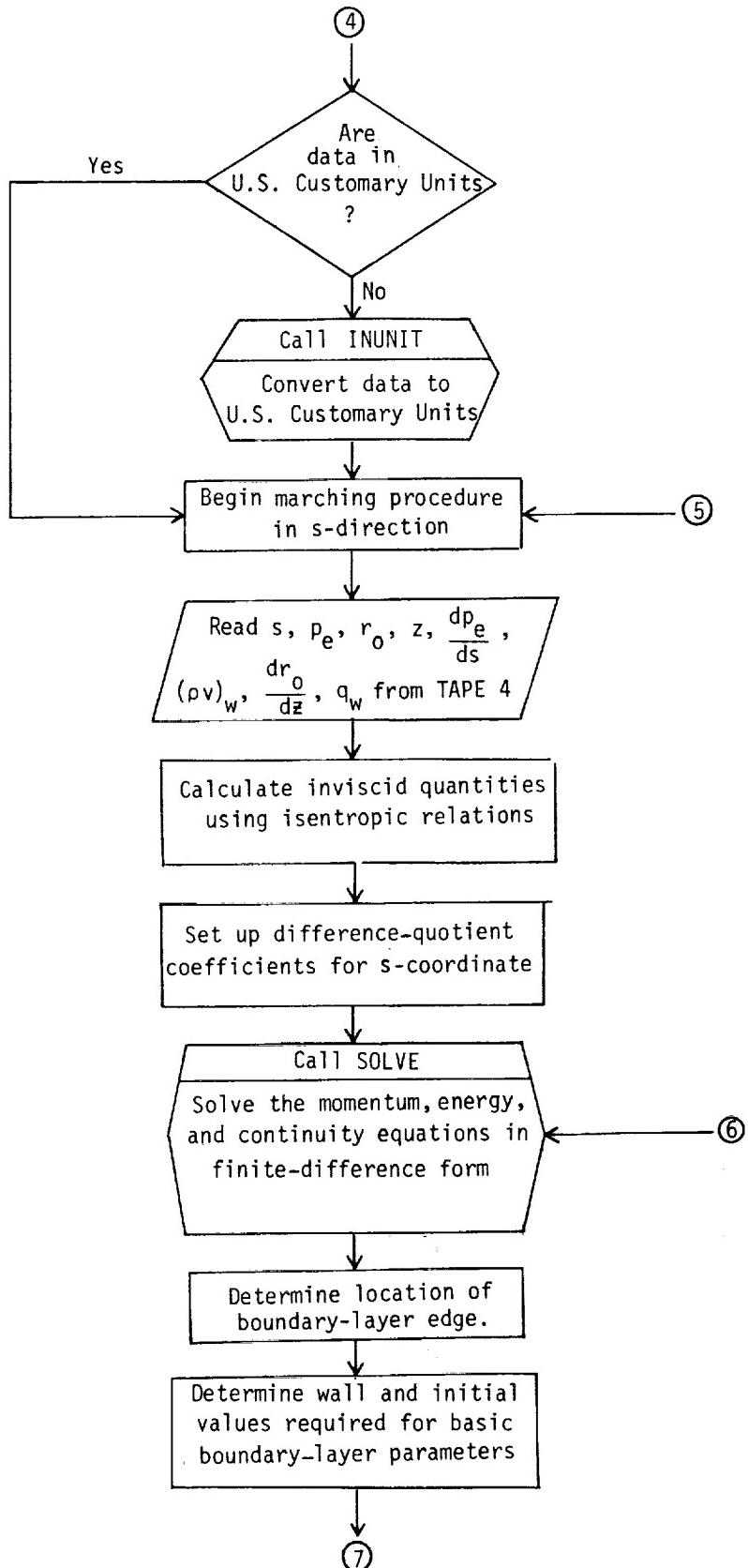
Program VGBLP controls the sequence of finite-difference solutions for the boundary-layer equations. It reads the input and, through its subroutines, sets up the computational grid, generates the initial solution, controls the parabolic marching procedure wherein the nonsimilar solutions are obtained, calculates all boundary-layer parameters, and prints the output at specified locations. The flow chart for the main program is as follows:

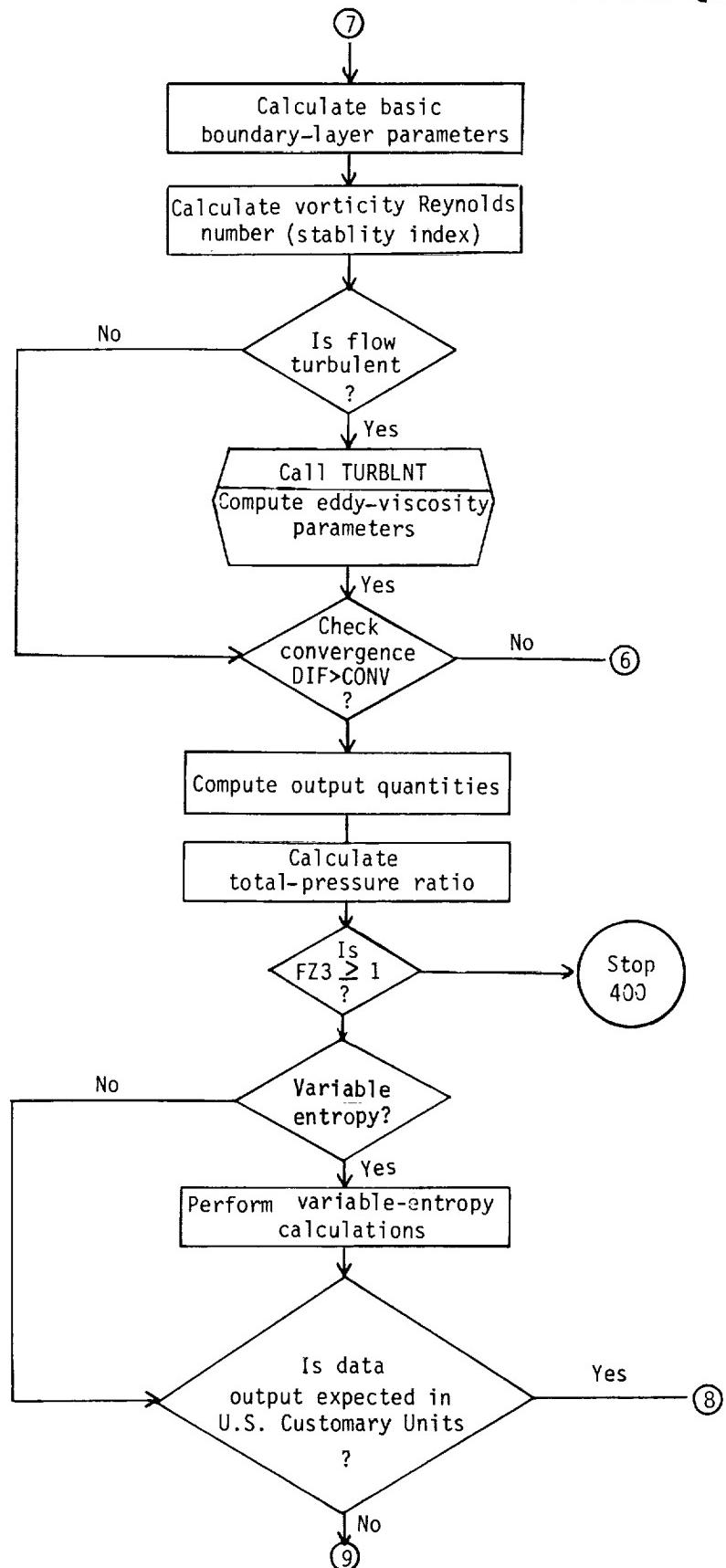


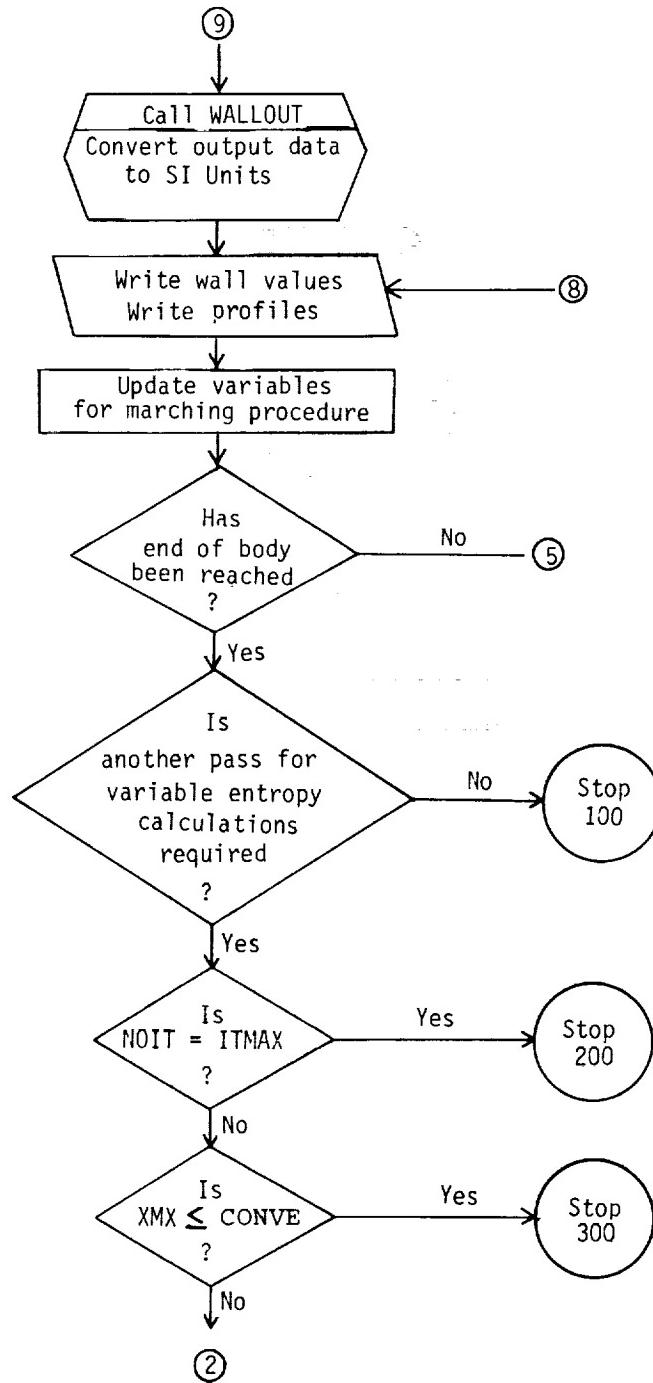


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The program listing for program VGBLP is as follows:

```

PROGRAM VGBLP(INPUT,OUTPUT,TAPE5=INPUT,TAPE6=OUTPUT,TAPE4)
DIMENSION PTOPT(JK), STA82(JK), MOME(JK), TTUTT(JK), CRUCCO(JK), U
1OUPL(JK), TCORD(JK), UDEF(JK), NONDEL(JK), UEE(JH), PROVAL(JN), PR
2NTVAL(JM), TAUP(JK), RRS(JL), ZZS(JL), DRSDZS(JL), DVT(JL,2), ANSI
32), PRTAR(JI)
COMMON /MESH1/ XN(JK),DN(JK),Y1(JK),Y2(JK),Y3(JK),Y4(JK),Y5(JK),Y6
1(JK)
COMMON /SOLV1/ F1(JK),F2(JK),F3(JK),T1(JK),T2(JK),T3(JK),V1(JK),V2
1(JK),V3(JK),EP2(JK),EP3(JK),F22(JK),F33(JK),T22(JK),T33(JK),XL2(JK
2),XL3(JK),XLP2(JK),XLP3(JK),RATO1(JK),RATO2(JK),RATO3(JK),EH2(JK),
3EH3(JK),DRATO1(JK),DRATO2(JK),DRATO3(JK),VARA(JK),VARB(JK),VARC(JK
4),VARD(JK),VARE(JK),Y(JK),EP1(JK),EH1(JK),XL1(JK),XLP1(JK)
COMMON /SOLV2/ Z1,Z2,Z3,Z4,Z5,TE,FAA,FAB,FAC,FAD,BEX1,BEX2,BEX3,BE
1X4
EQUIVALENCE (ZZS,DVT(1,1)), (DRSDZS,DVT(1,2))
COMMON /TRBULNT/ S,KSTR,TLNGTH,TRFACT,DISINC,XT1,XT2,XT6,XT3,XT4,X
1T5,PRTW,RE,UE,XNJE,J,RMI,EPS,JPOINT,IE,WW1,WW2,WW3,WW4,WW5, NEDGE
2,KODVIS,A,XBE,X,PR,KDUPRT,PRT,PRTAR,GLAR,NUMB1,XK
COMMON /UNIT/ VIS1C1,VIS1C2,VIS2C1,VIS2C2,PT1,TT1,WAVE,R,PHIO,DS,S
1ST,RT1,P1,TI,R1,U1,AA1,TREF,VISREF,PESTAR,TESTAR,RESTAR,UESTAR,MUE
2STAR,YESTAR,THETA,TAUD,QSD,HD,UPLUS,DISP,PE,2,TW,QW,RRWALD,PROINC,
3PRNTINC,ZS,RS
INTEGER W
REAL MOME,NUE,NJW,KWD,KED,INTEGT,INTEGL,NONDEL,MUESTAR
EXTERNAL INTEGT
NAMELIST /NAM1/IGEOM,XEND,IE,XK,DETA1,XMA,PT1,TT1,IGAS,VIS1C1,VIS1
1C2,VIS2C1,VIS2C2,G,R,PR,IBODY,WAVE,PHI1,J,W,IENTRU,SST,SMXTR,KODVI
2S,KTCUD,TLNGTH,IYINT,KODAMP,XT1,XT2,XT3,XT4,XT5,XT6,PRT,KODPRT,NUM
3B1,GLAR,PRTAR,IEND1,PROINC,PRNTINC,IPRO,IPRNT,NAUXPRO,PROVAL,PRNTV
4AL,FT,KODE,KODWAL,VELEDG,CONV,NITMAX,KODUNIT,ITMAX,CONVE
C
C   INITIALIZE DATA TO STANDARD INPUT
C
DATA G/1.4/,R/1716./,PR/.72/,PRT/.95/,W/0/,KODE/0/,KJDWAL/1/,IENTR
1U/1/,A/1./,KODVIS/2/,SST/1.E8/,FT/1./,SMXTR/1.E8/,TLNGTH/2./,XT1 /
2.4/,XT2/.0168/,XT3/5./,XT4/.78/,XT5/.108/,XT6/26./,PROINC/1./,PRNT
3INC/.1/,NAUXPRO/0/,NPUTYPE/1/,IPRO/0/,IPRNT/0/,CLNV/.0001/,NUMB1/0
4/
DATA THATS/0./,RS/0./,P20/0./,NITMAX/1/,SIGN/1./,ST2MAX/1000001/,T
1RFACT/0./,KSTR/0/,ITMAX/3/,NOIT/0/,DPEDS/0./,Z/0./,KODPRT/1/,KTCOD
2/2/,KTCD/0/,IGAS/1/,KODAMP/2/,VELEDG/.995/,IYINT/1/,SMXN/0./,SMXO/
30./,SMXP/0./,PRTW/.95/,KODUNIT/0/,ANRAD/1.745329E-2/,VIS1C1/2.27E-
48/,VIS1C2/198.6/,XVAL1/0./,CONVE/.01/
Y(1)=0.
NONDEL(1)=0.
DO 1 I=1,JN
1 PROVAL(I)=0.
DO 2 I=1,JM
2 PRNTVAL(I)=0.
DO 3 I=1,JL
3 DRSDZS(I)=0.

```

```
3 UEE(I)=0.  
DO 4 I=1,JK  
EP2(I)=EP3(I)=XL2(I)=XL3(I)=RATO1(I)=RATO2(I)=RATO3(I)=T1(I)=T2(I)  
I=T3(I)=F1(I)=F2(I)=F3(I)=EP1(I)=1.0  
TAUP(I)=1.  
STAB2(I)=FZ2(I)=TZ2(I)=XLP2(I)=XLP3(I)=FZ3(I)=TZ3(I)=DRATO1(I)=DRA  
IT02(I)=DRATO3(I)=0.  
4 CONTINUE
```

C  
C       READ NAMELIST INPUT  
C

```
READ (5,NAM1)  
IF (EOF(5)) 5,6  
5 STOP 3  
6 WRITE(6,82) IGEM, XEND, IE, XK, DETA1, XMA, PT1, TT1, IGAS, VIS1C1, VIS1C2,  
1VIS2C1, VIS2C2, G, R, PR, IBODY, WAVE, PHII, J, W, IENTRD, SST, SMXTR, KUDVIS, K  
2TCOD, TLNGTH, IYINT, KUDAMP, XT1, XT2, XT3, XT4, XT5, XT6, PRT, KUDPRT, NUMB1,  
3GLAR, PRTAR  
WRITE(6,83) IEND1, PROINC, PRNTINC, IPRO, IPRNT, NAUXPRO, FT, KODE, KUDWAL,  
1VELEDG, CONV, NITMAX, KUDUNIT, ITMAX, CONVE  
IF (KUDUNIT.NE.1) GO TO 8  
AT1=TT1  
AT2=TT1/2.  
IF (IGAS.EQ.2) GO TO 7  
AX1=VIS1C1*(AT1**1.5)/(AT1+VIS1C2)  
AX2=VIS1C1*(AT2**1.5)/(AT2+VIS1C2)  
AC1=SQRT(5./9.)/47.878258  
VIS1C1=AC1*SQRT(AX1*AX2*(AT1+VIS1C2)*(AT2+VIS1C2)/((AT1*AT2)**1.5))  
1)  
VIS1C2=VIS1C2*9./5.  
GO TO 8  
7 CONTINUE  
AX1=VIS2C1*(AT1**VIS2C2)  
AX2=VIS2C1*(AT2**VIS2C2)  
AC1=((5./9.)**VIS2C2)/47.860258  
VIS2C1=AC1*SQRT(AX1*AX2/((AT1*AT2)**VIS2C2))  
8 CONTINUE  
PHIO=PHII  
IF (KUDUNIT.EQ.1) CALL INUNIT (PROVAL, PRNTVAL, JM, JN)
```

C  
C       SET UP GRID NORMAL TO WALL  
C

```
W1=XK  
W2=1+W1  
W3=1+W1+W1*W1  
WW1=W3*W3*(W1*W2-1.)+W2  
WW2=W1*W2*W3*W3  
WW3=W3*W3  
WW4=1.+W1  
WW5=W1*W1*W1*W2*W3  
CALL MESH (XK, XEND, IE, IGEM, DETA1)  
RPR=1./PR  
DO 9 N=1,JK  
EH2(N)=RPR
```

```

EH3(N)=RPR
EH1(N)=RPR
9 CONTINUE

```

C  
C  
C      PROGRAM CONSTANTS

```

10 CONTINUE
XMAC=1.+.5*(G-1.)*XMA**2
RT1=PT1/(R*TT1)
P1=PT1/(XMAC)**(G/(G-1.))
R1=RT1/(XMAC)**(1./(G-1.))
TI=TT1/XMAC
AA1=SQRT(G*P1/R1)
U1=XMA*AA1
TREF=U1**2/((G/(G-1.))*R)
GP1=G+1.
GM1=G-1.
GM10G=GM1/G
XWAVE=ANRAD*WAVE
IF (KUDWAL.EQ.1) GO TO 12
IF (XWAVE.EQ.0.) GO TO 11
XAF=(XMA*SIN(XWAVE))**2
T2DT1=(2.*G*XAF-GM1)*(GM1*XAF+2.)/(GP1*GP1*XAF)
XM2=(GP1*GP1*XMA*XMA*XAF-4.*(XAF-1.)*(G*XAF+1.))/((2.*G*XAF-GM1)*(1.
GM1*XAF+2.))
AWT=TI*T2DT1*(1.+SQRT(PR)*GM1*XM2*0.5)
GO TO 12
11 AWT=TI*(1.+SQRT(PR)*GM1*XMA*XMA*0.5)
12 CONTINUE
IF (IGAS.EQ.2) GO TO 13
VIS1=VIS1C1*(TI**1.5)/(TI+VIS1C2)
VISREF=VIS1C1*(TREF**1.5)/(TREF+VIS1C2)
GO TO 14
13 VIS1=VIS2C1*(TI**VIS2C2)
VISREF=VIS2C1*(TREF**VIS2C2)
14 CONTINUE
REY=R1*U1*A/VIS1
REYREF=REY*VIS1/VISREF
XCONE=ANRAD*PHIO
EPS=1./SQRT(REYREF)
ABC=(XMA*SIN(XWAVE))**2
P10=PT1/(R1*U1*U1)
IF (XWAVE.GT..0000001.DK.XWAVE.LT.-.0000001) P10=(1./(G*XMA*XMA))*1
((XMAC*ABC*(G+1.))/(ABC*(G-1.)+2.))**((G/(G-1.))*(G+1.)/(2.*G*ABC-
2*(G-1.))**((1./(G-1.)))
T10=0.5+1.0/(XMA*XMA*(G-1.0))
R10=G*P10/(T10*(G-1.0))
TC=VIS1C2/(TI*XMAC)
RFL=SQRT(PR)
RFT=PR**0.33333

```

C  
C  
C      READ TABULAR DATA

```

IF (NUIT.GT.0) GO TO 20
NABC=NPUTYPE+1

```

GO TO (19,15,16), NABC  
15 CALL TABLE (IEND1,SD,R1,U1,A,TREF,KODWAL,VISREF,KJDUNIT,AWT)  
GO TO 17  
16 CALL TABLE1 (IEND1,SD,R1,U1,A,TREF,KODWAL,VISREF,KJDUNIT,AWT)  
17 GO TO (19,18), IENTRO  
18 CALL VARENT (RRS,ZZS,DRSDZS,NNN,KJDUNIT,A)  
19 CONTINUE

C  
C  
C

SET UP PRINT CONTROL

SD=SD\*A  
CALL SETUP (PROINC,PROVAL,SD,JN,IPRO)  
CALL SETUP (PRNTINC,PRNTVAL,SD,JM,IPRNT)  
WRIT E(6,97)  
IF(KJDUNIT.EQ.1) WRITE(6,84) (PROVAL(I)\*.3048,I=1,JN)  
IF(KJDUNIT.FQ.1) WRITE(6,85) (PRNTVAL(I)\*.3048,I=1,JM)  
IF(KJDUNIT.NE.1) WRITE(6,84) PROVAL  
IF(KJDUNIT.NE.1) WRITE(6,85) PRNTVAL  
20 CONTINUE  
READ (4) TW,RVWALD,QSD,PE,DS  
SI=DS  
UE=0.  
PEOP10=PE/P10  
IF (PEOP10.GT.1.) GO TO 21  
GO TO 22  
21 CONTINUE  
ABYZ=ABS(1.-PEOP10)  
WRITE (6,81) ABYZ  
STOP 600  
22 CONTINUE  
IF (IBODY.NE.1) UE=SQRT(2.\*T10\*(1.-(PEOP10)\*\*GM1UG))  
TE=T10-.5\*UE\*UE  
RE=G\*PE/((G-1.)\*TE)  
TR=T10\*TC/TE  
TW=TW/TE  
SUT=VIS1C2/TREF  
IF (IGAS.EQ.1) XNUE=(TE\*\*1.5)\*((1.+SUT)/(TE+SUT))  
IF (IGAS.EQ.2) XNUE=TE\*\*VIS2C2  
GO TO (23,25), IBODY

C  
C  
C

STARTING PROCEDURE FOR FLOWS WITH STAGNATION POINT

23 SUT=T10\*TC  
IF (IGAS.EQ.1) VIS10=(T10\*\*1.5)\*(1.+SUT)/(T10+SUT)  
IF (IGAS.EQ.2) VIS10=T10\*\*VIS2C2  
P1PT2=P1/PT1  
IF (XMA.LE.1.) GO TO 24  
P1PT2=((((G+1.)\*XMA\*\*2)/2.)\*(-G/(G-1.)))\*((G+1.)/((2.\*G\*XMA\*\*2)-(1G-1.)))\*(-1./(G-1.))  
24 CONTINUE  
DUEDS=SQRT(2.\*((G-1.)/G)\*T10\*(1.-P1PT2))  
BELA=R10\*VIS10\*DUEDS  
RMI=SI  
DX1DS=BELA\*(SI-DS)\*\*(2\*j+1)

```

DXDS=BELA*SI**((2*J+1)
DX1=(BELA*SI**((2*J+2))/(2*J+2)
X=DX1
ARGM=-778.26*EPS*A*PR/(VISREF*U1*U1*T10*SQRT((J+1)*R10*VIS10*DUEDS
1))
XAL=0.
XBE=1./(FLOAT(J)+1.)
GO TO 28

```

C           STARTING PROCEDURE FOR FLOWS WITHOUT STAGNATION POINT  
C

```

25 CONTINUE
IF (J.EQ.0) GO TO 26
RMI=SI*SIN(XCONE)
BELEX=RE*UE*XNUE*(SIN(XCONE)**(2*J))
IF (J.NE.0.AND.PHI0.EQ.0.) BELEX=RE*UE*XNUE
DX1DS=BELEX*((SI-DS)**(2*J))
GO TO 27
26 CONTINUE
RMI=1.
BELEX=RE*UE*XNUE
DX1DS=BELEX
27 DXDS=BELEX*SI**((2*J)
DX1=(BELEX*(SI**((2*J+1)))/(2*J+1)
X=DX1
QS=DISP=0.
XAL=UE**2/TE
XBE=0.
ARGM=0.
DUEDS=0.
28 CONTINUE

```

C           GENERATE SELF SIMILAR SOLUTION  
C

```

CALL SIMILAR (IE,IGAS,XAL,XBE,PR,KODWAL,TW,DTDZW,XK,TR,VIS2C2,F3,F
12,T3,T2,V3,V2,FZ3,TZ3,XL3,EP3,ARGM,QSD)
IF (KODWAL.EQ.1.AND.IBODY.EQ.1) QSD=TZ3(1)*XL3(1)/ARGM
MUESTAR=XNUE*VISREF
UESTAR=UE*U1
TESTAR=TE*TREF
PESTAR=PE*R1*U1*U1
RESTAK=RE*R1
X=0.
DX2=DX1

```

C           SET UP INITIAL PROFILES  
C

```

DO 29 N=1,IE
V2(N)=V3(N)
V1(N)=V3(N)
T2(N)=T3(N)
T1(N)=T3(N)
F2(N)=F3(N)
F1(N)=F3(N)

```

```

XL2(N)=XL3(N)
XL1(N)=XL3(N)
XLP2(N)=XLP3(N)
XLP1(N)=XLP3(N)
TZ2(N)=TZ3(N)
FZ2(N)=FZ3(N)
29 CONTINUE
IF (KODUNIT.EQ.1) CALL OUTUNIT (PROVAL,PRNTVAL,JM,JN)
IF (KODUNIT.EQ.1) CALL WALLOUT (PKVAL,PRNTVAL,JM,JN)

C      WRITE INITIAL STATION PARAMETERS
C
C      WRITE (6,72) MUESTAR,UESTAK,TESTAR,PESTAR,QSD,XAL,XBE,RESTAR
C      IF (KODUNIT.NE.1) WRITE (6,69)
C      IF (KODUNIT.EQ.1) WRITE (6,70)
PTREF=PT1/(R1*U1*U1)
WRITE (6,71) PT1,TT1,RT1,P1,T1,R1,U1,AA1,XMA,REY,R1*U1*U1,TREF,R1,
U1,VISREF,PTREF,P10,T10,R10
IF (KODUNIT.EQ.1) CALL INUNIT (PROVAL,PRNTVAL,JM,JN)
ZS=0.
IF((IENTRD.EQ.2) .AND. (NDIT.EQ.0)) WRITE(6,88)

C      BEGIN MARCHING PROCEDURE ALONG SURFACE
SM1=-DS
S=0.
DXDS=DX1DS
IENDP1=IEND1+1
DO 68 M=2,IENDP1
SM2=SM1
SM1=S
READ (4) S,PE,RMI,TW,Z,DPEDS,RVWALD,DRDZ,QW
PHI=ATAN(DRDZ)
COSTH=COS(PHI)
PP=DPEDS
UE=SQRT(2.0*T10*(1.0-(PE/P10)**((G-1.0)/G)))
IF (NUIT.GT.0) UE=UEE(M)
TE=T10-0.5*UE*UE
XAL=UE*UE/TE
RE=G*PE/((G-1.0)*TE)
IF (IGAS.EQ.1) XNUE=(TE**1.5)*(1.0+T10*TC)/(TE+T10*TC)
IF (IGAS.EQ.2) XNUE=TE**VIS2C2
DX2DS=DX1DS
DX1DS=DXDS
DXDS=RE*UE*XNUE*(RM1**2*J)
DX2=(DXDS+DX1DS)*.5*DS
IF (IBODY.EQ.1) DX2=DX2*.5
IF (M.EQ.2) DX1=DX2
IF (M.EQ.2) GO TO 31

C      CHECK FOR CHANGE IN STEP INCREMENT
C
CKK=(S-SM1)/(SM1-SM2)
IF (CKK.LT..999999999) GO TO 30
IF (CKK.GT.1.0000001) GO TO 30

```

```

DX2=(S-SM1)*(DXDS+4.*DX1DS+DX2DS)/3.-DX1
GO TO 31
30 DX2=(S-SM1)*(DX1DS+DXDS)/2.
31 X=X+DX2
OY=2.*X
OZ=SQRT(OY)
DUEDS=-PP/(RE*UE*DXDS)
DTEDS=-UE*DUEDS
XAL=UE*UE/TE
XBE=OY*DUEDS/UE
TR=T10*TC/TE

C
C      SET UP DIFFERENCE-QUOTIENT COEFFICIENTS FOR X-CORDINATE
C
Z1=2.*((DX1+2.*DX2)/(DX1+DX2))
Z2=2.*((DX1+DX2)/DX1
Z3=2.*((DX2*DX2)/(DX1*(DX1+DX2)))
Z4=(DX1+DX2)/DX1
Z5=DX2/DX1
FAA=OZ/(RE*UE*(RMI**J))
FAB=2.*EPS*W*FAA*COSTH/(RMI**J)
FAC=2.*EPS*OZ*COSTH/(RE*UE*RMI*RMI)
FAD=RMI/(EPS*COSTH)
BEX1=(RMI**J)/(EPS*COSTH)
IF (J.EQ.0) SIGN=ABS(SIGN)
BEX2=SIGN**J
BEX3=(2.***J)*EPS*COSTH*SQRT(2.*X)/(RE*UE*(RMI***(2.*J)))
BEX4=1./(J+1)
DFDZW=1.
N1T=0
32 CONTINUE
N1T=N1T+1
IF (KODWAL.NE.1) ARGM=-QW*778.26*(EPS*A/(VISREF*U1**2))*(PR*DZ/(RE
1*UE*TE*XNUE*RMI**J))
CALL SOLVE (KODWAL,ARGM,TR,VIS2C2,XAL,XBE,X,DX2,TW,IGAS,IE,J,NIT,R
1VWALD,R1,U1,WW1,WW2,WW3,WW4,WW5,XNUE,XK,EPS,M,IBODY,FT)
CO=0.
DISINC=0.
DISP=0.
TPK=0.
THETA=0.
KON=IE+2
DO 33 N=2,KON
TPK=TPK+.5*(T3(N-1)+T3(N))*DN(N-1)
RATO3(N)=SIGN*SQRT(1.+FAB*TPK)
DRATO3(N)=FAB*T3(N)
Y(N)=BEX1*(-1.+BEX2*(1.+BEX3*TPK)**BEX4)
DISP=DISP+.5*((T3(N-1)-F3(N-1))+(T3(N)-F3(N)))*DN(N-1)
C=1./(RATO3(N)**J)
C=C*(F3(N)*(1.-F3(N)))
THETA=THETA+.5*(CO+C)*DN(N-1)
CO=C
DISINC=DISINC+.5*((T3(N-1)*(1.-F3(N-1))/RATO3(N-1))+(T3(N)*(1.-F3(
1N))/RATO3(N)))*DN(N-1)

```

```

33 CONTINUE
DISINC=DISINC*EPS*FAA*A
THETA=THETA*EPS*FAA*A
DISP=DISP*EPS*FAA*A

C
C
DETERMINE THE LOCATION OF THE BOUNDARY-LAYER EDGE
SEE INPUT DESCRIPTION FOR DEFINITION FOR VELEDG
C

NCOUNT=0
DO 34 N=1,IE
NCOUNT=NCOUNT+1
IF (F3(N).GE.VELEDG) GO TO 35
34 CONTINUE
35 NEDGE=NCOUNT
YEDGE=Y(NEDGE-1)+(VELEDG-F3(NEDGE-1))*(Y(NEDGE)-Y(NEDGE-1))/(F3(NEDGE)-F3(NEDGE-1))

C
C
CHECK THE CONVERGENCE
C

DIF=ABS(1.-FZ3(1)/DFDZW)
DFDZW=FZ3(1)
DIFI=DIF
IF (NIT.GT.NITMAX) DIF=0.

C
C
CALCULATE WALL AND INITIAL VALUES REQUIRED FOR BASIC BOUNDARY
C
LAYER PARAMETERS

C

MOME(1)=F3(1)/SQRT(T3(1))
XMF1=2.+XAL
XMF2=T3(1)*TE/T10
XMF3=1.-XMF2
TTOTT(1)=(2.*T3(1)+XAL*F3(1)*F3(1))/XMF1
CRDCCO(1)=(TTOTT(1)-XMF2)/XMF3
UUUPL(1)=0.
TCORD(1)=0.
UDEF(1)=0.
NONDEL(1)=0.
XMF4=EPS*XNUE*UE*UE*(RMI**J)*XL3(1)*FZ3(1)/DZ

C
C
CALCULATE BASIC BOUNDARY LAYER PARAMETERS
C

KON=IE+2
DO 37 N=2,KON
IF (TRFACT.EQ.0.0) GO TO 36
UPLUS=SQRT(XMF4*T3(1))
UUUPL(N)=UE*F3(N)/UPLUS
TCORD(N)=(Y(N)*UPLUS*RE)/(EPS*XNUE*((T3(N)*XL3(N))**2))
UDEF(N)=UE*(1.-F3(N))/UPLUS
36 CONTINUE
TTOTT(N)=(2.*T3(N)+XAL*F3(N)*F3(N))/XMF1
CRDCCO(N)=(TTOTT(N)-XMF2)/XMF3
MOME(N)=F3(N)/SQRT(T3(N))
37 CONTINUE

```

```

C
C      CALCULATE VORTICITY REYNOLDS NUMBER
C      AND DETERMINE STABILITY INDEX
C
C      IF (TRFACT.GT.0.0.AND.TRFACT.LT.0.9999) GO TO 40
DO 38 I=1,NEDGE
TERM3B=RE*RE*UE*UE*Y(I)*Y(I)*(RMI*RATO3(I))**J/(SQRT(2.*X)*XNUE*EPS
1)
38 STAB2(I)=TERM3B*FZ3(I)/(XL3(I)*T3(I)**3)
ST2MAX=STAB2(1)
DO 39 IX=2,IE
IF (ST2MAX.GT.STAB2(IX)) GO TO 39
ST2MAX=STAB2(IX)
39 CONTINUE
SMXP=ST2MAX
40 CONTINUE
DSMXD=(SMXP-SMXN)/(S-SM1)
SMXN=SMXD
SMXD=SMXP
IF (KTC00.EQ.2.OR.KTC0.EQ.1) GO TO 41
KTC0=1
RRRR=RE*UE*R1*U1/(XNUE*VISREF)
TLNGTH=1.+(.5.*RRRR**(-1.)*(RRRR*A*SST)**.8)/SST
41 CONTINUE
IF (SMXTR.LE.ST2MAX) CALL TURBLNT (T3,XL3,FZ3,RATO3,Y,EP3,F3,EH3,V
1ARA,VARB,VARC,VARD,VARE,KODAMP,IYINT,YEDGE,TAUP)
IF (SST.LE.S*A) CALL TURBLNT (T3,XL3,FZ3,RATO3,Y,EP3,F3,EH3,VARA,V
1ARB,VARC,VARD,VARE,KODAMP,IYINT,YEDGE,TAUP)
IF (DIF.GT.CONV) GO TO 32
C
C      OUTPUT QUANTITIES
C
DO 42 N=2,KDN
NONDEL(N)=Y(N)/YEDGE
42 CONTINUE
IF (J.NE.1) GO TO 44
TIBURON=2.*DISP/RMI
IF(TIBURON.LT.-1.)GO TO 43
DISP=RMI*(-1.+SQRT(1.+TIBURON))
GO TO 44
43 WRITE(6,93)
44 CONTINUE
THADIS=DISP/THETA
REDELT=(RE*UE*DISP/(XNUE*A))*REYREF
RETHET=REDELT/THADIS
RES=(RE*UE*S/XNUE)*KEYREF
XMAE=UE/SQRT(TE*(G-1.))
TWOTT1=T3(1)*TE*TREF/TT1
RFCTOR=(T3(1)-1.)/((TT1/(TE*TREF))-1.)
TAUD=VISREF*U1*(XL3(1)*RE*XNUE*UE*UE*(RMI**J)*FZ3(1)/DZ)/(EPS*A)
CFE=TAUD/(.5*R1*J1*U1*RE*UE*UE)
CFW=CFE*TW/TE
IF (KUDWAL.NE.1) GO TO 45
QS=-XL3(1)*RE*UE*TE*XNUE*(RMI**J)*TZ3(1)/(PR*DZ*EPS)

```

```

QSD=QS*VISREF*U1*U1/(778.26*A)
GU TO 46
45 QSD=QW
46 CONTINUE
IF(FZ3(1).GE.0.) GO TO 92
WRITE(6,91)S,TAUD,QSD
STOP 400
92 CONTINUE
TWD=TREF*TW
TAWD=(RFL+(RFT-RFL)*TRFACT)*(TT1-TE*TREF)+TE*TREF
HD=QSD/(TWD-TAWD)
CHE=778.26*HD*(G-1.)/(G*R*R1*U1*RE*UE)
CHW=CHE*TW/TE
HSD=HD*A*S
KED=R*VISREF*XNUE*G/(778.26*PR*(G-1.))
KWD=KED*XL3(1)*T3(1)
NUE=HSD/KED
NUW=HSD/KWD

```

```

C          TOTAL PRESSURE RATIO, (PT2)BL/(PT2)REF
C

```

```

DO 49 I=1,IE
ZEB=(MOME(I)*XMAE)**2
IF (SQRT(ZEB)-1.) 47,47,48
47 PT2=PE*((1.+(G-1.)*ZEB/2.)**(G/(G-1.)))
GO TO 49
48 BBA=(ZEB*(G+1.)/2.)**(G/(G-1.))
BBB=((G+1.)/((2.*G*ZEB)-(G-1.)))**(1./(G-1.))
PT2=PE*BBA*BBB
49 PTJPT(I)=PT2/PTREF

```

```

C          VARIABLE ENTROPY CALCULATIONS
C

```

```

GO TO (51,50), IENTRO
50 INTEGL=INTEGR(F3,NEDGE,DN)
XXJ=J
RS=((J+1)*EPS*DZ*INTEGL)**((2.-XXJ)/2.)
IPT=-1
CALL IUNI (JL,NNN,KRS,2,0VT,2,RS,ANS,IPT,IERR)
ZS=ANS(1)
TANTHTS=ANS(2)
THATS=ATAN(TANTHTS)
SWANG=THATS/.0174533
PTTWO=(G+1.)*XMA**2*SIN(THATS)**2
PTTWO=PTTWO/((G-1.)*(XMA)**2*SIN(THATS)**2+2.)
PTTWO=PTTWO**(G/(G-1.))*PT1
PTTWO=PTTWO*((G+1.)/(2.*G*XMA**2*SIN(THATS)**2-(G-1.)))**(1./(G-1.))
P20=PTTWO/(R1*J1*U1)
UEE(M)=SQRT(2.*T10*(1.-(PE/P20)**((G-1.)/G)))
XVAL2=ABS((UEE(M)-UE)/UE)
IF(XVAL2.GE.XVAL1) XMX=XVAL2
XVAL1=XVAL2
NN=IE+2

```

51 CONTINUE  
NN=IE+2  
IF (IENTRO.EQ.1) P20=P10  
C  
C PRINT PROFILES AND WALL VALUES  
C  
KPRNT=0  
IF (ABS(A-1.).LE.0.0000001) GO TO 52  
S=S\*A  
Z=Z\*A  
RMI=RMI\*A  
ZS=ZS\*A  
RS=RS\*A  
52 CONTINUE  
DO 53 NUMBR=1,JN  
IF (S.GT.PROVAL(NUMBR)-.000001.AND.S.LT.PROVAL(NUMBR)+.000001) GO  
1TO 54  
53 CONTINUE  
GO TO 63  
54 CONTINUE  
IF (KODUNIT.EQ.1) S=S\*.3048  
WRITE (6,73) S  
IF (KODUNIT.EQ.1) S=S/.3048  
IEDGEX=NEDGE+10  
IF (IEDGEX.GT.IE) IEDGE=IE  
IF (NAUXPRO.NE.1) GO TO 56  
WRITE (6,74)  
DO 55 I=1,IEDGEX  
55 WRITE (6,75) (XN(I),TAUP(I),V3(I),FZ3(I),TZ3(I),VARA(I),VARB(I),VA  
1RL(I),VARD(I),EP3(I),VARE(I))  
56 CONTINUE  
IF (KUDE.EQ.1) GO TO 58  
IF (TRFACT.GT.0.9999) GO TO 61  
IF (TRFACT.GT.0.0.AND.TRFACT.LT.0.9999) GO TO 58  
WRITE (6,76)  
DO 57 I=1,IEDGEX  
57 WRITE (6,77) XN(I),NONDEL(I),F3(I),T3(I),TTOTT(I),CROCCO(I),PTOPT(1  
II),MOME(I),FZ3(I),TZ3(I),STAB2(I),XL3(I)  
GO TO 63  
58 WRITE (6,76)  
DO 59 I=1,IEDGEX  
59 WRITE (6,77) XN(I),NONDEL(I),F3(I),T3(I),TTOTT(I),CROCCO(I),PTOPT(1  
II),MOME(I),FZ3(I),TZ3(I),STAB2(I),XL3(I)  
WRITE (6,78)  
DO 60 I=1,IEDGEX  
60 WRITE (6,77) XN(I),NONDEL(I),F3(I),T3(I),TTOTT(I),CROCCO(I),PTOPT(1  
II),MOME(I),TCORD(I),UDUPL(I),UDEF(I),EP3(I)  
GO TO 63  
61 WRITE (6,78)  
DO 62 I=1,IEDGEX  
62 WRITE (6,77) XN(I),NONDEL(I),F3(I),T3(I),TTOTT(I),CROCCO(I),PTOPT(1  
II),MOME(I),TCORD(I),UDUPL(I),UDEF(I),EP3(I)

```
63 CONTINUE
  DO 64 NUMBER=1,JM
    IF (S.GT.PRNTVAL(NUMBER)-.000001.AND.S.LT.PRNTVAL(NUMBER)+.000001)
      1 GO TO 65
  64 CONTINUE
    GO TO 66
  65 CONTINUE
    PESTAR=PE*R1*U1*U1
    TESTAR=TE*TREF
    RESTAR=RE*R1
    UESTAR=UE*U1
    MUESTAR=XNUE*VISREF
    YESTAR=YEDGE*EPS*A
    RVWAL=RVWALD/(RESTAR*UESTAR)
    GANDOG=RVWALD
    IF(KODUNIT.EQ.1)GANDOG=GANDOG/.0063658804
    IF (KODUNIT.EQ.1) CALL WALLOUT (PRUVAL,PRNTVAL,JM,JN)
    WRITE (6,79) S,RETHET,PP,CFW,ZS,YESTAR,X,RES,DTEDS,QSD,RS,UPLUS,RM
    1I,PESTAR,DUEOS,HQ,NDIT,TRFACT,Z,TESTAR,DISP,CHE,TWDTT1,JPOINT,XBE,
    2RESTAR,THETA,CHW,RFCTDR,P20
    WRITE (6,80) XAL,UESTAR,THAD1S,NUE,ST2MAX,EPS,GANDOG,XMAE,TAUD,NUW
    1,DSMXD,REDELT,MUESTAR,CFE,SWANG,V3(1),RVWAL,NIT,DIF1
    KPRNT=1
  66 CONTINUE
    AINV=1./A
    IF (KODUNIT.EQ.1.AND.KPRNT.EQ.1) AINV=AINV*3.280839895
    S=S*AINV
    Z=Z*AINV
    RMI=RMI*AINV
    ZS=ZS*AINV
    RS=RS*AINV
C
C          UPDATE VARIABLES FOR MARCHING PROCEDURE
C
    DO 67 N=1,NN
      F1(N)=F2(N)
      T1(N)=T2(N)
      V1(N)=V2(N)
      RAT01(N)=RAT02(N)
      DRAT01(N)=DRAT02(N)
      XL1(N)=XL2(N)
      XLP1(N)=XLP2(N)
      F2(N)=F3(N)
      T2(N)=T3(N)
      V2(N)=V3(N)
      RAT02(N)=RAT03(N)
      DRAT02(N)=DRAT03(N)
      XL2(N)=XL3(N)
      XLP2(N)=XLP3(N)
      TZ2(N)=TZ3(N)
      EP1(N)=EP2(N)
      EP2(N)=EP3(N)
      EP3M=EP3(N)
      IF (N.GT.1.AND.N.LT.1E) EP3M=(EP3(N-1)+EP3(N)+EP3(N+1))/3.
```

```

TAUP(N)=1./(XL3(1)*FZ3(1))*XL3(N)*ABS(FZ3(N))*EP3M
EH1(N)=EH2(N)
EH2(N)=EH3(N)
FZ2(N)=FZ3(N)

```

```

67 CONTINUE
68 DX1=DX2
  IF (IENIT.EQ.1) STOP 100
  IF (NOIT.EQ.ITMAX) WRITE(5,89)
  IF (NOIT.EQ.ITMAX) STOP 200
  IF (XMX.LE.CONVE) WRITE(6,90)
  IF (XMX.LE.CONVE) STOP 300
  NOIT=NOIT+1
  WRITE(6,86) ITMAX,NOIT
  REWIND 4
  GO TO 10

```

C  
C  
C

```

69 FORMAT (1H1,20X,64H****DIMENSIONAL OUTPUT QUANTITIES ARE IN U.S. S
1TANDARD UNITS****,/)
70 FORMAT (1H1,20X,55H****DIMENSIONAL OUTPUT QUANTITIES ARE IN S.I. U
INITS****,/)
71 FORMAT (2X,30HFREE STREAM VALUES-DIMENSIONAL,/,,5X,5HPT1 *,E14.6,2X
1,5HTT1 *,E14.6,2X,5HRT1 *,E14.6,2X,5H P1 *,E14.6,2X,7H T1=,E14.
26,2X,5H R1 *,E14.6,/,5X,5H U1 *,E14.6,2X,5HAA1 *,E14.6,2X,5HXMA *,E
3E14.6,2X,5HREY *,E14.6,/,2X,28HREFERENCE VALUES-DIMENSIONAL,/,,5X,
55HPREF=,E14.6,2X,5HTREF=,E14.6,2X,5HRREF=,E14.6,2X,5HUREF=,E14.6,2
6X,7HVISREF=,E14.6,2X,5HPTK =,E14.6,/,2X,25HPARAMETERS-NONDIMENSION
7AL,/,,5X,5HP10 *,E14.6,2X,5HT10 =,E14.6,2X,5HR10 =,E14.6,/,)
72 FORMAT (2X,5HMUE *,E12.0,2X,5HUE *,E12.6,2X,5HTE *,E12.6,2X,5HPE
1 *,E12.6,2X,5HQSD *,E12.6,/,2X,5HXAL *,E12.6,2X,5HXBE *,E12.6,2X,
25HRE *,E12.6)
73 FORMAT (//1X,2HS=F14.4,9H PROFILE/)
74 FORMAT (130H          ETA          TAUP          V          GRAD(U/UE)  GRAD
1(T/TE)      FC1          DAMP          EPI          EPO          EP
2      MIXDEL//)
75 FORMAT (11E12.3)
76 FORMAT (//4X,3HETA,8X,4HY/YE,7X,4HU/UE,7X,4HT/TE,6X,6HTT/TTE,5X,6H
1CRDCC0,5X,6HPT/ PTR,6X,4HM/ME,8X,2HFZ,9X,2HTZ,6X,7HVORTREY,6X,5HXLM
211/)
77 FORMAT (12E11.3)
78 FORMAT (//4X,3HETA,8X,4HY/YE,7X,4HU/UE,7X,4HT/TE,6X,6HTT/TTE,5X,6H
1CRDCC0,5X,6HPT/ PTR,6X,4HM/ME,7X,5HYPLUS,6X,5HUPLUS,6X,4HUDEF,6X,6H
2V1SEFF//)
79 FORMAT (/2X,7HS      *,E12.5,2X,7HRETHET=,E12.5,2X,7HDPEDS=,E12.5,
12X,7HCFW=,E12.5,2X,7HLSHK=,E12.5,2X,7HYE=,E12.5,/,2X,7HXI
2=,E12.5,2X,7HRES=,E12.5,2X,7HDTEDS=,E12.5,2X,7HQSD=,E12.
35,2X,7HRSHK=,E12.5,2X,7HUTAU=,E12.5,/,2X,7HRMI=,E12.5,2X,7HP
4E=,E12.5,2X,7HDUEDS=,E12.5,2X,7HHD=,E12.5,2X,7HITRD=,I1
52,2X,7HTRFCFT=,E12.5,/,2X,7HZ=,E12.5,2X,7HTE=,E12.5,2X,7HD
6LTAST=,E12.5,2X,7HNSTE=,E12.5,2X,7HTW/TT1=,E12.5,2X,7HYMP=,I1
72,/,2X,7HBETA=,E12.5,2X,7HRE=,E12.5,2X,7HTHETA=,E12.5,2X,7HN
85TW=,E12.5,2X,7HRFTRUE=,E12.5,2X,7HP20=,E12.5)
```

```

80 FORMAT(2X,7HXAL *,E12.5,2X,7HUE *,E12.5,2X,7HFORM *,E12.5,2
1X,7HNUE *,E12.5,2X,7HRHOUSE *,E12.5,2X,7HUMEGA *,E12.5,/2X,7HRVWA
2LD=,E12.5,2X,7HME *,E12.5,2X,7HTAUD *,E12.5,2X,7HNUW *,E12.5
3,2X,7HDSMXO *,E12.5/2X,7HREDELT=,E12.5,2X,7HMUE *,E12.5,2X,7HCFE
4 *,E12.5,2X,7HSWANG *,E12.5,2X,7HVW *,E12.5,2X,7HRVWAL *,E12.
55/2X,7HNOITER=,I12,2X,7HERRUR *,E12.5)
81 FORMAT(/2X,8HMIISTAKE=,E12.5,37H MISTAKE=ABSOLUTE VALUE OF 1.-PE/
1P10/10X,106HYOU HAVE MADE AN ERROR IN YOUR INPUT SUCH THAT THE RAT
2IO OF STATIC TO TOTAL PRESSURE IS GREATER THAN UNITY/11X,66HERROR
3COULD INVOLVE EITHER OR ALL OF THE FOLLOWING:XMA,PT1,PE,WAVE//12X,
497HTHE PROBABILITY IS VERY HIGH THAT YOUR SPECIFIED VALUE OF PE(1)
5 IN $NAM3 IS NOT CORRECT FOR YOUR /,12X,40HSELECTED VALUES OF XMA,P
6T1,WAVE IN $NAM2./,12X,27HPE/P10 CANNOT EXCEED UNITY./)
82 FORMAT(1H1,2X,54$NAM1,/,2X,8HIGEOM *,I12,2X,8HXEND *,E12.5,2X,
18HIE *,I12,2X,8HXX *,E12.5,2X,8HDETA1 *,E12.5,2X,8HXMA
2 *,E12.5,/2X,8HPRT1 *,E12.5,2X,8HTT1 *,E12.5,2X,8HIGAS *,I
312,2X,8HVVIS1C1 *,E12.5,2X,8HVVIS1C2 *,E12.5,2X,8HVVIS2C1 *,E12.5,/2
4X,8HVVIS2C2 *,E12.5,2X,8HG *,E12.5,2X,8HK *,E12.5,2X,8HPR
5 *,E12.5,/,2X,8HIBODY *,I12,2X,8HWAVE *,E12.5,2X,8PHPII
6 *,E12.5,2X,8HJ *,I12,2X,8HW *,I12,2X,8HIENTRO *,I12,/12
7X,8HSST *,E12.5,2X,8HSMXTR *,E12.5,2X,8HKODVIS *,I12,2X,8HKTCO
8D *,I12,2X,8HTLNGTH *,E12.5,2X,8HIYINT *,I12,/,2X,8HKODAMP *,I12
9,2X,8HXT1 *,E12.5,2X,8HXT2 *,E12.5,2X,8HXT3 *,E12.5,2X,8H
1XT4 *,E12.5,2X,8HXT5 *,E12.5,/,2X,8HXT6 *,E12.5,2X,8HPRT
2 *,E12.5,2X,8HKODPRT *,I12,2X,8HNUMB1 *,I12,2X,8HGLAR *,E12.5
4,/,2X,8HPRTAR /(10E12.5))
83 FORMAT(/,2X,8HIEND1 *,I12,2X,8HPROINC *,E12.5,2X,8HPRNTINC=,E12.5
1,2X,8HIPRO *,I12,2X,8HPRNT *,I12,2X,8HNAUXPKD=,I12,/,2X,8HFT
1 *,E12.5,2X,8HKODE *,I12,2X,8HKOUWAL *,I12,2X,8HVELEDG *,E12.5
1,2X,8HCNV *,E12.5,2X,8HNITMAX *,I12,/,2X,8HKODUNIT=,I12,2X,8HIT
2MAX *,I12,2X,8HCNV *,E12.5,/,2X,119HTHIS COMPLETES THE OUTPUT
3 OF $NAM1 WITH THE EXCEPTION OF PROVAL AND PRNTVAL. THESE VALUES A
4RE PRINTED JUST PRIOR TO THE /,2X,22HINITIAL STATION PRINT.)
84 FORMAT(2X,6HPROVAL,/(10E12.5))
85 FORMAT(2X,8HPRNTVAL /(10E12.5))
86 FORMAT(/,35X,50*****)
1*,/35X,1H*,10X,28HVARIBLE ENTROPY CALCULATIONS,10X,1H*,/,35X,1H*,1
21X,6HITMAX=,I8,2X,5HNOIT=,I8,8X,1H*,/,35X,1H*,48X,1H*,/,35X,50H***
3*****)
87 FORMAT(/,2X,63HPRINT STATIONS DESIGNATED IN $NAM1 INPUT AND GENERA
TED IN SETUP,/)
88 FORMAT(/,2X,125HFOR YOUR VARIABLE ENTROPY CASE (IENTRO=2) THE FIRST
1 PASS OVER THE BODY IS EQUIVALENT TO A CONVERGED CONSTANT ENTROPY(
2IENTRO=1)/,2X,92HSOLUTION. VARIABLE ENTROPY EFFECTS ARE TREATED IN
3SUBSEQUENT PASSES; THAT IS FOR NOIT=1,2,...)
89 FORMAT(/,2X,117HYOUR VARIABLE ENTROPY CASE HAS NOT CONVERGED FOR YO
UR INPUT VALUES OF CONVE AND ITMAX. YOU MUST EITHER INCREASE ITMA
2X,/,2X,66HOR REDUCE YOUR CONVERGENCE LEVEL BY INCREASING THE VALUE
3 OF CONVE.)
90 FORMAT(/,2X,77HYOUR VARIABLE CASE ENTROPY IS CONVERGED TO YOUR SELE
CTED INPUT VALUE OF CONVE.)
91 FORMAT(2X,47HBOUNDARY-LAYER SEPARATION INDICATED BY SOLUTION,/,2X,
12HS=,E12.5,2X,5HTAUD=,E12.5,2X,4HQSD=,E12.5)

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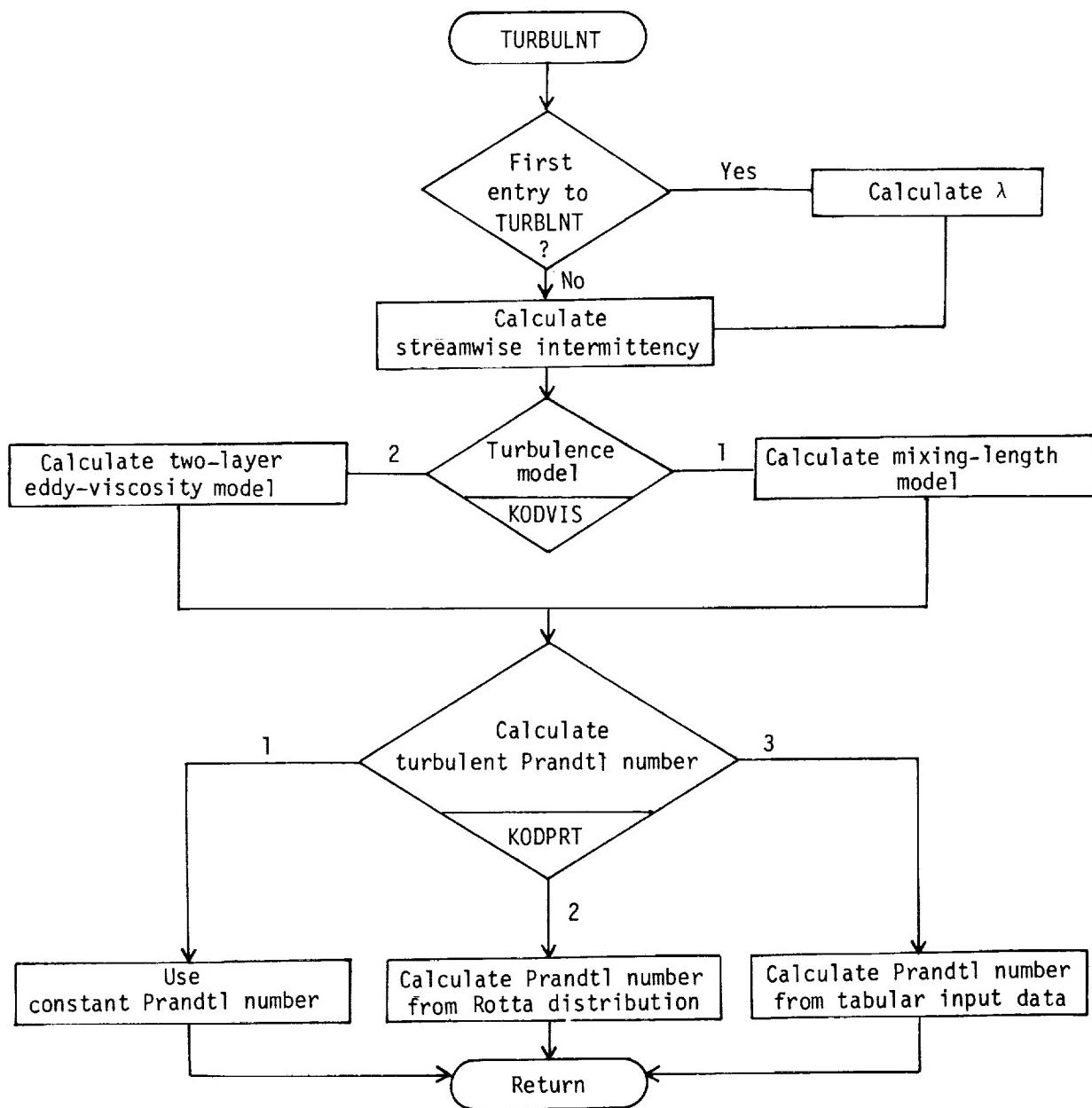
APPENDIX C

93 FORMAT(1H1,2X,61HFOR J=1 D1SP IS DEFINED AS (SEE AIAA PAPER NO. 69-  
1687) FOLLOWS, //,4X,41H0ISP=RMI\*(-1.+SQRT(1.+2.\*DISP(J=0)/RMI))),//  
2,2X,109HFOR YOUR CURRENT S-STATION DISP(J=0) IS NEGATIVE(ALLOWED)  
3AND 2.\*DISP(J=0)/RMI IS LESS THAN -1.(NOT ALLOWED);,/,2X,112HCONSE  
4QUENTLY, THE VALUE PRINTED ABOVE IS DISP(J=0) WHERE DISP(J=0) IS TH  
5E TWO DIMENSIONAL DEFINITION. THE PROBLEM,/,2X,111HNORMALLY OCCURS  
6 FOR (1)EXTREMELY FINE DS NEAR S=0. FOR BLUNT BODIES WHERE RMI IS  
7VERY SMALL; (2) FLOW OVER VERY,/,2X,110HSLENDER BODY OF REVOLUTION  
8(NEEDLE). THE PROBLEM IS EASILY SOLVED BY REFINED GRID DISTRIBUTIO  
9N. HOWEVER, IF YOURE NOT INTERESTED IN THE TWO ABOVE ME  
1NTIONED CASES, IGNORE THIS MESSAGE AND PROBLEM WILL CURE ITSELF,/,2  
2X,50HAS S INCREASES FOR ALL PHYSICALLY REALISTIC FLOWS.)  
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## Subroutine TURBLNT

Subroutine TURBLNT calculates either the eddy viscosity or mixing-length parameters required for the transitional and/or turbulent boundary-layer equations. The flow chart for subroutine TURBLNT is as follows:



## APPENDIX C

The program listing for subroutine TURBLNT is as follows:

```
SUBROUTINE TURBLNT (T3,XL3,FZ3,RATO3,Y,EP3,F3,EH3,VARA,VARB,VARC,V
1ARD,VARE,KODAMP,IYINT,YEDGE,TAUP)
DIMENSION VARA(JK), VARB(JK), VARC(JK), VARD(JK), VARE(JK), Y(JK),
1 T3(JK), XL3(JK), FZ3(JK), RATO3(JK), EP3(JK), F3(JK), EH3(JK), TA
2UP(JK)
DIMENSION PRTAR(JI), GLAR(JI), DVT(JI,1)
EQUIVALENCE (PRTAR,DVT(1,1))
COMMON /TRBULNT/ S,KSTR,TLNGTH,TRFACT,DISINC,XT1,XT2,XT6,XT3,XT4,X
1T5,PRTW,RE,UE,XNUE,J,RMI,EPS,JPOINT,IE,WW1,WW2,WW3,WW4,WW5, NEDGE
2,KODVIS,A,XBE,X,PR,KODPRT,PRT,PRTAR,GLAR,NUMB1,XK
COMMON /UNIT/ VIS1C1,VIS1C2,VIS2C1,VIS2C2,PT1,TT1,WAVE,R,PHIO,DS,S
1ST,RT1,P1,T1,R1,U1,AA1,TREF,VISREF,PESTAR,TESTAR,RESTAR,UESTAR,MUE
2STAR,YESTAR,THETA,TAUD,QSD,HD,UPLUS,DISP,PE,Z,TW,QW,RVWALD,PROINC,
3PRNTINC,ZS,RS
GO TO (1,2), KSTR+1
1 KSTR=1
PRTW=PRT
STR=S
XLAMDA=STR*(TLNGTH-1.)/(SQRT((ALOG(50.))/412))
2 CONTINUE
C
C          CALCULATE STREAMWISE INTERMITTANCY
C
SNORM=.412*((S-STR)/XLAMDA)**2
TRFACT=1.
IF (SNORM.LT.20.) TRFACT=1.-EXP(-SNORM)
C
C          CALCULATE EDDY-VISCOSITY
C          2 LAYER MODEL
C
IFC=0
A2=RE*RE*UE*UE*(RMI**J)*XL3(1)*FZ3(1)/(SQRT(2.*X)*XNUE*EPS)
A3=RE*RE*UE*UE*(RMI**J)/(A*A*EPS*EPS*EPS*XNUE*SQRT(2.*X))
A4=RE*UE*XT2*DISINC/(EPS*EPS*XNUE*A)
A5=SQRT(A2/(XL3(1)*XL3(1)*T3(1)**3))
NDAMP=0
DO 8 N=2,IE
ERA=XT3*((Y(N)/YEDGE)-XT4)
CALL ERF (ERA,ERB)
YINTER=.5*(1.-ERB)
IF (IYINT.EQ.1) YINTER=1.
IF (IFC.EQ.1) GO TO 3
YPLUS=Y(N)*SQRT(A2/(XL3(N)*XL3(N)*T3(N)**3))
IF (KODAMP.EQ.2) YPLUS=Y(N)*A5
DAMP=1.
B2=-YPLUS/XT6
IF (NDAMP.EQ.0) DAMP=1.-EXP(B2)
IF (DAMP.GT.0.9999.AND.NDAMP.EQ.0) NDAMP=1
VARA(N)=A3*(RATO3(N)**J)*ABS(FZ3(N))/(XL3(N)*T3(N)**3)
VARB(N)=DAMP
IF (KODVIS.EQ.1) GO TO 4
```

```

XMIXL=XT1*A*Y(N)*DAMP*EPS
EP1=1.+TRFACT*VARA(N)*XMIXL*XMIXL
VARC(N)=EP1
3 CONTINUE

C
C
C      OUTER EDDY VISCOSITY LAW
C
C
EP2=1.+TRFACT*A4*YINTER/(XL3(N)*T3(N)*T3(N))
VARD(N)=EP2
IF (IFC.EQ.1) GO TO 6
IF (EP1.LE.EP2.AND.IFC.EQ.0) GO TO 5
IFC=1
JPOINT=N
GO TO 6

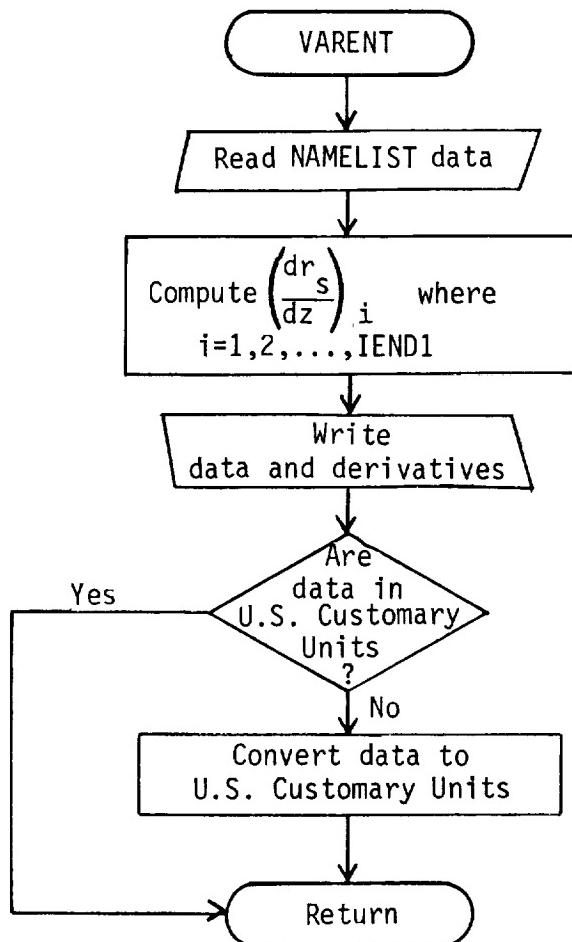
C
C      MIXING LENGTH MODEL
C
4 CONTINUE
YRAT=1.
IF (Y(N).LE.YEDGE) YRAT=Y(N)/YEDGE
XMIXL=XT5*TANH(XT1*YRAT/XT5)*EPS*A*YEDGE*DAMP
EP3(N)=1.+TRFACT*YINTER*VARA(N)*XMIXL*XMIXL
GO TO 7
5 EP3(N)=EP1
GO TO 7
6 EP3(N)=EP2
7 CONTINUE
VARE(N)=XMIXL/YEDGE
8 CONTINUE

C
C      CALCULATE TURBULENT PRANDTL NUMBER
C
DO 12 N=2,IE
GO TO (11,9,10), KODPRT
9 PRT=PRTW-PRTW*.5*((Y(N)/YEDGE)**2)
IF (Y(N).GE.YEDGE) PRT=PRTW*.5
GO TO 11
10 GL=Y(N)/YEDGE
IF (GL.GT.1) GL=1.
CALL IUNI (JI,NUMB1,GLAR,1,DVT,2,GL,PRT,IPT,IERR)
11 EH3(N)=(PRT+(EP3(N)-1.)*PR)/(PR*PRT)
12 CONTINUE
DO 13 N=2,IE
IF (EP3(N).LT.1.) EP3(N)=1.
13 CONTINUE
VARA(1)=VARA(2)
VARB(1)=0.
VARC(1)=1.
VARD(1)=VARD(2)
VARE(1)=0.
RETURN
END

```

Subroutine VARENT

Subroutine VARENT reads the variable-entropy input (coordinates for shock wave; see fig. 2), computes the derivatives  $dR_S/dz$ , and writes the input and derivatives. The flow chart for subroutine VARENT is as follows:



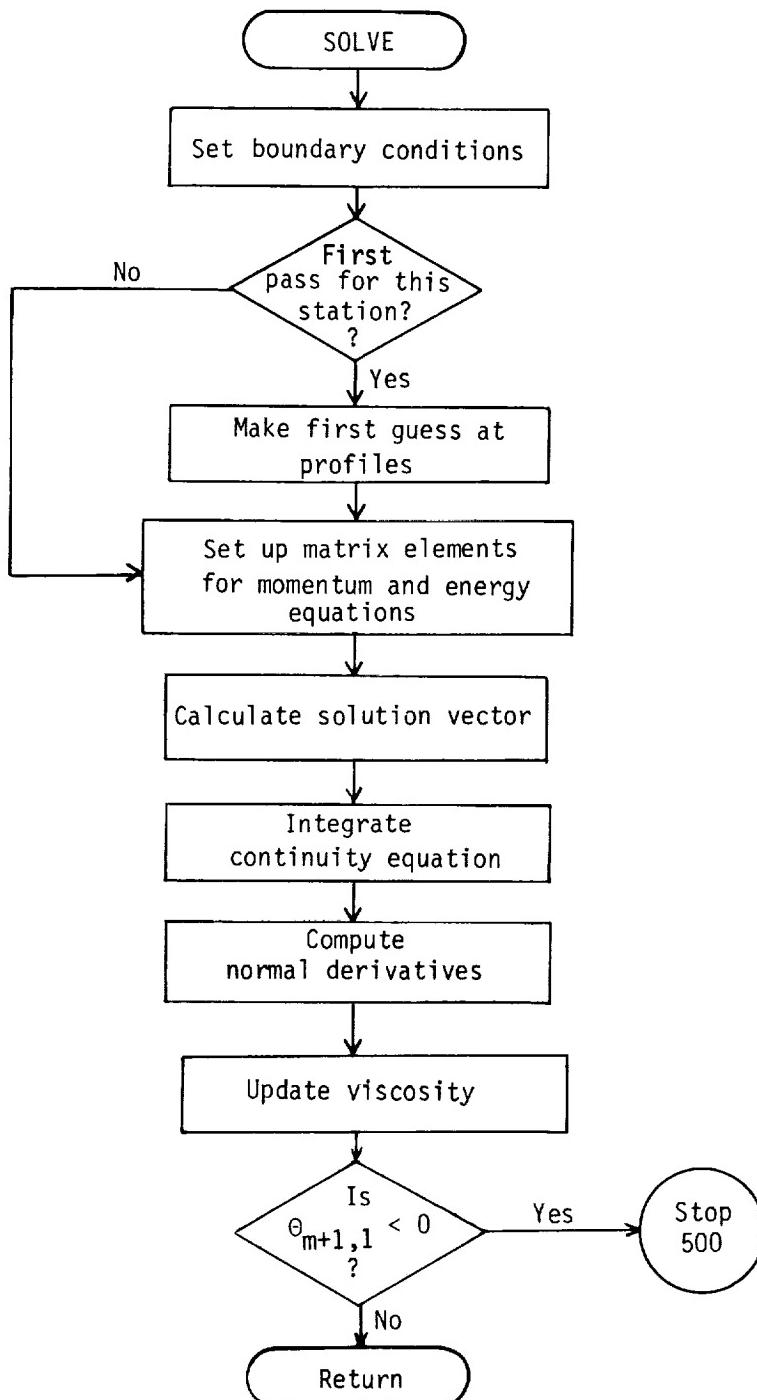
The program listing for subroutine VARENT is as follows:

```
SUBROUTINE VARENT (RRS,ZZS,DRSDZS,NUMBER,KODUNIT,A)
DIMENSION RRS(JL), ZZS(JL), DRSDZS(JL)
NAMELIST /NAM3/ NUMBER,RRS,ZZS,DRSDZS
READ (5,NAM3)
NUMM1=NUMBER-1
DO 1 I=2,NUMM1
1 DRSDZS(I)=(RRS(I+1)-RRS(I-1))/(ZZS(I+1)-ZZS(I-1))
DRSDZS(1)=(RRS(2)-RRS(1))/(ZZS(2)-ZZS(1))
DRSDZS(NUMBER)=(RRS(NUMBER)-RRS(NUMBER-1))/(ZZS(NUMBER)-ZZS(NUMBER
1-1))
WRITE(6,3) NUMBER,RRS
WRITE(6,4) ZZS
WRITE(6,5) DRSDZS
C5=1.
IF (KODUNIT.EQ.1) C5=3.28083985
C6=C5/A
DO 2 I=1,NUMBER
RRS(I)=RRS(I)*C6
ZZS(I)=ZZS(I)*C6
2 CONTINUE
3 FORMAT(2X,5H$NAM3,/,2X,8HNUMBER =,I12,/,2X,3HRRS,/,10E12.5)
4 FORMAT(2X,3HZZS,/,10E12.5)
5 FORMAT(2X,6HDRSDZS,/,10E12.5)
RETURN
END
```

APPENDIX C  
Subroutine SOLVE

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Subroutine SOLVE is the main subroutine of program VGBLP wherein the nonsimilar laminar, transitional, and/or turbulent boundary-layer equations are solved using a coupled algorithm for the energy and momentum equations. The continuity equation is solved using the trapezoidal rule. An iterative loop is provided to assure convergence of the system of equations to a preselected value. The flow chart for subroutine SOLVE is as follows:



The program listing for subroutine SOLVE is as follows:

```

SUBROUTINE SOLVE (KODWAL,ARGM,TR,VIS2C2,XAL,XBE,X3,DX2,TW,IGAS,IE,
1J,NIT,RVWALD,R1,U1,WW1,WW2,WW3,WW4,WW5,XNUE,XK,EPS,M,IBODY,FT)
COMMON /SOLV1/ F1(JK),F2(JK),F3(JK),T1(JK),T2(JK),T3(JK),V1(JK),V2
1(JK),V3(JK),EP2(JK),EP3(JK),FZ2(JK),FZ3(JK),TZ2(JK),TZ3(JK),XL2(JK
2),XL3(JK),XLP2(JK),XLP3(JK),RATO1(JK),RATO2(JK),RATO3(JK),EH2(JK),
3EH3(JK),DRATO1(JK),DRATO2(JK),DRATO3(JK),VARA(JK),VARB(JK),VARC(JK
4),VARD(JK),VARE(JK),Y(JK),EP1(JK),EH1(JK),XL1(JK),XLP1(JK)
COMMON /SOLV2/ Z1,Z2,Z3,Z4,Z5,TE,FAA,FAB,FAC,FAD,BEX1,BEX2,BEX3,BE
1X4
COMMON /MESH1/ XN(JK),DN(JK),Y1(JK),Y2(JK),Y3(JK),Y4(JK),Y5(JK),Y6
1(JK)
DIMENSION XK1(JK), XK2(JK), XK3(JK), XM1(JK), XM2(JK), XM3(JK)

C THIS SUBROUTINE SOLVES THE COMPLETE B.L. EQUATIONS
C
C SET UP THE BOUNDARY-CONDITIONS
XK1(1)=XK2(1)=XK3(1)=XM2(1)=XM3(1)=0.
IF (KODWAL.EQ.1) GO TO 1
T23(1)=ARGM/XL3(1)
GO TO 2
1 CONTINUE
XM1(1)=TW/TE
T3(1)=XM1(1)
2 CONTINUE
F3(1)=0.
IF (NIT.GT.1) GO TO 6
C MAKE FIRST GUESS AT THE CURRENT STATION PROFILES
C
DO 5 N=2,IE
T3(N)=Z4*T2(N)-Z5*T1(N)
F3(N)=Z4*F2(N)-Z5*F1(N)
IF (T3(N).LT.0.) WRITE (6,18) T3(N),N,M
IF (T3(N).LT.0.) T3(N)=.5*(T2(N)+T1(N))
RATO3(N)=Z4*RATO2(N)-Z5*RATO1(N)
IF (IGAS.EQ.2) GO TO 3
XL3(N)=((1.+TR)*SQRT(T3(N))/(T3(N)+TR))
XLP3(N)=XL3(N)*(TR-T3(N))/(2.*T3(N)*(T3(N)+TR))
GO TO 4
3 CONTINUE
XL3(N)=T3(N)**(VIS2C2-1.)
XLP3(N)=(VIS2C2-1.)*(T3(N)**(VIS2C2-2.))
4 CONTINUE
TZ3(N)=TZ2(N)
FZ3(N)=FZ2(N)
EP3(N)=EP2(N)
V3(N)=Z4*V2(N)-Z5*V1(N)
EH3(N)=EH2(N)
5 CONTINUE
6 CONTINUE
IM=IE-1

```

```

C      SET UP MATRIX ELEMENTS
C
C      DO 8 N=2,IM
C
C      MOMENTUM EQUATION
C
A11=X3*F3(N)/DX2*FT
A12=V3(N)/(DN(N)+DN(N-1))
CLEBP=.5*RATO3(N+1)**(2*J)*XL3(N+1)*EP3(N+1)+.5*RATO3(N)**(2*J)*XL
13(N)*EP3(N)
CLEBM=.5*RATO3(N-1)**(2*J)*XL3(N-1)*EP3(N-1)+.5*RATO3(N)**(2*J)*XL
13(N)*EP3(N)
A13=XBE
A14=-XBE*F3(N)**2
A1=-A12-Y3(N)*CLEBM
B1=A11*Z1+Y1(N)*CLEBP+Y3(N)*CLEBM+2.*A13*F3(N)
C1=A12-Y1(N)*CLEBP
D1=0.
E1=-A13
H1=0.
G1=A11*(Z2*F2(N)-Z3*F1(N))-A14
C
C      ENERGY EQUATION
C
CLEHP=.5*RATO3(N+1)**(2*J)*XL3(N+1)*EH3(N+1)+.5*RATO3(N)**(2*J)*XL
13(N)*EH3(N)
CLEHM=.5*RATO3(N-1)**(2*J)*XL3(N-1)*EH3(N-1)+.5*RATO3(N)**(2*J)*XL
13(N)*EH3(N)
A15=XAL*XL3(N)*EP3(N)*RATO3(N)**(2*J)
A16=-A15*FZ3(N)**2
A17=FZ3(N)/(DN(N-1)+DN(N))
A2=2.*A15*A17
B2=0.
C2=-A2
D2=-A12-Y3(N)*CLEHM
E2=A11*Z1+Y1(N)*CLEHP+Y3(N)*CLEHM
H2=A12-Y1(N)*CLEHP
G2=A11*(Z2*T2(N)-Z3*T1(N))+A16
IF (KODWAL.EQ.1) GO TO 7
IF (N.GT.2) GO TO 7
DID=(C2*D1-C1*D2)-((C2*H1-C1*H2)*(((1.+XK)**2)-1.))
XM1(1)=((C2*G1-C1*G2)+(C2*H1-C1*H2)*(XK*(1.+XK)*DN(1))*TZ3(1))/DID
XM2(1)=-(C2*B1-C1*B2)/DID
XM3(1)=-(C2*E1-C1*E2)+((C2*H1-C1*H2)*((1.+XK)**2)))/DID
7 CONTINUE
C      SET UP MATRIX ARRAYS
C
B1S=B1+A1*XK2(N-1)+D1*XM2(N-1)
B2S=B2+A2*XK2(N-1)+D2*XM2(N-1)
E1S=E1+A1*XK3(N-1)+D1*XM3(N-1)
E2S=E2+A2*XK3(N-1)+D2*XM3(N-1)
G1S=G1-A1*XK1(N-1)-D1*XM1(N-1)

```

```

G2S=G2-A2*XK1(N-1)-D2*XM1(N-1)
D=1./(B1S*E2S-E1S*B2S)
XK1(N)=D*(G1S*E2S-G2S*E1S)
XK2(N)=D*(E1S*C2-C1*E2S)
XK3(N)=D*(E1S*H2-H1*E2S)
XM1(N)=D*(B1S*G2S-B2S*G1S)
XM2(N)=D*(C1*B2S-B1S*C2)
XM3(N)=D*(H1*B2S-B1S*H2)
8 CONTINUE
KON=IM

C
C      CALCULATE THE SOLUTION VECTOR
C
DO 9 N=2,IM
F3(KON)=XK1(KON)+XK2(KON)*F3(KON+1)+XK3(KON)*T3(KON+1)
T3(KON)=XM1(KON)+XM2(KON)*F3(KON+1)+XM3(KON)*T3(KON+1)
KON=KON-1
9 CONTINUE
IF (KODWAL.EQ.1) GO TO 10
T3(1)=(XK*(1.+XK)*DN(1)*TZ3(1)-(1.+XK)**2*T3(2)+T3(3))/(1.-(1.+XK)
1**2)
TW=T3(1)*TE
10 CONTINUE

C
C      INTEGRATE CONTINUITY EQUATION
C
V3(1)=(RVWALD*FAA)/(R1*U1*EPS*XNUE)
BO=0.
A28=.5*X3/DX2*FT
DO 11 N=2,IE
B=A28*(Z1*F3(N)-Z2*F2(N)+Z3*F1(N))+F3(N)*.5
V3(N)=V3(N-1)-(B+BO)*DN(N-1)
BO=B
11 CONTINUE

C
C      COMPUTE NORMAL DERIVATIVES
C
DO 12 N=2,IM
RDN=1./(DN(N-1)+DN(N))
TZ3(N)=(T3(N+1)-T3(N-1))*RDN
FZ3(N)=(F3(N+1)-F3(N-1))*RDN
12 CONTINUE
FZ3(IE)=0.
TZ3(IE)=0.
IF (KODWAL.EQ.1) TZ3(1)=(-WW1*T3(1)+WW2*T3(2)-WW3*T3(3)+WW4*T3(4))
1/(WW5*DN(1))
FZ3(1)=(-WW1*F3(1)+WW2*F3(2)-WW3*F3(3)+WW4*F3(4))/(WW5*DN(1))

C
C      UPDATE VISCOSITY
C
KON=IE+2
DO 17 N=1,KON
IF (T3(N).LT.0.) GO TO 13
GO TO 14

```

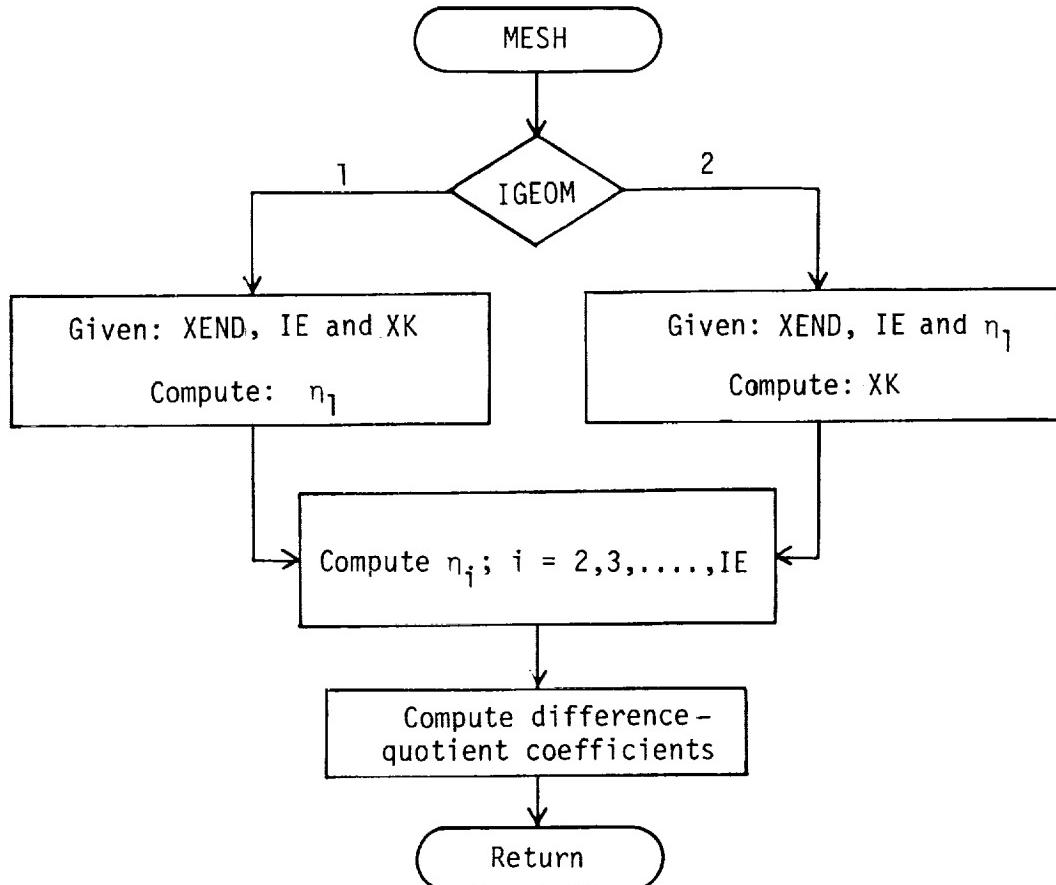
```

13 WRITE(6,19) T3(N),N,M
  STOP 500
14 CONTINUE
  IF (IGAS.EQ.2) GO TO 15
  XL3(N)=((1.+TR)*SQRT(T3(N))/(T3(N)+TR))
  XLP3(N)=XL3(N)*(TR-T3(N))/(2.*T3(N)*(T3(N)+TR))
  GO TO 16
15 CONTINUE
  XL3(N)=T3(N)**(VIS2C2-1.)
  XLP3(N)=(VIS2C2-1.)*(T3(N)**(VIS2C2-2.))
16 CONTINUE
  IF (IBODY.NE.1) GO TO 17
  IF (M.NE.2) GO TO 17
  T1(N)=T3(N)
  F1(N)=F3(N)
  RATO1(N)=RATO3(N)
  DRATO1(N)=DRATO3(N)
  XL1(N)=XL3(N)
  XLP1(N)=XLP3(N)
  V1(N)=V3(N)
17 CONTINUE
  RETURN
C
C
C
18 FORMAT (2X,12HNEGATIVE T3=,F15.7,2X,27H REPLACE WITH MEAN OF T1,T2
  1,2X,7HAT N = ,I5,2X,20H AND AT STATION M = ,I5)
19 FORMAT(//,2X,125HSOLUTION HAS RESULTED IN GENERATION OF NEGATIVE T
  1EMPERATURE WHICH CANNOT BE PHYSICALLY ACCEPTED. THIS GENERALLY OCC
  2URS IN THE,/2X,125HREGION OF ADVERSE PRESSURE GRADIENT AND/OR MAS
  3S INJECTION AT WALL BOUNDARY AND IS AN INDICATION OF BOUNDARY LAYE
  4R SEPARATION.,//,2X,118HIF DPEDS IS NEGATIVE AND THERE IS NO MASS
  5INJECTION AT THE WALL BOUNDARY, THE PROBLEM IS PROBABLY CAUSED BY
  6TOO COURSE,/2X,32HA STEP SIZE IN THE S-COORDINATE.,//,2X,6HT3(N)=
  7,F15.7,2HN=,I5,2X,2HM=,I5)
  END

```

## Subroutine MESH

Subroutine MESH generates the grid in the y-coordinate and obtains the difference quotient coefficients descriptive of the grid. The flow chart for subroutine MESH is as follows:



The program listing for subroutine MESH is as follows:

```

SUBROUTINE MESH (K,ETAMAX,IE,IGEOM,DETA1)
REAL K
COMMON /MESH1/ XN(JK),DN(JK),Y1(JK),Y2(JK),Y3(JK),Y4(JK),Y5(JK),Y6
1(JK)
XN(1)=0.
JKP1=JK
C
C IGEOM=1 SPECIFY ETAMAX,IE,K ,=2 SPECIFY ETAMAX,IE,DETA(1)
C
IF (K.EQ.1.) GO TO 5
IF (IGEOM.EQ.2) GO TO 1
GO TO 4
  
```

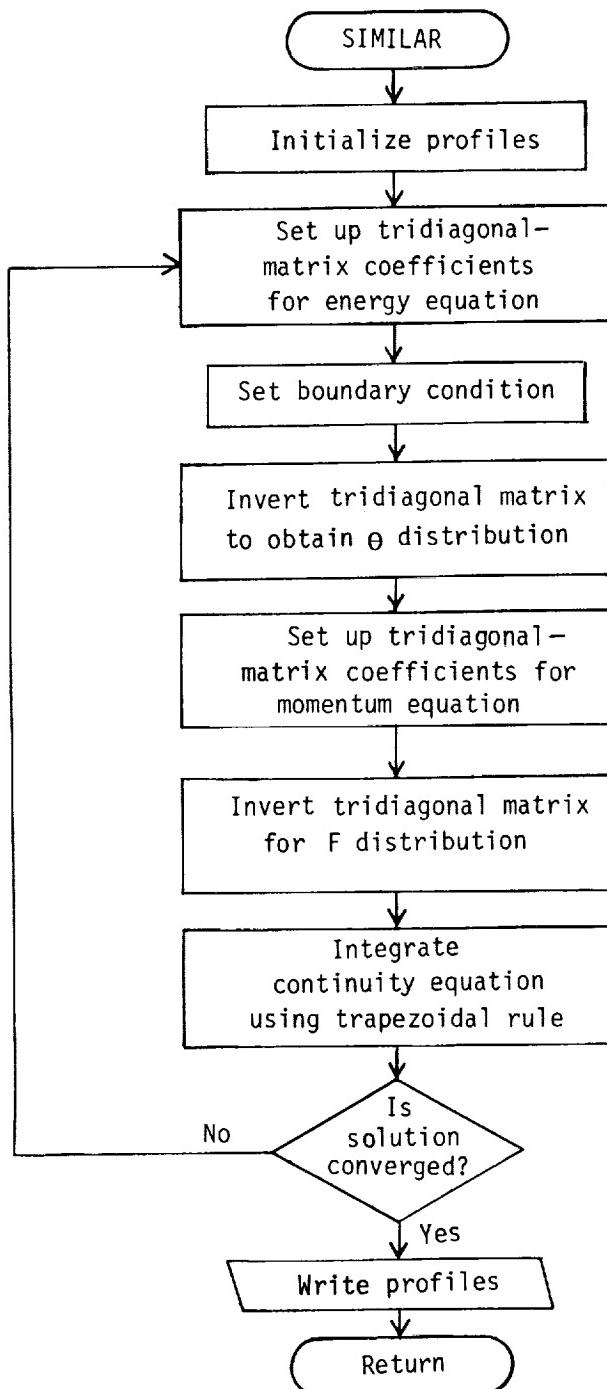
```

1 CONTINUE
XKO=1.0001
DIF=1.
RATIO=ETAMAX/DETA1
NIT=0
2 CONTINUE
A11=1.+(XKO-1.)*RATIO
A12=1./FLOAT(IE-1)
XKN=A11**A12
NIT=NIT+1
DIF=ABS(1.-XKN/XKO)
XKO=XKN
IF (NIT.GT.20) DIF=0.
IF (DIF.GT.0.0005) GO TO 2
NIT2=0
DIF2=1.0
3 CONTINUE
AN1=FLOAT(IE-1)
AN2=AN1-1.
FK=(XKO)**AN1-1.-(XKO-1.)*RATIO
DFK=AN1*XKO**AN2-RATIO
XKN=XKO-FK/DFK
NIT2=NIT2+1
DIF2=ABS(1.-XKN/XKO)
XKO=XKN
IF (NIT.GT.100) DIF2=0.
IF (DIF2.GT.0.00000001) GO TO 3
WRITE (6,9) NIT,NIT2,DIF,DIF2,XKN
K=XKN
4 CONTINUE
DN(1)=((1-K)/(1-K**(IE-1)))*ETAMAX
GO TO 6
5 DN(1)=ETAMAX/(IE-1)
6 XN(2)=DN(1)
DN(2)=K*DN(1)
DO 7 N=3,JKP1
DN(N)=(K**(N-1))*DN(1)
7 XN(N)=XN(N-1)+DN(N-1)
DO 8 N=2,JKP1
D1=DN(N-1)
D2=DN(N)
Y1(N)=2./(D2*(D1+D2))
Y2(N)=2./(D1*D2)
Y3(N)=2./(D1*(D1+D2))
Y4(N)=D1/(D2*(D1+D2))
Y5(N)=(D1-D2)/(D1*D2)
Y6(N)=D2/(D1*(D1+D2))
8 CONTINUE
RETURN
C
C
C
9 FORMAT (2X,2I5,3E16.8)
END

```

## Subroutine SIMILAR

Subroutine SIMILAR generates the similar solutions for the boundary-layer equations at the initial station ( $\xi = 0$ ). The flow chart for subroutine SIMILAR is as follows:



The program listing for subroutine SIMILAR is as follows:

```

SUBROUTINE SIMILAR (IE,IGAS,XAL,XBE,PR,KODWAL,TW,DTDZW,XK,TR,VIS2C
12,F3,F2,T3,T2,V3,V2,DFDZ,DTDZ,VIS,EP,ARGM,QW)
DIMENSION F3(JK), F2(JK), T3(JK), T2(JK), V3(JK), V2(JK), DFDZ(JK)
1, DTDZ(JK), VIS(JK), EP(JK), E(JK), F(JK)
COMMON /MESH1/ XN(JK),DN(JK),Y1(JK),Y2(JK),Y3(JK),Y4(JK),Y5(JK),Y6
1(JK)

C THIS SUBROUTINE GENERATES THE SELF-SIMILAR SOLUTIONS TO THE
C BOUNDARY-LAYER EQUATIONS
NITMAX=30
CONV=.0001
C INITIALIZE THE PROFILES
DO 1 N=1,JK
F3(N)=F2(N)=T3(N)=T2(N)=VIS(N)=EP(N)=1.0
DFDZ(N)=DTDZ(N)=0.0
V3(N)=V2(N)=-XN(N)
1 CONTINUE
DFDZW=1.
NIT=1
2 CONTINUE
IF (KODWAL.NE.1) DTDZW=QW*ARGM/VIS(1)

C SET UP FOR ENERGY EQUATION
C
E(IE)=0.
F(IE)=1.0
IM=IE-1
N=IM
DO 3 I=2,IM
RDN=1./(DN(N-1)+DN(N))
VISM1=.5*VIS(N-1)+.5*VIS(N)
VISP1=.5*VIS(N+1)+.5*VIS(N)
A=-V3(N)*RDN-VISM1/PR*Y3(N)
B=VISP1/PR*Y1(N)+VISM1/PR*Y3(N)
C=V3(N)*RDN-VISP1/PR*Y1(N)
D=XAL*VIS(N)*DFDZ(N)**2
E(N)=-A/(B+C*E(N+1))
F(N)=(D-C*F(N+1))/(B+C*E(N+1))
N=N-1
3 CONTINUE
T3(1)=TW
IF (KODWAL.EQ.1) GO TO 4

C HEAT TRANSFER BOUNDARY CONDITION
C
ANMR=XK*(1.+XK)*DN(1)*DTDZW-(1.+XK)*(1.+XK)*F(2)+E(3)*F(2)+F(3)
DNMR=1.-(1.+XK)*(1.+XK)+E(2)*(1.+XK)*(1.+XK)-E(3)*E(2)
T3(1)=ANMR/DNMR
4 CONTINUE
DO 5 N=2,IE
T2(N)=T3(N)
T3(N)=E(N)*T3(N-1)+F(N)

```

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```

5 CONTINUE
  DO 7 N=1, IE
    IF (T3(N).LT.0.) T3(N)=1.
    IF (IGAS.EQ.2) GO TO 6
    VIS(N)=((1.+TR)*SQR(T3(N))/(T3(N)+TR))
    GO TO 7
6 CONTINUE
  VIS(N)=T3(N)**(VIS2C2-1.)
7 CONTINUE

C
C      SET UP FOR SOLVING MOMENTUM EQUATION
C
E(IE)=0.
F(IE)=1.
IM=IE-1
N=IM
DO 8 I=2, IM
  RDN=1./(DN(N-1)+DN(N))
  VISM1=.5*VIS(N-1)+.5*VIS(N)
  VISP1=.5*VIS(N+1)+.5*VIS(N)
  A=-V3(N)*RDN-VISM1*Y3(N)
  B=VISP1*Y1(N)+VISM1*Y3(N)+2.*XBE*F3(N)
  C=V3(N)*RDN-VISP1*Y1(N)
  D=XBE*(F3(N)**2+T3(N))
  E(N)=-A/(B+C*E(N+1))
  F(N)=(D-C*F(N+1))/(B+C*E(N+1))
  N=N-1
8 CONTINUE
F3(1)=0.
DO 9 N=2, IE
  F2(N)=F3(N)
  F3(N)=E(N)*F3(N-1)+F(N)
9 CONTINUE
IF (NIT.LT.5) GO TO 11
DO 10 N=2, IE
  F3(N)=.5*(F3(N)+F2(N))
  T3(N)=.5*(T3(N)+T2(N))
10 CONTINUE
11 CONTINUE
DO 12 N=2, IM
  RDN=1./(DN(N-1)+DN(N))
  DTDZ(N)=(T3(N+1)-T3(N-1))*RDN
  DFDZ(N)=(F3(N+1)-F3(N-1))*RDN
12 CONTINUE
XK1=XK+1.
XK2=XK1**2
DTDZ(1)=DTDZ
IF (KODWAL.EQ.1) DTDZ(1)=((1.-XK2)*T3(1)+XK2*T3(2)-T3(3))/(XK*XK1*
1DN(1))
DFDZ(1)=((1.-XK2)*F3(1)+XK2*F3(2)-F3(3))/(XK*XK1*DN(1))
DTDZ(IE)=0.
DFDZ(IE)=0.

```

```

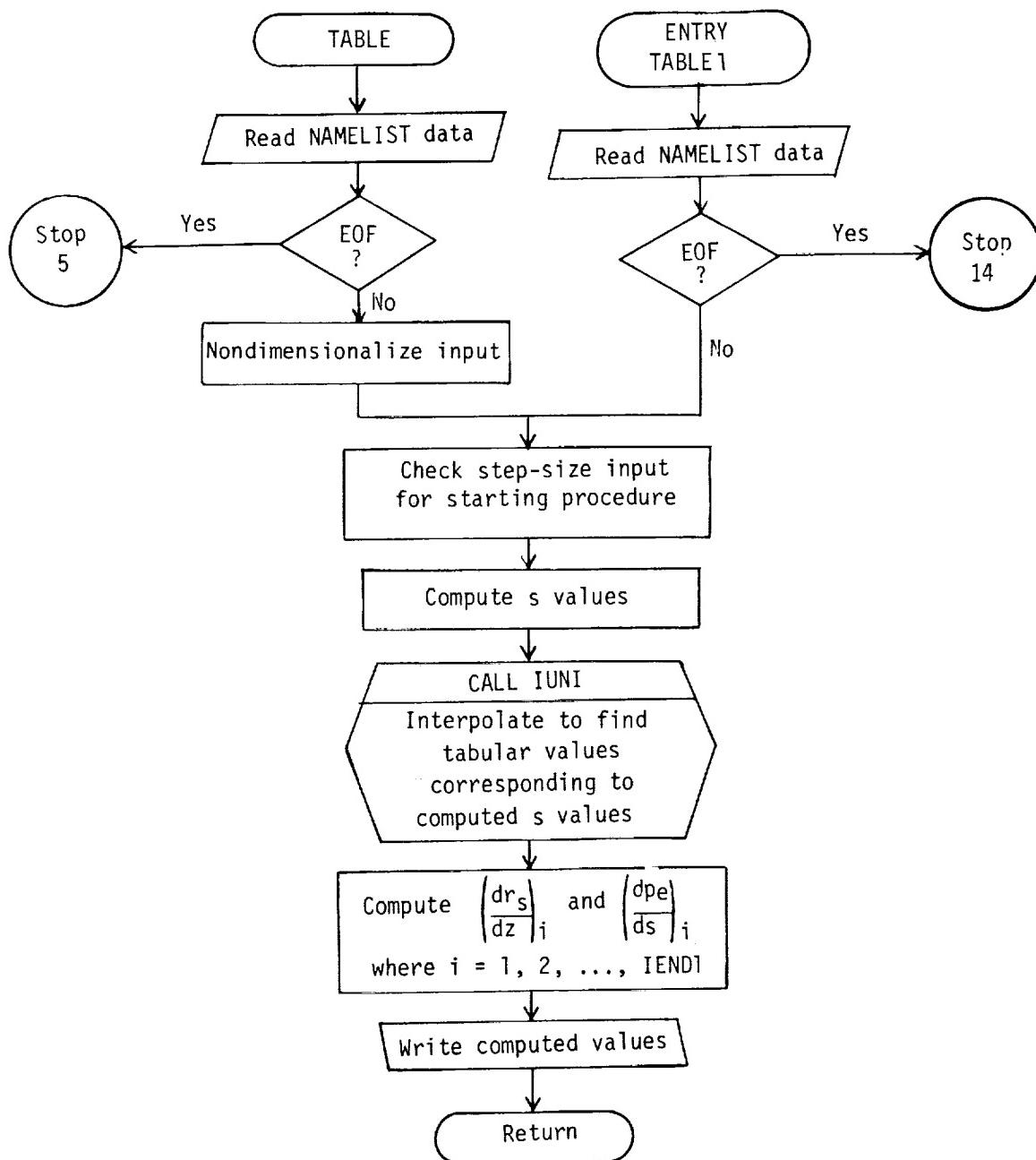
C
C      SOLVE THE CONTINUITY EQUATION
C

V3(1)=0.
DO 13 N=2,IE
V3(N)=V3(N-1)-DN(N-1)*.5*(F3(N)+F3(N-1))
13 CONTINUE
DIF=ABS(1.-DFDZW/DFDZ(1))
DFDZW=DFDZ(1)
NIT=NIT+1
IF (NIT.GT.NITMAX) WRITE (6,15) DIF,NIT
IF (NIT.GT.NITMAX) DIF=0.
IF (DIF.GT.CONV) GO TO 2
C      ASSIGN PROFILES AT THE PREVIOUS STATION
C      AND PRINT THE SIMILAR SOLUTION
WRITE (6,18)
WRITE (6,19)
DO 14 N=1,IE
WRITE (6,20) XN(N),F3(N),T3(N),V3(N),DFDZ(N),DTDZ(N),VIS(N)
F2(N)=F3(N)
T2(N)=T3(N)
V2(N)=V3(N)
14 CONTINUE
WRITE (6,17) NIT
WRITE (6,16)
RETURN
C
C
C
15 FORMAT (2X,27HTHE ERROR IN WALL SHEAR IS=,E15.7,5HAFTER,I5,12HITER
IATIONS= /)
16 FORMAT (1H0,20X,26HINITIAL STATION PARAMETERS,/)
17 FORMAT (9X,40HCONVERGED SELF-SIMILAR SOLUTION REQUIRED,I5,11HITERA
ITIONS.,/)
18 FORMAT (1H1,20X,46HSIMILAR SOLUTION REQUIRED TO INITIATE MARCHING,
110H PROCEDURE,///,20X,14HPROFILE VALUES,/)
19 FORMAT (15X,3HETA,11X,4HU/UE,10X,4HT/TE,10X,1HV,13X,2HFZ,12X,2HTZ,
112X,2HXL,///)
20 FORMAT (10X,7E14.6)
END

```

## Subroutine TABLE

Subroutine TABLE reads tabular input data for body geometry, pressure distribution, and wall-boundary conditions. These inputs are nondimensionalized and distributed to the solution stations designated in the SS array. The flow diagram for subroutine TABLE is as follows:



The program listing for subroutine TABLE is as follows:

```

SUBROUTINE TABLE (IEND1,SD,R1,U1,A,TREF,KODWAL,VISREF,KODUNIT,AWT)
DIMENSION PE(JJ), Z(JJ), RMI(JJ), TW(JJ), S(JJ), RVWALD(JJ), QW(JJ)
1, PD(JH), ZED(JH), RMIDD(JH), SS(JH)
DIMENSION DVT1(JJ,3), ANS1(3)
EQUIVALENCE (Z,DVT1(1,1)), (RMI,DVT1(1,2)), (PE,DVT1(1,3))
NAMELIST /NAM2/ NUMBER,L,PE,Z,RMI,TW,RVWALD,QW,S,SS
DATA C1/.0208854346/,C2/1.8/,C5/3.280839895/,C15/.0063658804/,C16/
1.0000881/,SS(2)/0./,L/1/
DO 1 I=1,JJ
QW(I)=RVWALD(I)=0.0
RMI(I)=1.
TW(I)=AWT
1 CONTINUE
READ (5,NAM2)
IF (EOF(5)) 2,3
2 STOP 5
3 CONTINUE
WRITE(6,23) NUMBER,L,S
WRITE(6,24) Z
WRITE(6,25) RMI
IF(KODWAL.EQ.1) WRITE(6,26) TW
WRITE(6,27) QW
WRITE(6,28) RVWALD
WRITE(6,29) PE
WRITE(6,30) SS
C
C
IF (KODUNIT.NE.1) GO TO 7
C
C      CONVERT $NAM2   INPUT DATA TO U.S.STANDARD UNITS
C
DO 4 I=1,IEND1
4 SS(I)=SS(I)*C5
DO 6 I=1,NUMBER
S(I)=S(I)*C5
Z(I)=Z(I)*C5
RMI(I)=RMI(I)*C5
PE(I)=PE(I)*C1
RVWALD(I)=RVWALD(I)*C15
IF (KODWAL.NE.1) GO TO 5
TW(I)=TW(I)*C2
GO TO 6
5 QW(I)=QW(I)*C16
6 CONTINUE
7 DO 9 I=1,NUMBER
PE(I)=PE(I)/(R1*U1*U1)
S(I)=S(I)/A
RMI(I)=RMI(I)/A
IF (KODWAL.NE.1) GO TO 8
TW(I)=TW(I)/TREF
GO TO 9

```

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```

8 CONTINUE
9 Z(I)=Z(I)/A
DO 10 I=1,IEND1
10 SS(I)=SS(I)/A
GO TO 12
ENTRY TABLE1
READ (5,NAM2)
IF (EOF(5)) 11,12
11 STOP 14
12 CONTINUE
DS=SS(1)
IF (SS(1).GT.DS+.000001.OR.SS(1).LT.DS-.000001) GO TO 13
IF (SS(2).GT.DS+.000001.OR.SS(2).LT.DS-.000001) GO TO 13
IF (SS(3).GT.DS+.000001.OR.SS(3).LT.DS-.000001) GO TO 13
GO TO 14
13 WRITE (6,22) SS(1),SS(2),SS(3),DS
STOP 77
14 CONTINUE
TEMP=0.
DO 15 I=1,IEND1
SS(I)=TEMP+SS(I)
15 TEMP=SS(I)
WRITE(6,31) SS
TEMP1=0.
TEMP2=SS(1)
DO 16 I=1,IEND1
SS(I)=TEMP1
TEMP1=TEMP2
IF (I.LT.IEND1) TEMP2=SS(I+1)
IPT=-1
SD=DS*(I-1)
IF (SS(2).NE.0.) SD=SS(I)
CALL IUNI (JJ,NUMBER,S,3,DVT1,L,SD,ANS1,IPT,IERR)
ZED(I)=ANS1(1)
RMIDDD(I)=ANS1(2)
PD(I)=ANS1(3)
16 CONTINUE
SD=TEMP1
IENDP1=IEND1+1
IPT=-1
CALL IUNI (JJ,NUMBER,S,3,DVT1,L,SD,ANS1,IPT,IERR)
ZED(IENDP1)=ANS1(1)
RMIDDD(IENDP1)=ANS1(2)
PD(IENDP1)=ANS1(3)
SS(IENDP1)=TEMP1
WRITE (4) TW(1),RVWALD(1),QW(1),PE(1),DS
TWODS=2.*DS
DO 21 I=2,IENDP1
IPT=-1
SD=DS*(I-1)
IF (SS(2).NE.0.) SD=SS(I)
IF (KODWAL.EQ.1) GO TO 17
CALL IUNI (JJ,NUMBER,S,1,QW,L,SD,QWD,IPT,IERR)
GO TO 18

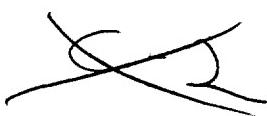
```



```
17 CONTINUE
    CALL IUNI (JJ,NUMBER,S,1,TW,L,SD,TWD,IPT,IERR)
18 CONTINUE
    CALL IUNI (JJ,NUMBER,S,1,RVWALD,L,SD,RVWALDD,IPT,IERR)
    IF (I.EQ.IENDP1) GO TO 19
    DRDZ=(RMIDD(I+1)-RMIDD(I-1))/(ZED(I+1)-ZED(I-1))
    IF (SS(2).NE.0.) TWODS=SS(I+1)-SS(I-1)
    DPEDSD=(PD(I+1)-PD(I-1))/TWODS
    GO TO 20
19 IF (SS(2).NE.0.) DDS=SS(I)-SS(I-1)
    DPEDSD=(PD(I)-PD(I-1))/DDS
    DRDZ=(RMIDD(I)-RMIDD(I-1))/(ZED(I)-ZED(I-1))
20 WRITE (4) SD,PD(I),RMIDD(I),TWD,ZED(I),DPEDSD,RVWALDD,DRDZ,QWD
21 CONTINUE
    REWIND 4
    RETURN
```

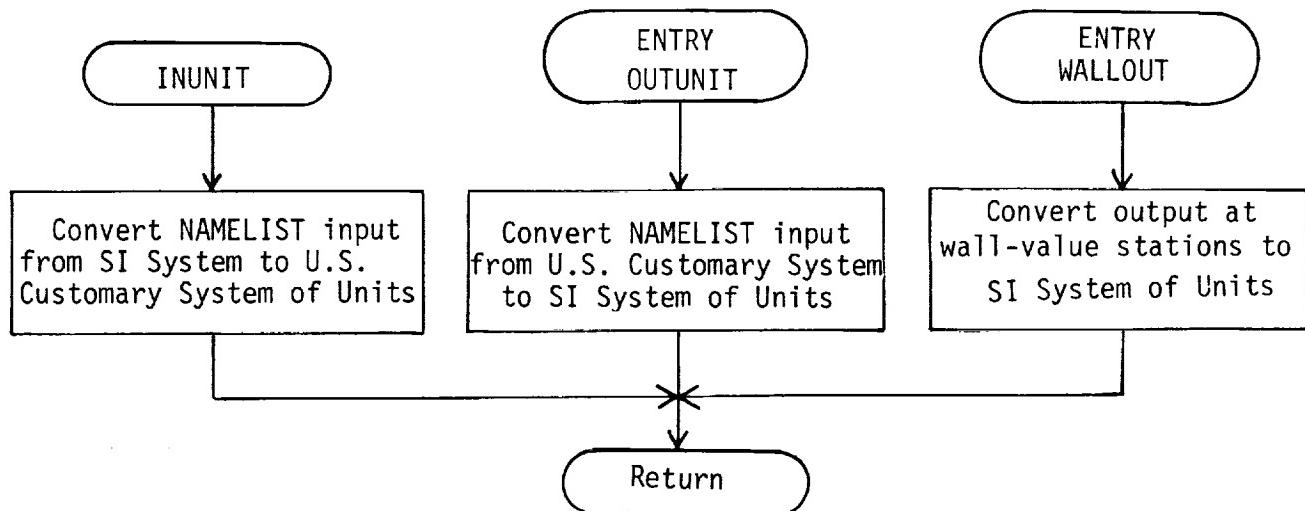
C
C
C

```
22 FORMAT (1X,7HSS(1) =,F9.4,/1X,7HSS(2) =,F9.4,/1X,7HSS(3) =,F9.4,/1
1X,7HDS      =,F9.4,/1X,53HTHESE VALUES MUST BE EQUAL FOR THE STARTIN
2G PROCEDURE)
23 FORMAT(1,2X,5H$NAM2,/,2X,8HNUMBER =,I12,1,2X,8HL      =,I12,1,2X,
11HS,/,10E12.5)
24 FORMAT(2X,1HZ,/,10E12.5)
25 FORMAT(2X,3HRMI,/,10E12.5)
26 FORMAT(2X,2HTW,/,10E12.5)
27 FORMAT(2X,2HQW,/,10E12.5)
28 FORMAT(2X,6HRVWALD,/,10E12.5)
29 FORMAT(2X,2HPE,/,10F12.5)
30 FORMAT(2X,2HSS,/,10E12.5)
31 FORMAT(117HTHE FOLLOWING SPOINT VALUES DESIGNATE THE S-COORD
1INATE LOCATIONS WHERE THE SOLUTIONS ARE OBTAINED DURING THE S-MARC
2H.,/,2X,116HYOUR PRINT STATION MUST AGREE WITH ONE OR MORE OF THE
3SPOINT LOCATIONS; IE, YOU CAN PRINT ONLY AT SOLUTION STATIONS.,/,2
4X,113HIF THE CASE COMPLETES WITH A NORMAL STOP AND NO OUTPUT IS PR
5INTED, YOUR PRINT INPUT IS IN ERROR. THE ERROR CAN BE,/,2X,50HNOTE
6D BY COMPARING PROVAL AND PRNTVAL WITH SPOINT.,/,2X,6HSPOINT,/,1
710E12.5)
    END
```



## Subroutine INUNIT

Subroutine INUNIT converts the International System (SI) of dimensional input data to the U.S. Customary System of Units for calculations in the program. The subroutine then converts the output data back to the SI System of Units before output. The flow diagram for subroutine INUNIT is as follows:



The program listing for subroutine INUNIT is as follows:

```

SUBROUTINE INUNIT (PROVAL, PRNTVAL, JM, JN)
COMMON /TRBULNT/ S,KSTR,TLNGTH,TRFACT,DISINC,XT1,XT2,XT6,XT3,XT4,X
1T5,PRTW,RE,UE,XNUE,J,RMI,EPS,JPOINT,IE,WW1,WW2,WW3,WW4,WW5, NEDGE
2,KODVIS,A,XBE,X,PR,KODPRT,PRT,PRTAR,GLAR,NUMB1,XK
COMMON /UNIT/ VIS1C1,VIS1C2,VIS2C1,VIS2C2,PT1,TT1,WAVE,R,PHIO,DS,S
1ST,RT1,P1,T1,R1,U1,AA1,TREF,VISREF,PESTAR,TESTAR,RESTAR,UESTAR,MUE
2STAR,YESTAR,THETA,TAUD,QSD,HD,UPLUS,DISP,PE,Z,TW,QW,RVWALD,PROINC,
3PRNTINC,ZS,RS
DIMENSION PROVAL(JN), PRNTVAL(JM)
REAL MUESTAR
DATA RT1,P1,T1,R1,U1,AA1,TREF,VISREF/8*1.0/,UPLUS/0.0/
DATA TAUD,S,RMI,Z,ZS,RS,YESTAR,DISP,THETA,QSD,HD/11*0./
DATA CC1/.0208854346/,CC2/1.8/,CC4/5.97995/,CC5/3.280839895/,CC6/.
10019403196/,CC7/47.880258/,CC8/.55555555/,CC10/.167225478/,CC11/.3
2048/,CC12/515.379/,CC13/11348.93/,CC14/20428.0758/

```

C  
C  
C

CONVERT \$NAM1 VALUES TO U.S. STANDARD UNITS

```

PROINC=PROINC*CC5
PRNTINC=PRNTINC*CC5
DO 1 I=1,JN
1 PROVAL(I)=PROVAL(I)*CC5
DO 2 I=1,JM

```

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```

2 PRNTVAL(I)=PRNTVAL(I)*CC5
A=A*CC5
U1=U1*CC5
AA1=AA1*CC5
SST=SST*CC5
PT1=PT1*CC1
P1=P1*CC1
VISREF=VISREF*CC1
TREF=TREF*CC2
T1=T1*CC2
TT1=TT1*CC2
R=R*CC4
RT1=RT1*CC6
R1=R1*CC6
GO TO 5

```

C            CONVERT \$NAM1 VALUES TO INTERNATIONAL STANDARD UNITS

```

C
C ENTRY OUTUNIT
PROINC=PROINC*CC11
PRNTINC=PRNTINC*CC11
DO 3 I=1,JN
3 PROVAL(I)=PROVAL(I)*CC11
DO 4 I=1,JM
4 PRNTVAL(I)=PRNTVAL(I)*CC11
A=A*CC11
SST=SST*CC11
U1=U1*CC11
AA1=AA1*CC11
PT1=PT1*CC7
P1=P1*CC7
VISREF=VISREF*CC7
TREF=TREF*CC8
T1=T1*CC8
TT1=TT1*CC8
R=R*CC10
RT1=RT1*CC12
R1=R1*CC12
GO TO 5

```

C            CONVERT WALL VALUES TO INTERNATIONAL STANDARD UNITS

```

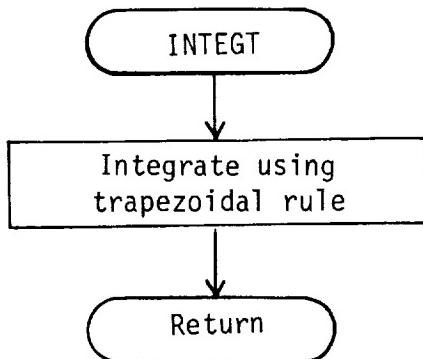
C
C ENTRY WALLOUT
PESTAR=PESTAR*CC7
MUESTAR=MUESTAR*CC7
TAUD=TAUD*CC7
TESTAR=TESTAR*CC8
S=S*CC11
RMI=RMI*CC11
Z=Z*CC11
ZS=ZS*CC11
RS=RS*CC11

```

```
UPLUS=UPLUS*CC11
DISP=DISP*CC11
UESTAR=UESTAR*CC11
YESTAR=YESTAR*CC11
THETA=THETA*CC11
RESTAR=RESTAR*CC12
QSD=QSD*CC13
HD=HD*CC14
5 RETURN
END
```

## Function INTEGR

Function subroutine INTEGR integrates the continuity equation by the trapezoidal rule. The flow diagram for function INTEGR is as follows:

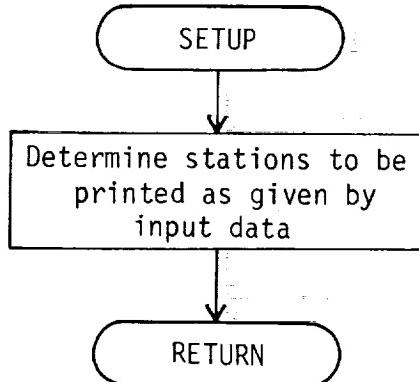


The program listing for function subroutine INTEGR is as follows:

```
REAL FUNCTION INTEGR(YY,NOPTS,DX)
DIMENSION YY(NOPTS), DX(NOPTS)
INTEGR=0.
IF (NOPTS.LT.2) GO TO 2
DO 1 N=2,NOPTS
1 INTEGR=INTEGR+(DX(N-1)/2.)*(YY(N-1)+YY(N))
2 RETURN
END
```

## Subroutine SETUP

Subroutine SETUP determines from input where profiles and wall values are to be printed. The flow diagram for subroutine SETUP is as follows:



The program listing for subroutine SETUP is as follows:

```
SUBROUTINE SETUP (A,B,C,J,K)
DIMENSION B(J)
IF (A.EQ.0) RETURN
KPLUS2=K+2
B(K+1)=A
IF(KPLUS2.GT.J) RETURN
DO 1 I=KPLUS2,J
B(I)=B(I-1)+A
IF (B(I).GE.C) RETURN
1 CONTINUE
RETURN
END
```

APPENDIX D

RESULTS FROM TEST CASES - INPUT/OUTPUT

The input and selected output from each of the test cases is presented in the following order: (1) VARDIM data; (2) input data for \$NAM1, \$NAM2, and \$NAM3 (note that \$NAM3 data are required only for test case number 4); (3) initial profile ( $\xi = 0$ ); (4) free-stream and reference values; (5) selected wall-print locations; (6) selected profile-print locations. It should be noted that (5) and (6) are selected locations and not all the print locations obtained for the input data. The selected print values allow users to verify that the software has been correctly implemented on their computer system.

## TEST CASE NO. 1

THE LISTING FOR TEST CASE NO. 1 INCLUDES THE FOLLOWING: (1) VARDIM DATA; (2) \$NAM1 AND \$NAM2 INPUT;  
 (3) INITIAL STATION SOLUTION; (4) REFERENCE VALUES; (5) PROFILE AND WALL PRINTS AT S=1.0 M.

```
*VARDIM/VGBLP(JK=103,JL=1,JM= 11,JN= 2,JI=1,JH=217)
*VARDIM/TABLE(JJ=2,JH=217)
*VARDIM/VARENT(JL=1)
*VARDIM/TURBLNT(JI=1,JK=103)
*VARDIM/MESH(JK=103)
*VARDIM/SIMILAR(JK=103)
*VARDIM/SOLVE(JK=103)
```

## \$NAM1

```
IGEOM = .41400E+07 1 XEND = .12000E+03 IE = .12754E+01 XK = .12754E+01
PT1 = .14000E+01 1 TT1 = .31000E+03 IGAS = .14582E-05 XIC1 = .11033E+03 XMA = .28000E+01
VIS2C2 = .14000E+00 1 G = .14000E+01 R = .28696E+03 VIS1C2 = .72000E+00 VIS2C1 = .1
IBODY = 2 WAVE = 0. PHII = 0. J = - 0 W = - 0 IENTRO = 1
SST = .10000E+09 SMXTR = .24000E+04 KODVIS = .16800E-01 XT3 = .50000E+01 XT4 = .20000E+01 IYINT = .10800E+00
KODAMP = .40000E+00 2 XT1 = .40000E+00 XT2 = .16800E-01 XT5 = .78000E+00
XT6 = .95000E+00 PRT = .95000E+00 KODPRT = .1 NUMB1 = 0 GLAR = .1
PRTAR = .26000E+02
IEND1 = 216 PROINC = .10000E+01 PRNTINC = .10000E+00 IPRO = 1 IPRNT = 1 NAUXPRO = 0
FT = .10000E+01 KODE = 0 VELEDG = .99500E+00 CONV = .10000E-03 NITMAX = 5
KODUNIT = 1 ITMAX = 3 CONVE = .10000E-01
```

THIS COMPLETES THE OUTPUT OF \$NAM1 WITH THE EXCEPTION OF PROVAL AND PRNTVAL. THESE VALUES ARE PRINTED JUST PRIOR TO THE INITIAL STATION PRINT.

## \$NAM2

NUMBER =	2
L =	1



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THE FOLLOWING SPPOINT VALUES DESIGNATE THE S-COORDINATE LOCATIONS WHERE THE SOLUTIONS ARE OBTAINED DURING THE S-MARCH. YOUR PRINT STATION MUST AGREE WITH ONE OR MORE OF THE SPPOINT LOCATIONS; IE, YOU CAN PRINT ONLY AT SOLUTION STATIONS. IF THE CASE COMPLETES WITH A NORMAL STOP AND NO OUTPUT IS PRINTED, YOUR PRINT INPUT IS IN ERROR. THE ERROR CAN BE NOTED BY COMPARING PROVAL AND PRNTVAL WITH SPPOINT.

PRINT STATIONS DESIGNATED IN SNAME1 INPUT AND GENERATED IN SETUP

PROVAL .70000E-02 • 10000E+01  
PPNTVAL .70000E-02 • 10000E+00 • 20000E+00 • 30000F+00 • 40000E+00 • 50000E+00 • 60000E+00 • 70000E+00 • 80000E+00 • 90000E+00

## SIMILAR SOLUTION REQUIRED TO INITIATE MARCHING PROCEDURE

## PROFILE VALUES

ETA	U/UE	T/TE	V	FZ	TZ	XL
0.	0.	232179E+01	0.	502786E+00	0.	900739E+00
*.900542E-09	*.452780E-09	.232203E+01	-.203874E-18	*.502786E+00	*.115652E+06	*.900739E+00
*.204909E-08	*.103026E-08	.232203E+01	-.105554E-17	*.502786E+00	-.163130E-04	*.900739E+00
*.351396E-08	*.176677E-08	.232203E+01	-.310417E-17	*.502786E+00	-.426349E-05	*.900739E+00
*.538224E-08	*.270612E-08	.232203E+01	-.728248E-17	*.502786E+00	*.668574E-05	*.900739E+00
*.776505E-08	*.390416E-08	.232203E+01	-.151580E-16	*.502786E+00	*.131052E-04	*.900739E+00
*.108041E-07	*.543214E-08	.232203E+01	-.293447E-16	*.502786E+00	*.143855E-04	*.900739E+00
*.146801E-07	*.738094E-08	.232203E+01	-.541764E-16	*.502786E+00	*.193358E-04	*.900739E+00
*.196235E-07	*.986643E-08	.232203E+01	-.968070E-16	*.502786E+00	*.240042E-04	*.900739E+00
*.259228E-07	*.130364E-07	.232203E+01	-.169007E-15	*.502786E+00	*.237738E-04	*.900739E+00
*.339696E-07	*.170794E-07	.232203E+01	-.290091E-15	*.502786E+00	*.256304E-04	*.900739E+00
.	.	.	.	.	.	.
.	.	.	.	.	.	.
*	*	*	*	*	*	*
*.134489E+02	*.999814E+00	*.999709E+00	-.122815E+02	-.315453E-05	-.713927E-05	*.100001E+01
*.171400E+02	*.100001E+01	*.100002E+01	-.159823E+02	*.137030E-05	*.299940E-05	*.999999E+00
*.218603E+02	*.999825E+00	*.999734E+00	-.207022E+02	-.618434E-06	-.132710E-05	*.100001E+01
*.278896E+02	*.100000E+01	*.100001E+01	-.267220E+02	-.285730E-06	-.605893E-06	*.100000E+01
*.355529E+02	*.999829E+00	*.999743E+00	-.343997E+02	-.133390E-06	-.282025E-06	*.100001E+01
*.453519E+02	*.100000E+01	*.100000E+01	-.441918E+02	-.633907E-07	-.132873E-06	*.100000E+01
*.578418E+02	*.999831E+00	*.999746E+00	-.566807E+02	-.301764E-07	-.630844E-07	*.100001E+01
*.737715E+02	*.1C0000E+01	*.100000E+01	-.726609E+02	-.144213E-07	-.300990E-07	*.100000E+01
*.90881E+02	*.999831E+00	*.999747E+00	-.929239E+02	-.690972E-08	-.144071E-07	*.100001E+01
*.120000E+03	*.100000E+01	*.100000E+01	-.118834E+03	0.	0.	*.100000E+01

CONVERGED SELF-SIMILAR SOLUTION REQUIRED 16 ITERATIONS.

## INITIAL STATION PARAMETERS

MUE = .839745E-05    UE = \*617610E+03    TE = \*1211C6E+03    PF = .152552E+06    OSD = 0.  
 XAL = .313600E+01    XBF = 0.    RF = .4388968E+01

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\*\*\*\*\*DIMENSIONAL OUTPUT QUANTITIES ARE IN S.I. UNITS\*\*\*\*\*

FREE STREAM VALUES-DIMENSIONAL

REFERENCE VALUES-DIMENSIONAL  
PREF# .167441E+07 TREF=

## 1.00000 PROFILE

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APPENDIX D

S	=	.10000E+01	RETHETI=	.17548E+06	DPEDS =	0.	CFW =	.23161E-02	ZSHK =	0.	YE =	.75919E-02
XI	=	.38133E+00	RFS	.32285E+09	DTEDS =	0.	OSD =	0.	RSHK =	0.	UTAU =	.10372E-01
RMI	=	.10000E+01	PE	.15255E+06	DUEDS =	0.	HD =	0.	ITRC =	0.	TRFCF =	.10000E+01
Z	=	.10000E+01	TE	.12111E+03	DLTAST=	0.	.25105E-02	NSTE =	TW/TT1 =	.95169E+00	YMP =	.92
BETA	=	0.	RE	.43897E+01	THETA =	*54.354E-03	NSTW =	0.	RFTURE=	.92088E+00	P20 =	.24725E+01
XAL	=	.31360E+01	UE	.61761E+03	FORM =	.46189E+01	NUE =	0.	ROUSE =	.28124E+06	OMEGA =	.90126E-04
RWALD=	0.	.ME	.28000E+01	TAUD =	.79342E+03	NUW =	0.	DSMX0 =	-.11551E+03			
REDELT=	.81052E+06	MUF	.83975E-05	CFF =	.94770E-03	SWANG =	I	VW =	0.	RVWAL =	0.	
NOITER=	4	ERROP =	.47339E-04									

TEST CASE NO. 2

THE LISTING FOR TEST CASE NO. 2 INCLUDES THE FOLLOWING: (1) VAPDIM DATA; (2) \*NAMI AND \$NAM2 INPUT;  
 (3) INITIAL STATION SOLUTION; (4) REFERENCE VALUES; (5) PROFILE AND WALL PRINTS AT S=1.07 M.  
 NOTE: TWO RUNS ARE INCLUDED IN THIS TEST CASE: W=1; W=0.

TEST CASE NO. 2; W = 1.

```
*VARDIM/VGRLP(JK= 63,JL=1,JM= 17,JN=2,JI=1,JH=165)
*VARDIM/TABLE(JJ=41,JH=165)
*VARDIM/VARENT(JL=1)
*VARDIM/TURBLNT(JI=1,JK= 63)
*VARDIM/MESH(JK= 63)
*VARDIM/SIMILAR(JK= 63)
*VARDIM/SOLVE(JK= 63)
```

\$NAMI	I	XFND	IE	VIS1C1	DETAL	XMA	.17000E+01							
IGEDM		1		1										
PT1		47511E+05	TT1	29780E+03	12754E+01									
VIS2C2		1	G	14000E+01	14582E-05	VIS2C1								
				R	28696E+03									
					PP									
					.72000E+00									
IRNDY		2	WAVE	43523E+02	PHII	.20000E+02	J		1	W		1	IENTRO	
SST		90000E-01	SMXTR	10000E+09	KODVIS	2	KTCOD		TLNGTH		2	YINT		
KODAMP		2	XT1	40000E+00	XT2	16800E-01	XT3		20000E+01		XT5			
XT6		.26000E+02	PPT	.95000E+00	KODPRT	1	NUM81	0	GLAR		1			
PRTAP														
I														
TEND1		164	PPOINC	0.	PRNTINC	.10000E+00	IPPO		IPRNT		2	NAUXPRO		0
FT		.10000E+01	KODE		0	KODWAL	2	VELEDG		CONV		NITMAX		5
KODUNIT		1	ITMAX		3	CONVE								

THIS COMPLETES THE OUTPUT OF \$NAMI WITH THE EXCEPTION OF PROVAL AND PRNTVAL. THESE VALUES ARE PRINTED JUST PRIOR TO THE INITIAL STATION PRINT.

**ORIGINAL PAGE IS  
OF POOR QUALITY**

## APPENDIX D

SNAME2									
NUMBER	=	41	L	=	1	S	=	L	=
0.	40049E+00	• 40545E-01	• 81090E-01	• 12164E+00	• 16218E+00	• 20273E+00	• 24324E+00	• 28334E+00	• 32288E+00
• 43877E+00	• 43877E+00	• 47690E+00	• 51501E+00	• 55242E+00	• 59164E+00	• 63023E+00	• 66689E+00	• 70777E+00	• 74652F+00
• 78518E+00	• 82316E+00	• 86227E+00	• 90072E+00	• 93913E+00	• 97749E+00	• 10158E+01	• 10541E+01	• 10922E+01	• 11303E+01
• 11685E+01	• 12066E+01	• 12452E+01	• 12836E+01	• 13220E+01	• 13605E+01	• 13991E+01	• 14377E+01	• 14764E+01	• 15152E+01
Z									
0.	38100E+00	• 38100E-01	• 76200E-01	• 11430E+00	• 15240E+00	• 19050E+00	• 22860E+00	• 26670E+00	• 30480E+00
• 41910E+00	• 45720E+00	• 49530E+00	• 53340E+00	• 57150E+00	• 60960E+00	• 64770E+00	• 68580E+00	• 72390E+00	• 76580E+00
• 76200E+00	• 80010E+00	• 83820E+00	• 87630F+00	• 91440E+00	• 95250E+00	• 99060E+00	• 10287E+01	• 10668E+01	• 11049F+01
• 11430E+01	• 11811E+01	• 12192E+01	• 12573E+01	• 12954E+01	• 13335E+01	• 13716E+01	• 14097E+01	• 14478E+01	• 14859F+01
• 15240E+01									
RMI									
0.	13867E-01	• 27735E-01	• 41602E-01	• 55469F-01	• 69336E-01	• 83118E-01	• 95612E-01	• 10618E+00	• 11457E+00
• 12063E+00	• 12430E+00	• 12559E+00	• 12463E+00	• 12161E+00	• 11684E+00	• 11070E+00	• 10368E+00	• 96332E-01	• 89279F-01
• 82739E-01	• 76661E-01	• 71071E-01	• 65875E-01	• 61061E-01	• 56593E-01	• 52443E-01	• 49042E-01	• 47498E-01	• 48314E-01
• 51229E-01	• 55247E-01	• 59612E-01	• 64313E-01	• 69384E-01	• 74659E-01	• 80772E-01	• 87156E-01	• 94046E-01	• 10147F+00
• 10948E+00									
W									
0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
RVWALD									
0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
0.	0.	0.	0.	0.	0.	0.	0.	0.	0.
P_E									
• 116545E+05	• 16605E+05	• 16665E+05	• 16726E+05	• 16817E+05	• 16847E+05	• 16545E+05	• 15291E+05	• 12882E+05	• 11293E+05
• 98360E+04	• 85489E+04	• 74028E+04	• 64416E+04	• 57289E+04	• 53851E+04	• 53078E+04	• 5409E+04	• 578E+04	• 63758E+04
• 77020E+04	• 76013E+04	• 81278E+04	• 886529E+04	• 90624F+04	• 95845E+04	• 10174E+05	• 10923F+05	• 12019E+05	• 12759E+05

THE FOLLOWING POINT VALUES DESIGNATE THE S-COORDINATE LOCATIONS WHERE THE SOLUTIONS ARE OBTAINED DURING THE S-MARCH. YOUR PRINT STATION MUST AGREE WITH ONE OR MORE OF THE SPPOINT LOCATIONS; IE, YOU CAN PRINT ONLY AT SOLUTION STATIONS. IF THE CASE COMPLETES WITH A NORMAL STOP AND NO OUTPUT IS PRINTED, YOUR PRINT INPUT IS IN ERROR. THE ERROR CAN BE NOTATED BY COMPARING PROVAL AND PRNTVAL WITH SPPOINT.

SPOINT	• 10000E-01	• 20000E-01	• 30000E-01	• 40000E-01	• 50000E-01	• 60000E-01	• 70000E-01	• 80000E-01	• 90000E-01
• 10000E+00	• 11000E+00	• 11500E+00	• 11600E+00	• 11500E+00	• 11500E+00	• 12500E+00	• 13000E+00	• 13500E+00	• 14000E+00
• 15000E+00	• 15500E+00	• 16000E+00	• 16500E+00	• 17000E+00	• 17500E+00	• 18000E+00	• 19000E+00	• 20000E+00	• 21000E+00
• 22000E+00	• 23000E+00	• 24000E+00	• 25000E+00	• 26000E+00	• 27000E+00	• 28000E+00	• 29000E+00	• 30000E+00	• 31000E+00
• 32000E+00	• 33000E+00	• 34000E+00	• 35000E+00	• 36000E+00	• 37000E+00	• 38000E+00	• 39000E+00	• 40000E+00	• 41000E+00
• 42000E+00	• 43000E+00	• 44000E+00	• 45000E+00	• 46000E+00	• 47000E+00	• 48000E+00	• 49000E+00	• 50000E+00	• 51000E+00
• 52000E+00	• 53000E+00	• 54000E+00	• 55000E+00	• 56000E+00	• 57000E+00	• 58000E+00	• 59000E+00	• 60000E+00	• 61000E+00
• 62000E+00	• 63000E+00	• 64000E+00	• 65000E+00	• 66000E+00	• 67000E+00	• 68000E+00	• 69000E+00	• 70000E+00	• 71000E+00
• 72000E+00	• 73000E+00	• 74000E+00	• 75000E+00	• 76000E+00	• 77000E+00	• 78000E+00	• 79000E+00	• 80000E+00	• 81000E+00

.82000E+00	.83000E+00	.84000E+00	.85000E+00	.86000E+00	.87000E+00	.88000E+00	.89000E+00	.90000E+00	.91000E+00
*.92000E+00	*.93000E+00	*.94000E+00	*.95000E+00	*.96000E+00	*.97000E+00	*.98000E+00	*.99000E+00	*.10000E+01	*.10100E+01
.10200E+01	.10300E+01	.10400E+01	.10500E+01	.10600E+01	.10700E+01	.10800E+01	.10900E+01	.11000E+01	.11100E+01
*.11200E+01	*.11300E+01	*.11400E+01	*.11500E+01	*.11600E+01	*.11700E+01	*.11800E+01	*.11900E+01	*.12000E+01	*.12100E+01
*.12200E+01	*.12300E+01	*.12400E+01	*.12500E+01	*.12600E+01	*.12700E+01	*.12800E+01	*.12900E+01	*.13000E+01	*.13100E+01
*.13200E+01	*.13300E+01	*.13400E+01	*.13500E+01	*.13600E+01	*.13700E+01	*.13800E+01	*.13900E+01	*.14000E+01	*.14100E+01
*.14200E+01	*.14300E+01	*.14400E+01	*.14500E+01	*.14600E+01	*.14700E+01	*.14800E+01	*.14900E+01	*.15000E+01	*.15100E+01
*.15200E+01	*.15300E+01	*.15400E+01	*.15500E+01	0.					

## PRINT STATIONS DESIGNATED IN \$NAME1 INPUT AND GENERATED IN SETUP

## PROVAL

*.10700E+01	0.								
PRNTVAL									
*.10700E+01	*.15500E+01	*.10000E+00	*.20000E+00	*.30000E+00	*.40000E+00	*.50000E+00	*.60000E+00	*.70000E+00	*.80000E+00
*.90000E+00	*.10000E+01	*.11000E+01	*.12000E+01	*.13000E+01	*.14000E+01	*.15000E+01			

## **SIMILAR SOLUTION EQUIPPED TO INITIATE MARCHING PROCEDURE**

CONVERGED SELF-SIMILAR SOLUTION REQUIRED 15 ITERATIONS.

## INITIAL STATION PARAMETERS

MUE = .144383E-09 UE = .393777E+03 TE = .220606E+03 PE = .165451E+05 QSD = 0. XAL = .699833E+00 XRE = 0. RE = .261356E+00

ORIGINAL PAGE IS  
OF POOR QUALITY

## APPENDIX D

\*\*\*\*\*DIMENSIONAL OUTPUT QUANTITIES ARE IN S.I. UNITS\*\*\*\*

```

FREE STREAM VALUES-DIMENSIONAL
PT1 = .475108E+05 TT1 = .297800E+03 RT1 = .555966E+00 P1 =
U1 = .468092E+03 AA1 = .275348F+03 XMA = .170000E+01 REY =
                                         .962529E+04
                                         .658109E+07

REFERENCE VALUES-DIMENSIONAL
PREF = .389443E+05 TREF = .218160E+03 RREF = .177738E+00 UREF =
                                         .468002E+03 VISREF =
                                         .143045E-04 PTR =
                                         .121997E+01

```

1.0700 PROFILE

ETA	Y/YF	U/UF	T/TF	TT/TTF	CRCGCC	PT/PTR	M/MF	YPLUS	UPLUS	UDEF	VISEFF
0.	0.	0.	• 147E+01	• 977E+00	• 310E-08	• 240E+00	0.	0.	0.	0.	• 100E+01
• 757E-05	• 532F-06	• 289F-04	• 147F+01	• 977E+00	• 342E-08	• 240E+00	• 239E-04	• 107E-02	• 100E-02	• 346E+02	• 100E+01
• 172E-04	• 658E-04	• 147E+01	• 977E+00	• 177E-07	• 240E+00	• 543E-04	• 245E-02	• 228E-02	• 228E-02	• 346E+02	• 100E+01
• 296E-04	• 208E-05	• 113E-03	• 147E+01	• 977E+00	• 521E-07	• 240E+00	• 932E-04	• 419E-02	• 391E-02	• 346E+02	• 100E+01
• 453E-04	• 318E-05	• 173F-03	• 147E+01	• 977E+00	• 122E-06	• 240E+00	• 143F-03	• 642E-02	• 598E-02	• 346E+02	• 100E+01
• 653E-04	• 459E-05	• 249E-03	• 147E+01	• 977E+00	• 254E-06	• 240E+00	• 206E-03	• 927E-02	• 863E-02	• 346E+02	• 100E+01
• 909E-04	• 638E-05	• 347E-03	• 147E+01	• 977E+00	• 492E-06	• 240E+00	• 287E-03	• 120E-01	• 129E-01	• 346E+02	• 100E+01
• 123E-03	• 867E-05	• 472E-03	• 147E+01	• 977E+00	• 909E-06	• 240E+00	• 389E-03	• 175E-01	• 163E-01	• 346E+02	• 100E+01
• 165E-03	• 116E-04	• 631F-03	• 147E+01	• 977F+00	• 162E-05	• 240E+00	• 520E-03	• 234E-01	• 218E-01	• 346E+02	• 100E+01
• 218E-03	• 153E-04	• 833E-03	• 147E+01	• 977E+00	• 284E-05	• 240E+00	• 688E-03	• 309E-01	• 288E-01	• 346E+02	• 100E+01
•	•	•	•	•	•	•	•	•	•	•	•
•	•	•	•	•	•	•	•	•	•	•	•
• 672E+01	• 384F+00	• 753F+00	• 121E+01	• 997F+00	• 878E+00	• 501E+00	• 688E+00	• 105E+04	• 261E+02	• 855E+01	• 320E+02
• 857E+01	• 475E+00	• 801E+00	• 118E+01	• 999E+00	• 939E+00	• 555E+00	• 738E+00	• 178E+04	• 277E+02	• 688E+01	• 333E+02
• 109E+02	• 583E+00	• 855E+00	• 113E+01	• 1000E+01	• 999E+00	• 629E+00	• 903E+00	• 296E+04	• 296E+02	• 501E+01	• 333E+02
• 139E+02	• 710E+00	• 917E+00	• 108E+01	• 1000E+01	• 105E+01	• 727E+00	• 880I+00	• 234E+04	• 317E+02	• 289E+01	• 273E+02
• 178E+02	• 857E+00	• 981E+00	• 102E+01	• 1000E+01	• 104E+01	• 854E+00	• 972E+00	• 313E+04	• 340E+02	• 649E+00	• 130E+02
• 227E+02	• 103E+01	• 998E+00	• 100E+01	• 1000E+01	• 996E+00	• 892E+00	• 997E+00	• 267E+04	• 387E+02	• 753E-01	• 187E+02
• 289E+02	• 124E+01	• 100E+01	• 100E+01	• 1000E+01	• 101E+01	• 898E+00	• 1000E+01	• 467E+04	• 646E+02	• 129E+01	• 255E-01
• 369E+02	• 148E+01	• 100E+01	• 100E+01	• 1000E+01	• 101E+01	• 896E+00	• 1000E+01	• 569E+04	• 346E+02	• 980E-02	• 100E+01
• 470E+02	• 178E+01	• 100E+01	• 100E+01	• 1000E+01	• 101E+01	• 897E+00	• 1000E+01	• 671E+04	• 346E+02	• 107E-01	• 100E+01
• 600E+02	• 213E+01	• 100E+01	• 100E+01	• 1000E+01	• 1000E+01	• 997F+00	• 1000E+01	• 803E+04	• 346E+02	• 163E-07	• 100E+01

S	=	*10700E+01	RETHET=	*14735E+05	DPEDS =	*73790E+00	CFW =	*16699E-02	ZSHK =	*0.	YE =	*19267E-01
XI	=	*66998E-02	RES	=	*72574E+07	OTEDS =	*28226E+03	QSD =	*0.	RSHK	=	*0.
RMI	=	*49397E-01	PE	=	*11381E+05	DUEDS =	*29544E+03	HD =	*0.	ITRO	=	*0.
Z	=	*10446E+01	TE	=	*19824E+03	DLTAST =	*55260E-02	NSTE =	=	TW/T1=	=	*97708E+00
BETA	=	- *41437E+01	RE	=	*20006E+00	THETA =	*21724E-02	NSTW =	=	RFTRUE=	=	*93145E+00
XAL	=	*10045E+01	UE	=	*44720E+03	FORM =	*25437E+01	NUE =	=	P20 =	=	*12142E+01
RVWALD=	0.	*37481E+05	ME	=	*15847E+01	TAUD =	*22759E+02	NUW =	=	ROUSE =	=	*25905E+05
REDELT=	*37481E-04	MUE	=	*13191E-04	CFE =	*11377E-02	SWANG =	=	DSMX0 =	=	*41465E-03	
NOTER=	*98881E-05	ERRDP =	3									*43617E+04
												RVWAL = 0.
												VW = 0.

TEST CASE NO. 2 ;  $W = 0$   
 NOTE : ALL INPUT WITH THE EXCEPTION OF  $W = 0$  IN \$NAME! IS IDENTICAL TO CASE FOR  $W = 1$  ; CONSEQUENTLY, ONLY THE PROFILE AND WALL PRINT AT  $S = 1.07 M$  ARE PRESENTED.

1-0700 PROFILE

## APPENDIX D

**ORIGINAL PAGE IS  
OF POOR QUALITY**

ORIGINAL PAGE IS  
OF POOR QUALITY

APPENDIX D

TEST CASE NO. 3

THE LISTING FOR TEST CASE 3 INCLUDES THE FOLLOWING: (1) VARDIM DATA; (2) \$NAMI AND \$NAM2 INPUT;  
(3) INITIAL STATION SOLUTION VALUES; (4) REFERENCE VALUES; (5) PROFILE AND WALL PRINTS.  
NOTE: THREE RUNS ARE INCLUDED IN THIS TEST CASE: RWALD = 0 ; RWALD < 0 ; RWALD > 0 .

TEST CASE NO. 3 ; RWALD = 0.

PREPROCESSOR CONTROL CARDS

```
*VARDIM/VGBLP(JK=43,JL=1,JM=30,JN=3,JI=1,JH=85)
*VARDIM/TABLE(JJ=11,JH=85)
*VARDIM/VARENTIAL(11)
*VAROIM/TURBLNT(JI=1,JK=43)
*VARDIM/MESH(JK=43)
*VARDIM/SIMILAR(JK=43)
*VARDIM/SCLEVE(JK=43)
```

```
$NAMI
IGEDM = 1 XEND = *1000CE+02 IE = *1000CE+02 IGAS = *1275E+01 DETA1 = 0.
PT1 = *41400E+07 TTI = *83300E+03 IGAS = *14582E+01 VIS1C1 = *74000E+01
VIS2C1 = 0.
VIS2C2 = C. G. = *1400CE+C11 R = *2869CE+03 PR = *7200CE+00
IBODY = 2 WAVE = *92140E+01 PHII = *50000E+01 J = 1 W = - O IENTRO = 1
SST = *10000E+09 SMXT@ = *1000CE+09 KUVIS = *16800E-01 XT3 = *20000E+01 IYINT = 1
KODAMP = 2 XT1 = *4000CE+0C XT2 = *50000E+01 XT4 = *78000E+00 XT5 = *10800E+01
XT6 = *26000E+02 PRT = *9500CE+00 KCDPRT = 1 NUMR1 = 0.
PRTAR
0.
IEND1 = 84 PROINC = *10000E+00 PKTINC = *1000CF-C1 IPRNT = 0
PT = *10000E+01 KODE = C KGDWAL = 1 VELEDG = *99500E+00 CUNV = *10000E-03
KODUNIT = 1 ITMAX = 3 CGNVE = *10000E-01 NAUXPRO = 0
NITMAX = 5
```

THIS COMPLETES THE OUTPUT OF \$NAMI WITH THE EXCEPTION OF PROVAL AND PRNTVAL. THESE VALUES ARE PRINTED JUST PRIOR TO THE INITIAL STATION PRINT.

## APPENDIX D

ORIGINAL PAGE IS  
OF POOR QUALITY

THE FOLLOWING SPOINT VALUES DESIGNATE THE S-COORDINATE LOCATIONS WHERE THE SJLUTIONS ARE OBTAINED DURING THE S-MARCH. YOUR PRINT STATION MUST AGREE WITH ONE OR MORE OF THE SPOINT LOCATIONS; IE, YOU CAN PRINT ONLY AT SOLUTION STATIONS. IF THE CASE COMPLETES WITH A NORMAL STOP AND NO OUTPUT IS PRINTED, YOUR PRINT INPUT IS IN ERROR. THE ERROR CAN BE NOTED BY COMPARING PROVAL AND PRNTVAL WITH SPOINT.

SPOINT	*10000E-01	*15000E-01	*20000E-01	*25000E-01	*30000E-01	*35000E-01	*40000E-01	*45000E-01	*50000E-01
*50000E-02	*60000E-01	*65000E-01	*70000E-01	*75000E-01	*80000E-01	*85000E-01	*90000E-01	*91000E-01	*92000E-01
*55000E-01	*94000E-01	*95000E-01	*96000E-01	*97000E-01	*98000E-01	*99000E-01	*100000E+00	*101000E+00	*102000E+00
*93000E-01	*10400E+00	*10500E+00	*10600E+00	*10700E+00	*10800E+00	*10900E+00	*11000E+00	*11100E+00	*11200E+00
*10300E+00	*11400E+00	*11500E+00	*11600E+00	*11700E+00	*11800E+00	*11900E+00	*12000E+00	*12500E+00	*13000E+00
*11300E+00	*14000E+00	*14500E+00	*15000E+00	*15500E+00	*16000E+00	*16500E+00	*17000E+00	*17500E+00	*18000E+00
*13500E+00	*19000E+00	*19500E+00	*20000E+00	*20500E+00	*21000E+00	*21500E+00	*22000E+00	*22500E+00	*23000E+00
*18500E+00	*24000E+00	*24500E+00	*25000E+00	*25500E+00	*26000E+00	*26500E+00	*27000E+00	*27500E+00	*28000E+00
*23500E+00	*28500E+00	*29000E+00	*29500E+00	*30000E+00					

PRINT STATIONS DESIGNATED IN \$NAM1 INPUT AND GENERATED IN SETUP

PROVAL	*20000E+00	*30000E+00							
PRNTVAL	*20000E-01	*30000E-01	*40000E-01	*50000E-01	*60000E-01	*70000E-01	*80000E-01	*90000E-01	*100000E+00
*10000E-01	*12000E+00	*13000E+00	*14000E+00	*15000E+00	*16000E+00	*17000E+00	*18000E+00	*19000E+00	*20000E+00
*11000E+00	*22000E+00	*23000E+00	*24000E+00	*25000E+00	*26000E+00	*27000E+00	*28000E+00	*29000E+00	*30000E+00
*21000E+00									

## APPENDIX D

**ORIGINAL PAGE  
OF POOR QUALITY**

## SIMILAP SOLUTION REQUIRED TO INITIATE MARCHING PROCEDURE

PROFILE VALUES						
ETA	U/UE	T/TE	V	FZ	TZ	XL
0.	0.	.3848058E+01	0.	.497793E+00	.214623E+01	.884947E+00
*163732E-03	*815055E-04	*384893E+01	-.667252E-08	*497806E+00	*214598E+01	*884928E+00
*372556E-03	*185460E-03	*384938E+01	-.345469E-07	*497820E+00	*214504E+01	*884903E+00
*638889E-03	*318046E-03	*384995E+01	-.101598E-06	*497838E+00	*214422E+01	*884871E+00
*978571E-03	*487158E-03	*385068E+01	-.238355E-06	*497862E+00	*214318E+01	*884831E+00
*141180E-02	*702852E-03	*385161E+01	-.496129E-06	*497892E+00	*214186E+01	*884779E+00
*196434E-02	*977966E-03	*385279E+01	-.960490E-06	*497930E+00	*214017E+01	*884714E+00
*266906E-02	*132888E-02	*385430E+01	-.177332E-05	*497978E+00	*213891E+01	*884630E+00
*356785E-02	*177448E-02	*385622E+01	-.316865E-05	*498040E+00	*213526E+01	*884523E+00
*471416E-02	*234742E-02	*385867E+01	-.553249E-05	*498119E+00	*213174E+01	*884388E+00
.	.	.	.	.	.	.
.	.	.	.	.	.	.
*111938E+01	*556641E+00	*421333E+01	-.316420E+00	*436282E+00	-.136939E+01	*865131E+00
*142782E+01	*684086E+00	*371567E+01	-.507796E+00	*363826E+00	-.177287E+01	*892238E+00
*182121E+01	*812184E+00	*296909E+01	-.802102E+00	*261914E+00	-.179556E+01	*935873E+00
*232293E+01	*918527E+00	*210844E+01	-.123627E+01	*148601E+00	-.137770E+01	*965428E+00
*296283E+01	*981830E+00	*139627E+01	-.184429E+01	*563286E-01	-.731029E+00	*101057E+01
*377896E+01	*100545E+01	*104405E+01	-.265322E+01	*966652E-02	-.217523E+00	*102929E+01
*481984E+01	*999781E+00	*992329E+00	-.369428E+01	-.212271E-03	-.179766E-01	*999332E+00
*614739E+01	*100004E+01	*100147E+01	-.502171E+01	*372291E-04	*169536E-02	*100011E+01
*784055E+01	*999893E+00	*997450E+00	-.671481E+01	-.105317E-04	-.38171UE-03	*999813E+00
*100000E+02	*100000E+01	*100000E+01	-.8877415E+01	0.	0.	*100000E+01
CONVERGED SELF-SIMILAR SOLUTION REQUIRED 15 ITERATIONS.						

## INITIAL STATION PARAMETERS

MUE = .565042E-05	UE = .122800E+04	TE = .822781E+02	PE = .124651E+04	QSD = 0.
XAL = .182484E+02	XAE = 0.	RE = .527947E-01		

\*\*\*DIMENSIONAL OUTPUT QUANTITIES ARE IN S.I. UNITS \*\*\*

```

FREE STREAM VALUES-DIMENSIONAL
PT1 = .414000E+07 TT1 =
U1 = .123625E+04 AA1 =
*833000E+03 RT1 =
.167331E+03 XMA =
*740000E+C1 P1 =
REY =
*.713195E+02 *.701388E+03
*.921384E+07
REFERENCE VALUES-DIMENSIONAL
PREF2 = 5.277124E+05 TREF2 =
*152661E+04 KREF =
*3.500699E-01 UREF =
*.123825E+04 VISREF =
*.531367E-04 PTR =
*.769929E+02

```

REFERENCE VALUES-DIMENSIONAL										XLM11										
PREF=	• 537712t+05	TPEF=	• 152661E+04	KREF=	• 3500699E-01	UREF=	• 123825E+04	VISREF=	• 531367E-04	PTR =	• 769929E+02									
• 1000 PROFILE																				
ETA																				
0.	0.	0.	• 815E-04	• 385E+01	• 380E+00	• 573E-14	• 301E-03	• 498E+00	• 214E+01	• 885E+00	• 342E-05	0.	• 885E+00							
• 164E-03	• 625E-04	• 115E-03	• 142E-03	• 385E+01	• 380E+00	• 560E-04	• 301E-03	• 415E-04	• 214E+01	• 98E+00	• 177E-04	0.	• 177E-04	• 521E-04	• 214E+01	• 98E+00	• 177E-04	• 521E-04	• 214E+01	
• 373E-03	• 244E-03	• 318E-03	• 487E-03	• 385E+01	• 380E+00	• 528E-03	• 218E-03	• 162E-03	• 214E+01	• 98E+00	• 248E-03	0.	• 248E-03	• 214E+01	• 98E+00	• 248E-03	• 214E+01	• 98E+00	• 248E-03	
• 639E-03	• 374E-03	• 703E-03	• 539E-03	• 385E+01	• 380E+00	• 534E-03	• 334E-03	• 162E-03	• 214E+01	• 98E+00	• 358E-03	0.	• 358E-03	• 214E+01	• 98E+00	• 358E-03	• 214E+01	• 98E+00	• 358E-03	
• 979E-03	• 141E-02	• 978E-03	• 751E-03	• 385E+01	• 381E+00	• 567E-03	• 672E-03	• 162E-03	• 214E+01	• 98E+00	• 498E-03	0.	• 498E-03	• 214E+01	• 98E+00	• 498E-03	• 214E+01	• 98E+00	• 498E-03	
• 196E-02	• 267E-02	• 1133E-02	• 102E-02	• 385E+01	• 381E+00	• 591E-03	• 701E-03	• 167E-03	• 214E+01	• 98E+00	• 677E-03	0.	• 677E-03	• 214E+01	• 98E+00	• 677E-03	• 214E+01	• 98E+00	• 677E-03	
• 357E-02	• 136E-02	• 178E-02	• 235E-02	• 386E+01	• 381E+00	• 586E-02	• 692E-02	• 172E-02	• 213E+01	• 98E+00	• 905E-03	0.	• 905E-03	• 213E+01	• 98E+00	• 905E-03	• 213E+01	• 98E+00	• 905E-03	
• 471E-02	• 180E-02	• 236E-02	• 308E-02	• 386E+01	• 381E+00	• 586E-02	• 692E-02	• 161E-02	• 213E+01	• 98E+00	• 119E-02	0.	• 119E-02	• 213E+01	• 98E+00	• 119E-02	• 213E+01	• 98E+00	• 119E-02	
• 618E-02	• 236E-02	• 308E-02	• 386E-02	• 386E+01	• 381E+00	• 586E-02	• 692E-02	• 212E-02	• 213E+01	• 98E+00	• 156E-02	0.	• 156E-02	• 213E+01	• 98E+00	• 156E-02	• 213E+01	• 98E+00	• 156E-02	
• 112E+01	• 475E+00	• 557E+00	• 421E+01	• 696E+00	• 421E+01	• 509E+00	• 145E-02	• 271E+00	• 436E+00	• 436E+00	• 135E+03	0.	• 135E+03	• 246E+03	• 135E+03	• 246E+03	• 135E+03	• 246E+03	• 135E+03	
• 143E+01	• 591E+00	• 684E+00	• 372E+01	• 789E+00	• 684E+00	• 659E+00	• 237E-02	• 355E+00	• 364E+00	• 364E+00	• 936E+00	0.	• 936E+00	• 262E+00	• 364E+00	• 936E+00	• 262E+00	• 364E+00	• 936E+00	
• 182E+01	• 714E+00	• 812E+00	• 297E+01	• 888E+00	• 812E+00	• 819E+00	• 407E-02	• 471E+00	• 471E+00	• 471E+00	• 949E+00	0.	• 949E+00	• 149E+00	• 949E+00	• 949E+00	• 149E+00	• 949E+00	• 949E+00	
• 232E+01	• 833E+00	• 918E+00	• 211E+01	• 988E+00	• 918E+00	• 949E+00	• 721E-02	• 632E+00	• 632E+00	• 632E+00	• 123E+01	0.	• 123E+01	• 123E+01	• 931E+00	• 123E+01	• 123E+01	• 931E+00	• 123E+01	
• 296E+01	• 933E+00	• 982E+00	• 140E+01	• 101E+01	• 101E+01	• 101E+01	• 101E+01	• 123E+01	• 123E+01	• 123E+01	• 101E+01	0.	• 101E+01	• 564E-01	• 731E+00	• 159E+04	• 731E+00	• 159E+04	• 731E+00	
• 378E+01	• 103E+01	• 100E+01	• 104E+01	• 101E+01	• 101E+01	• 998E+00	• 171E-01	• 979E+00	• 979E+00	• 979E+00	• 110E+01	0.	• 110E+01	• 998E+00	• 698E-02	• 218E+00	• 793E+03	• 218E+00	• 793E+03	• 218E+00
• 482E+01	• 112E+01	• 100E+01	• 100E+01	• 998E+00	• 998E+00	• 998E+00	• 180E-01	• 100E+01	• 100E+01	• 100E+01	• 100E+01	0.	• 100E+01	• 180E-01						
• 615E+01	• 124E+01	• 100E+01	• 100E+01	• 997E+00	• 997E+00	• 997E+00	• 178E-01	• 998E+00	• 998E+00	• 998E+00	• 100E+01	0.	• 100E+01	• 178E-01	• 998E+00	• 370E-04	• 170E-02	• 170E-02	• 170E-02	
• 789E+01	• 139E+01	• 100E+01	• 100E+01	• 997E+00	• 997E+00	• 997E+00	• 179E-01	• 998E+00	• 998E+00	• 998E+00	• 100E+01	0.	• 100E+01	• 179E-01	• 998E+00	• 105E-04	• 382E-03	• 382E-03	• 382E-03	
• 100E+02	• 159E+01	• 100E+01	• 100E+01	• 100E+01	• 100E+01	• 100E+01	• 178E-01	• 100E+01	• 100E+01	• 100E+01	• 100E+01	0.	• 100E+01	• 178E-01	• 100E+01					

APPENDIX D

S	-10000E+00	RETHET	.37964E+03	DPEDS	0.	CFW	.38783E-02	ZSHK	0.	YE	.76769E-03
XI	-40149E-06	RES	.11474E+07	DTEDS	0.	QSD	-.16140E+05	RSHK	0.	UTAU	0.
RMI	-87146E-02	PE	.12465E+04	DUEDS	0.	HD	.40086E+02	ITRO	0.	TRFCT	0.
Z	-99619E-01	TE	.82278E+02	DLTAST	.56296E-03	NSTE	.61611E-03	TW/TITI	.38014E+00	YMP	0.
BETA	0.	RE	.52795E-01	THETA	.33088E-04	NSTW	.23712E-02	RFTRUE	.31220E+00	P20	.76543E+02
XAL	.18248E+02	UE	.12280E+04	FORM	.17014E+02	NUE	.50898E+03	ROUSE	.15917E+04	OMEGA	.11062E-02
RWALD	0.	ME	.67543E+01	TAUD	.40114E+02	NUN	.14945E+03	DSMMXO	.85922E+04		
KEDLT	.64593E+04	MUE	.26504E-05	CFE	.10377E-02	SWANG	0.	VW	0.	RWVAL	0.
NOITER	2	ERROR	.36994E-10								
S	-11000E+00	RETHFT	.39819E+03	DPEDS	0.	CFW	.36976E-02	ZSHK	0.	YE	.80673E-03
XI	-5353E-06	RES	.12621E+07	DTEDS	0.	QSD	-.15388E+05	RSHK	0.	UTAU	0.
RMI	-95867E-02	PE	.12465E+04	DUEDS	0.	HD	.38219E+02	ITRO	0.	TRFCT	0.
Z	-10558E+00	TE	.82278E+02	DLTAST	.59289E-03	NSTE	.58741E-03	TW/TITI	.38014E+00	YMP	0.
BETA	0.	RE	.52795E-01	THETA	.34705E-04	NSTW	.22607E-02	RFTRUE	.31220E+00	P20	.76543E+02
XAL	.18248E+02	UE	.12280E+04	FORM	.17084E+02	NUE	.53379E+03	ROUSE	.16754E+04	OMEGA	.11062E-02
RWALD	0.	ME	.67543E+01	TAUD	.38245E+02	NUN	.15673E+03	DSMMXO	.81947E+04		
KEDLT	.68028E+04	MUE	.56504E-05	CFE	.96077E-03	SWANG	0.	VW	0.	RWVAL	0.
NOITER	2	ERROR	.26056E-10								

## APPENDIX D

TEST CASE NO. 3 : RYWARD < O.  
NOTE : ALL INPUT WITH THE EXCEPTION OF RYWARD IS IDENTICAL TO THE CASE FOR RYWARD = O ;  
CONSEQUENTLY ONLY RYWARD INPUT AND THE PROFILE AND WALL PRINTS ARE PRESENTED.

RWALD	0.	- .90117E-01 - .90117E-01 - .90117E-01 - .90117E-01 - .90117E-01
0.	- .90117E-01	

1600 PROFILE

S	-	*10000E+00	RETHET	*33251E+03	DPEDS	- 0.	CFW	- *86813E-02	ZSHK	- 0.	YE	- *63846E-03
XI	-	*40149E-06	RES	*11474E+07	DTEDS	- 0.	QSD	- *.34131E-05	RSHK	- 0.	UTAU	- 0.
RMI	-	*87146E-02	PE	*12465E+04	DUEDS	- 0.	HD	- *84770E+02	ITKO	- 0.	TRFC	- 0.
Z	-	*99619E-01	TE	*82278E+02	DLTAST	- *46610E-03	NSTE	- *13029E-02	TW/TI	- *38014E+00	YMP	- 0.
BETA	-	0.	RE	*52795E-01	THETA	- *28980E-04	NSTW	- *.50142E-02	RFTURE	- *31220E+00	P20	- *76543E+02
XAL	-	*18248E+02	UE	*12280E+04	FORM	- *16084E+02	NUE	- *.10763E+04	ROUSE	- *.10359E+04	OMEGA	- *11062E-02
RWALD	-	*90117E-01	ME	*67543E+01	TAUD	- *.89792E+02	NUW	- *.31603E+03	DSMXO	- *.88939E+03	VW	- *12151E+01
REDLT	-	*53480E+04	MUE	*56504E-05	CFE	- *.22557E-02	SWANG	- 0.	RWAL	- *13900E-02		
NOITER	-	4	ERROR	*90073E-04								
S	-	*11000E+00	RETHET	*28837E+03	DPEDS	- 0.	CFW	- *10460E-01	ZSHK	- 0.	YE	- *58139E-03
XI	-	*53453E-06	RES	*12621E+07	DTEDS	- 0.	QSD	- *.42263E+05	RSHK	- 0.	UTAU	- 0.
RMI	-	*95867E-02	PE	*12465E+04	DUEDS	- 0.	HD	- *10497E+03	ITKO	- 0.	TRFC	- 0.
Z	-	*10958E+00	TE	*82278E+02	DLTAST	- *41139E-03	NSTE	- *.16133E-02	TW/TI	- *38014E+00	YMP	- 0.
BETA	-	0.	RE	*52795E-01	THETA	- *25133E-04	NSTW	- *.62089E-02	RFTURE	- *31220E+00	P20	- *76543E+02
XAL	-	*18248E+02	UE	*12280E+04	FORM	- *.16369E-02	NUE	- *.14661E+04	ROUSE	- *.85055E+03	OMEGA	- *11062E-02
RWALD	-	*90117E-01	ME	*67543E+01	TAUD	- *.10819E+03	NUW	- *.43046E+03	DSMXO	- *.15633E+05	VW	- *.12745E+01
REDLT	-	*47202E+04	MUE	*56504E-05	CFE	- *.27179E-02	SWANG	- 0.	RWAL	- *13900E-02		
NOITER	-	2	ERROR	*19737E-04								

TEST CASE NO. 3 : RVWALD > O ;  
NOTE : ALL INPUT WITH THE EXCEPTION OF RVWALD IN SNAME IS IDENTICAL TO THE CASE FOR RVWALD = O ;  
CONSEQUENTLY ONLY RVWALD INPUT AND THE PROFILE AND WALL PRINTS ARE PRESENTED.

S		10000E+00	PETHET	-44266E+03	UPEDS	0.	CFW	.70232E-03	ZSHK	0.	YE	.10200E-02
XI		40149E-06	RES	.11474E+07	DTECS	0.	QSD	-.38437E+04	RSHK	0.	UTAU	0.
RMI		87146E-02	PE	.12465E+04	DUEDS	0.	HD	.95464E+01	ITRD	0.	TRFC	0.
Z		99619E-01	TE	.82278E+02	DLTAST	.75760E-03	NSTE	.14672E-03	TW/T1	.38014E+00	YMP	*****
BETA	0.		RE	.52795E-01	THETA	.38580E-04	NSTW	0.	RTRUE	.31220E+00	P20	.76543E+02
XAL		18248E+02	UE	.12280E+04	FORM	.19637E+02	NUE	.12121E+03	ROUSE	.27699E+04	OMEGA	.11062E-02
RVWALD		90117E-01	ME	.67543E+01	TAUD	.72642E+01	NUM	.35590E+02	DSMXO	.58418E+04		
KEDLT		86926E+04	MUE	.56504E-05	CFE	.18249E-03	SWANG	1	VW	.12151E+01	RVWAL	.13900E-02
NOITER	6		ERROR	.15178E-02								
S		11000E+00	RETHET	58659E+03	DPEOS	0.	CFW	.78597E-04	ZSHK	0.	YE	.15302E-02
XI		53453E-06	RES	.12621E+07	DTECS	0.	QSD	-.52038E+03	RSHK	0.	UTAU	0.
RMI		95667E-02	PE	.12465E+04	DUEDS	0.	HD	.12924E+01	ITRD	0.	TRFC	0.
Z		10958E+00	TE	.82278E+02	DLTAST	.11162E-02	NSTE	.19864E-04	TW/T1	.38014E+00	YMP	*****
BETA	0.		RE	.52795E-01	THETA	.51124E-04	NSTW	0.	RTRUE	.31220E+00	P20	.76543E+02
XAL		18248E+02	UE	.12280E+04	FORM	.21834E+02	NUE	.18051E+02	ROUSE	.51653E+04	OMEGA	.11062E-02
RVWALD		90117E-01	ME	.67543E+01	TAUD	.81295E+00	NUM	.53002E+01	DSMXO	.13475E-06		
KEDLT		12808E+05	MUE	.56504E-05	CFE	.20422E-04	SWANG	1	VW	.12745E+01	RVWAL	.13900E-02
NOITER	6		ERROP	.10152E-01								

SOLUTION HAS RESULTED IN GENERATION OF NEGATIVE TEMPERATURE WHICH CANNOT BE PHYSICALLY ACCEPTED. THIS GENERALLY OCCURS IN THE REGION OF ADVERSE PRESSURE GRADIENT AND/OR MASS INJECTION AT WALL BOUNDARY AND IS AN INDICATION OF BOUNDARY LAYER SEPARATION.  
 IF UPEDS IS NEGATIVE AND THERE IS NO MASS INJECTION AT THE WALL BOUNDARY, THE PROBLEM IS PROBABLY CAUSED BY TOO COURSE A STEP SIZE IN THE S-COORDINATE.

T3(N) = -5.8932609N = 36 H = 46

## APPENDIX D

ORIGINAL PAGE IS  
OF POOR QUALITY

TEST CASE NO. 4

THE LISTING FOR TEST CASE NO. 4 INCLUDES THE FOLLOWING: (1) VARDIM DATA; (2) NAME AND SNATE ANG.; (3) INITIAL STATION SOLUTION; (4) REFERENCE VALUES; (5) PROFILE AND WALL PRINTS AT S=.0695 M. NOTE: TWO OUTPUT LISTINGS OF RESULTS FOLLOW: (1) THE FIRST PASS OVER THE BODY CORRESPONDS TO CONSTANT ENTROPY CONDITIONS; (2) THE FINAL PASS OVER THE BODY FOR THE CONVERGED VARIABLE ENTROPY SOLUTION.

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* VARDIM/VGBLP (JK= 43,JL= 33,JM= 33,JN=2,JI=1,JP= 34)
* VARDIM/STABLE (JJ=150,JH= 34)
* VARDIM/VARENTI (JL= 33)
* VARDIM/TURBLNT (JI= 1,JK= 43)
* VARDIM/MESH(JK= '43)
* VARDIM/SIMILAR (JK= 43)
* VARDIM/SOLVE (JK= 43)

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THIS COMPLETES THE OUTPUT OF \$NAME WITH THE EXCEPTION OF PROVAL AND PRNTVAL. THESE VALUES ARE PRINTED JUST PRIOR TO THE INITIAL STATION PRINT.

1ENI	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30	31	32	33	34	35	36	37	38	39	40	41	42	43	44	45	46	47	48	49	50	51	52	53	54	55	56	57	58	59	60	61	62	63	64	65	66	67	68	69	70	71	72	73	74	75	76	77	78	79	80	81	82	83	84	85	86	87	88	89	90	91	92	93	94	95	96	97	98	99	100	101	102	103	104	105	106	107	108	109	110	111	112	113	114	115	116	117	118	119	120	121	122	123	124	125	126	127	128	129	130	131	132	133	134	135	136	137	138	139	140	141	142	143	144	145	146	147	148	149	150	151	152	153	154	155	156	157	158	159	160	161	162	163	164	165	166	167	168	169	170	171	172	173	174	175	176	177	178	179	180	181	182	183	184	185	186	187	188	189	190	191	192	193	194	195	196	197	198	199	200	201	202	203	204	205	206	207	208	209	210	211	212	213	214	215	216	217	218	219	220	221	222	223	224	225	226	227	228	229	230	231	232	233	234	235	236	237	238	239	240	241	242	243	244	245	246	247	248	249	250	251	252	253	254	255	256	257	258	259	260	261	262	263	264	265	266	267	268	269	270	271	272	273	274	275	276	277	278	279	280	281	282	283	284	285	286	287	288	289	290	291	292	293	294	295	296	297	298	299	300	301	302	303	304	305	306	307	308	309	310	311	312	313	314	315	316	317	318	319	320	321	322	323	324	325	326	327	328	329	330	331	332	333	334	335	336	337	338	339	340	341	342	343	344	345	346	347	348	349	350	351	352	353	354	355	356	357	358	359	360	361	362	363	364	365	366	367	368	369	370	371	372	373	374	375	376	377	378	379	380	381	382	383	384	385	386	387	388	389	390	391	392	393	394	395	396	397	398	399	400	401	402	403	404	405	406	407	408	409	410	411	412	413	414	415	416	417	418	419	420	421	422	423	424	425	426	427	428	429	430	431	432	433	434	435	436	437	438	439	440	441	442	443	444	445	446	447	448	449	450	451	452	453	454	455	456	457	458	459	460	461	462	463	464	465	466	467	468	469	470	471	472	473	474	475	476	477	478	479	480	481	482	483	484	485	486	487	488	489	490	491	492	493	494	495	496	497	498	499	500	501	502	503	504	505	506	507	508	509	510	511	512	513	514	515	516	517	518	519	520	521	522	523	524	525	526	527	528	529	530	531	532	533	534	535	536	537	538	539	540	541	542	543	544	545	546	547	548	549	550	551	552	553	554	555	556	557	558	559	560	561	562	563	564	565	566	567	568	569	570	571	572	573	574	575	576	577	578	579	580	581	582	583	584	585	586	587	588	589	590	591	592	593	594	595	596	597	598	599	600	601	602	603	604	605	606	607	608	609	610	611	612	613	614	615	616	617	618	619	620	621	622	623	624	625	626	627	628	629	630	631	632	633	634	635	636	637	638	639	640	641	642	643	644	645	646	647	648	649	650	651	652	653	654	655	656	657	658	659	660	661	662	663	664	665	666	667	668	669	670	671	672	673	674	675	676	677	678	679	680	681	682	683	684	685	686	687	688	689	690	691	692	693	694	695	696	697	698	699	700	701	702	703	704	705	706	707	708	709	710	711	712	713	714	715	716	717	718	719	720	721	722	723	724	725	726	727	728	729	730	731	732	733	734	735	736	737	738	739	740	741	742	743	744	745	746	747	748	749	750	751	752	753	754	755	756	757	758	759	760	761	762	763	764	765	766	767	768	769	770	771	772	773	774	775	776	777	778	779	780	781	782	783	784	785	786	787	788	789	790	791	792	793	794	795	796	797	798	799	800	801	802	803	804	805	806	807	808	809	810	811	812	813	814	815	816	817	818	819	820	821	822	823	824	825	826	827	828	829	830	831	832	833	834	835	836	837	838	839	840	841	842	843	844	845	846	847	848	849	850	851	852	853	854	855	856	857	858	859	860	861	862	863	864	865	866	867	868	869	870	871	872	873	874	875	876	877	878	879	880	881	882	883	884	885	886	887	888	889	890	891	892	893	894	895	896	897	898	899	900	901	902	903	904	905	906	907	908	909	910	911	912	913	914	915	916	917	918	919	920	921	922	923	924	925	926	927	928	929	930	931	932	933	934	935	936	937	938	939	940	941	942	943	944	945	946	947	948	949	950	951	952	953	954	955	956	957	958	959	960	961	962	963	964	965	966	967	968	969	970	971	972	973	974	975	976	977	978	979	980	981	982	983	984	985	986	987	988	989	990	991	992	993	994	995	996	997	998	999	1000
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## APPENDIX D

ORIGINAL PAGE IS  
OF POOR QUALITY

## APPENDIX D



THE FOLLOWING SPOINT VALUES DESIGNATE THE S-COORDINATE LOCATIONS WHERE THE SOLUTIONS ARE OBTAINED FOR ANS VECTORS... IF YOUR PRINT STATION MUST AGREE WITH ONE OR MORE OF THE SPOINT LOCATIONS; IE., YOU CAN PRINT ONLY AT SOLUTION STATIONS. IF THE CASE COMPLETES WITH A NORMAL STOP AND NO OUTPUT IS PRINTED, YOUR PRINT INPUT IS IN ERROR. THE ERROR CAN BE NOTED BY COMPARING PROVAL AND PRNTVAL WITH SPOINT.

SPOINT	SPINT	SPINT	SPINT	SPINT	SPINT
-1.5000E-02	-3.0000E-02	-4.5000E-02	-6.0000E-02	-7.5000E-02	-9.0000E-02
-1.8000E-01	-1.8000E-01	-1.9500E-01	-2.1000E-01	-2.2500E-01	-2.4000E-01
-3.1500E-01	-3.3000E-01	-3.4500E-01	-3.6000E-01	-3.7500E-01	-3.9000E-01
-4.6500E-01	-4.8000E-01	-4.9500E-01	-5.1000E-01	-5.2500E-01	-5.4000E-01

```

$NAM3
NUMBER = 30
RRS
0.    *76200E-03   *15240E-02   *22860E-02   *30480E-02   *38100E-02   *45720E-02   *53340E-02   *60960E-02   *68880E-02
      *83820E-02   *91440E-02   *9060E-02   *10668E-01   *11430E-01   *12192E-01   *12954E-01   *13716E-01   *14478E-01
      *15240E-01   *16002E-01   *16764E-01   *17526E-01   *18288E-01   *19050E-01   *19812E-01   *22860E-01   *34290E-01
      0.          0.          0.          0.          0.          0.          0.          0.          0.          0.
Z7S
-41910E-02   -41605E-02   -41453E-02   -40843E-02   -39624E-02   -38100E-02   -36576E-02   -34900E-02   -33223E-02   -31090E-02
-428575E-02   -26213E-02   -23470E-02   -20726E-02   -17678E-02   -14630E-02   -10973E-02   -76200E-03   -41148E-03   -60960E-04
      0.          0.          0.          0.          0.          0.          0.          0.          0.          0.
      0.          0.          0.          0.          0.          0.          0.          0.          0.          0.
DRSDZS
-24984E+02   .333348E+02   .29853E+01   .27775E+01   .26314E+01   .25000E+01   .22728E+01   .21740E+01   .22222E+01   .21739E+01
      .31251E+01   .166667E+01   .16130E+01   .15385E+01   .13986E+01   .13333E+01   .13889E+01   .13277E+01   .14000E+01
      0.          0.          0.          0.          0.          0.          0.          0.          0.          0.
      0.          0.          0.          0.          0.          0.          0.          0.          0.          0.
PRINT STATIONS DESIGNATED IN $NAMI INPUT AND GENERATED IN SETUP
PROVAL
*49500E-01   *30000E-01
PRNTVAL
*15000E-02   *30000E-02   *45000E-02   *60000E-02   *75000E-02   *90000E-02   *10500E-01   *12000E-01   *13500E-01   *15000E-01
      *16500E-01   *18000E-01   *19500E-01   *21000E-01   *22500E-01   *24000E-01   *25500E-01   *27000E-01   *28500E-01   *30000E-01
      *31500E-01   *33000E-01   *34500E-01   *36000E-01   *37500E-01   *39000E-01   *40500E-01   *42000E-01   *43500E-01   *45000E-01
      0.          0.          0.          0.          0.          0.          0.          0.          0.          0.

```

SIMILAR SOLUTION REQUIRED TO INITIATE MARCHING PROCEDURE

PROFILE VALUES		T/TE	V	FZ	TZ	XL
ETA	UE/UE					
0.	0.	.999615E+00	0.	.928175E+00	.180125E-03	.100014E+01
*.250000E+00	*.216480E+00	.999660E+00	-.270599E-01	.803662E-00	.179292E-03	.100012E+01
*.500000E+00	*.401831E+00	.999705E+00	-.104349E+00	.680178E+00	.177286E-03	.100010E+01
*.750000E+00	*.556554E+00	.999749E+00	-.226147E+00	.560071E+00	.172371E-03	.100009E+01
*.100000E+01	*.681867E+00	.999791E+00	-.378949E+00	.446656E+00	.163709E-03	.100007E+01
*.125000E+01	*.779882E+00	.999831E+00	-.561668E+00	.343457E-00	.151070E-03	.100006E+01
*.150000E+01	*.853595E+00	.999867E+00	-.765852E+00	.253608E+00	.134879E-03	.100005E+01
*.175000E+01	*.906686E+00	.999898E+00	-.985888E+00	.179157E+00	.116137E-03	.100004E+01
*.200000E+01	*.943173E+00	.999925E+00	-.121712E+01	.120683E-00	.962084E-04	.100003E+01
*.225000E+01	*.967027E+00	.999946E+00	-.145590E+01	.772904E-01	.765431E-04	.100002E+01
.	.	.	.	.	.	.
.	.	.	.	.	.	.
.	.	.	.	.	.	.
*.775000E+01	*.100000E+01	.100000E+01	-.694273E+01	.163425E-12	.381561E-11	.100000E+01
*.800000E+01	*.100000E+01	.100000E+01	-.719273E+01	.284217E-13	.966338E-12	.100000E+01
*.825000E+01	*.100000E+01	.100000E+01	-.744273E+01	.142109E-13	.234479E-12	.100000E+01
*.850000E+01	*.100000E+01	.100000E+01	-.769273E+01	.710543E-13	.710543E-13	.100000E+01
*.875000E+01	*.100000E+01	.100000E+01	-.794273E+01	.710543E-14	.284217E-13	.100000E+01
*.900000E+01	*.100000E+01	.100000E+01	-.819273E+01	.213163E-13	.213163E-13	.100000E+01
*.925000E+01	*.100000E+01	.100000E+01	-.844273E+01	.142109E-13	.284217E-13	.100000E+01
*.950000E+01	*.100000E+01	.100000E+01	-.869273E+01	.284217E-13	.284217E-13	.100000E+01
*.975000E+01	*.100000E+01	.100000E+01	-.894273E+01	.284217E-13	.284217E-13	.100000E+01
*.100000E+02	*.100000E+01	.100000E+01	-.919273E+01	0.	0.	.100000E+01

CONVERGED SELF-SIMILAR SOLUTION REQUIRED 7 ITERATIONS.

INITIAL STATION PARAMETERS

MUE = .196497E-04    UE = 0.    TE = .289000E+03    PE = .188020E+05    QSD = -.144357E+02  
 XBE = .500000E+00    RE = .312933E-01    XAL = 0.

## APPENDIX D

\*\*\*\*\*DIMENSIONAL OUTPUT QUANTITIES ARE IN S.I. UNITS\*\*\*\*\*

FREE STREAM VALUES-DIMENSIONAL	P1 = .700000E+07	TT1 = .289000E+03	RT1 = .116505E+02	P1 = .310923E+02	T1 = .208860E+01	R1 = .716049E-02
U1 = .172695E+04	AA1 = .850714E+02	XMA = .203000E+02	REY = .152799E+08			
REFERENCE VALUES-DIMENSIONAL						
PREF = .213551E+05	TREF = .573823E+03	REF = .716049E-02	UREF = .172695E+04	VISREF = .306256E-04	PTR = .327790E+03	

• 0495 PROFIL E

## APPENDIX D

S	=	.49500E-01	RETHET=	.84412E+02	DPEDS =	-.38981E-02	CFW =	*.58682E-02	ZSHK =	-.30304E-02	YC =	*.76811E-03
XI	=	.19720E-04	RES =	*.47197E+05	DTEDS =	-.10389E+01	QSD =	*.20878E+04	RSHK =	*.71088E-02	UTAU =	0.
RMI	=	*.37893E-01	PE =	*.12175E+05	DUEDS =	*.25865E+01	HD =	*.26827E+03	ITRD =	0	TRFCF =	0.
Z	=	*.30003E-01	TE =	*.24272E+03	DLTAST =	*.29136E-03	NSTE =	*.30868E-02	TW/TY1 =	*.99962E+00	YMP =	0
BETA	=	*.25399E-03	RE =	*.24127E-01	THETA =	*.68531E-04	NSTW =	*.36741E-02	RFTRUE =	*.99760E+00	P20 =	*.10154E+01
XAL	=	*.38139E+00	UE =	*.69362E+03	FORM =	*.32911E+01	NUE =	*.10023E+03	ROUSE =	*.19874E+03	OMEGA =	*.15737E-02
RVWALD	=	0.	ME =	*.75634E+00	TAUD =	*.28615E+02	NUW =	*.89554E+02	DSMXO =	*.15627E+04	RVWAL =	0.
REDELT=	.277781E+03	MUE =	*.17551E-04	CFE =	*.49302E-02	SWANG =	*.72469E+02	VW =	0.			
NOITER=	*.30815E-04	2	ERROR =	*.30815E-04								

```
*****
* VARIABLE ENTROPY CALCULATIONS      *
* ITMAX= 5  NOTI= 1                  *
*****
```

## APPENDIX D

YOUR VARIABLE CASE ENTROPY IS CONVERGED TO YOUR SELECTED INPUT VALUE OF CONVE.

ORIGINAL PAGE IS  
OF POOR QUALITY

APPENDIX D

TEST CASE NO. 5

THE LISTING FOR TEST CASE NO. 5 INCLUDES THE FOLLOWING: (1) VARDIM DATA; (2) \$NAM1 AND \$NAM2 INPUT;  
(3) INITIAL STATION SOLUTION; (4) REFERENCE VALUES; (5) PROFILE AND WALL PRINTS AT S=.6385 M.

```
*VARDIM/VGBLP(JK=103,JL=1,JM= 99,JN= 2,JI=1,JH=101)
*VARDIM/TABLE(JJ=100,JH=101)
*VARDIM/VARENT(JL=1)
*VARDIM/TURBLNT(JI=1,JK=103)
*VARDIM/MESH(JK=103)
*VARDIM/SIMILAR(JK=103)
*VARDIM/SOLVE(JK=103)
```

```
$NAM1
IGEOM = .34500E+07 XEND = .60000E+02 IF = .12754E+01 DETA1 = .12058E-01
PT1 = .34500E+07 TT1 = .37700E+03 IGAS = .14582E-05 VIS1C1 = .VIS2C1 =
VIS2C2 = .14000E+01 R = .28696E+03 PR = .72000E+00 IENTR = 1
IBODY = 2 WAVF = 0. PHII = 0. J = - 1 W = - 0 IENTR = 1
SST = .30000E-03 SMXTR = .10000E+09 KODVIS = .50000E+01 XT4 = .10800E+00
KODAMP = .2 XT1 = .40000E+00 XT2 = .16800E-01 XT5 = .78000E+00
XT6 = .26000E+02 PRT = .95000E+00 KODPRT = 1 NUMB1 = 0 GLAR = I
PRTAR = 1
```

```
IEND1 = 100 PROINC = 0. PRINIC = 0. IPRO = 2 IPRNT = 99 NAUXPRO = 0
FT = .10000E+01 KODE = 0 KODWAL = .99500E+00 CONV = .10000E-03 NITMAX = 5
KODUNIT = 1 ITMAX = 3 CONVE = .10000E-01
```

THIS COMPLETES THE OUTPUT OF \$NAM1 WITH THE EXCEPTION OF PROVAL AND PRNTVAL. THESE VALUES ARE PRINTED JUST PRIOR TO THE INITIAL STATION PRINT.

NAME

## APPENDIX D

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OF POOR QUALITY

ORIGINAL PAGE IS  
OF POOR QUALITY

## APPENDIX D

ORIGINAL PAGE IS  
OF POOR QUALITY

APPENDIX D

*63459E-02	*63459E-02	*63703E-02	*63398E-02	*63429E-02	*63642E-02	*63398E-02	*63581E-02	*63581E-02
*63368E-02	*63612E-02	*53431E-02	*73457E-02	*63581E-02	*63551E-02	*63551E-02	*63551E-02	*63551E-02
*5964E-02	*17556E-02	*63520E-02	*63520E-02	*63551E-02	*63520E-02	*63520E-02	*63520E-02	*63520E-02
*63520E-02	*63246E-02	*63490E-02	*71110E-02	*55900E-02	*63490E-02	*12704E-01	*63490E-02	*29962E-02
0.								

THE FOLLOWING SPOINT VALUES DESIGNATE THE S-COORDINATE LOCATIONS WHERE THE SOLUTIONS ARE OBTAINED DURING THE S-MARCH. YOUR PRINT STATION MUST AGREE WITH ONE OR MORE OF THE SPOINT LOCATIONS; IE, YOU CAN PRINT ONLY AT SOLUTION STATIONS. IF THE CASE COMPLETES WITH A NORMAL STOP AND NO OUTPUT IS PRINTED, YOUR PRINT INPUT IS IN ERROR. THE ERROR CAN BE NOTED BY COMPARING PROVAL AND PRNTVAL WITH SPOINT.

SPOINT	PROVAL	PRNTVAL	SPOINT	PROVAL	PRNTVAL	SPOINT	PROVAL	PRNTVAL
*43431E-02	*86862E-02	*13029E-01	*23303E-01	*36585E-01	*50368E-01	*62798E-01	*72764E-01	*82604E-01
*10107E+00	*10966E+00	*11861E+00	*12723E+00	*13579E+00	*13604E+00	*13683E+00	*13843E+00	*14001E+00
*14318E+00	*14636E+00	*15272E+00	*15906E+00	*16538E+00	*17175E+00	*17808E+00	*18444E+00	*19079E+00
*20350E+00	*20984E+00	*21619E+00	*22256E+00	*22891E+00	*23526E+00	*24161E+00	*24799E+00	*25434E+00
*26706E+00	*27342E+00	*27978E+00	*28613E+00	*29248E+00	*29885E+00	*30521E+00	*31157E+00	*31793E+00
*33062E+00	*33697E+00	*34333E+00	*34971E+00	*35604E+00	*36240E+00	*36876E+00	*37511E+00	*38164E+00
*39419E+00	*40053E+00	*40690E+00	*41324E+00	*41958E+00	*42595E+00	*43231E+00	*43865E+00	*44501E+00
*45771E+00	*46407E+00	*47042E+00	*47577E+00	*48311E+00	*48947E+00	*49582E+00	*50218E+00	*50853E+00
*51948E+00	*52124E+00	*52759E+00	*53394E+00	*54029E+00	*54665E+00	*55300E+00	*55935E+00	*51489E+00
*57840E+00	*58473E+00	*59108E+00	*59743E+00	*60454E+00	*61013E+00	*61648E+00	*62918E+00	*57205E+00
0.								

PRINT STATIONS DESIGNATED IN \$NAME1 INPUT AND GENERATED IN SETUP

PROVAL	PRNTVAL								
*13604E+00	*63853E+00	*13604E+00	*13604E+00	*13604E+00	*13604E+00	*13683E+00	*13843E+00	*14001E+00	*14161E+00
*43266E-02	*13029E-01	*23303E-01	*36585E-01	*50368E-01	*62798E-01	*72764E-01	*82604E-01	*92552E-01	*10107E+00
*10986E-00	*11861E+00	*12723E+00	*13579E+00	*13604E+00	*13683E+00	*13843E+00	*13843E+00	*14001E+00	*14161E+00
*14636E+00	*15272E+00	*15906E+00	*16538E+00	*17175E+00	*17808E+00	*18444E+00	*18444E+00	*19079E+00	*19713E+00
*20984E+00	*21619E+00	*22256E+00	*22891E+00	*23526E+00	*24161E+00	*24799E+00	*24799E+00	*25434E+00	*26065E+00
*27342E+00	*27978E+00	*28613E+00	*29248E+00	*29885E+00	*30521E+00	*31157E+00	*31157E+00	*31793E+00	*32427E+00
*33697E+00	*34333E+00	*34971E+00	*35604E+00	*36240E+00	*36876E+00	*37511E+00	*37511E+00	*38146E+00	*38846E+00
*39419E+00	*40053E+00	*40690E+00	*41324E+00	*41958E+00	*42595E+00	*43231E+00	*43231E+00	*44501E+00	*45137E+00
*45771E+00	*46407E+00	*47042E+00	*47577E+00	*48311E+00	*48947E+00	*49582E+00	*49582E+00	*50218E+00	*51489E+00
*51948E+00	*52124E+00	*52759E+00	*53394E+00	*54029E+00	*54665E+00	*55300E+00	*55935E+00	*56570E+00	*57205E+00
*57840E+00	*58473E+00	*59108E+00	*59743E+00	*60454E+00	*61013E+00	*61648E+00	*62918E+00	*63553E+00	*63853E+00

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OF POOR QUALITY

APPENDIX D

SIMILAR SOLUTION REQUIRED TO INITIATE MARCHING PROCEDURE

PROFILE VALUES					
ETA	U/UE	T/TE	V	FZ	XL
0.	0.	.100013E+01	0.	.468918E+00	.999963E+00
*450271E-09	*211140E-09	*100011E+01	*475351E-19	*468918E+00	*269108E+05
*102455E-08	*480428E-09	*100011E+01	-*246111E-18	*468918E+00	*999963E+00
*175698E-08	*823879E-09	*100011E+01	-*723768E-18	*468918E+00	*999963E+00
*269112E-08	*126191E-08	*100011E+01	-*169798E-17	*468918E+00	*170540E-04
*388253E-08	*182059E-08	*100011E+01	-*353424E-17	*468918E+00	*200572E-04
*540204E-08	*253312E-08	*100011E+01	-*684200E-17	*468918E+00	*235893E-04
*734004E-08	*344188E-08	*100011E+01	-*126318E-16	*468918E+00	*308260E-04
*981176E-08	*460091E-08	*100011E+01	-*225715E-16	*468918E+00	*338376E-04
*129642E-07	*607914E-08	*100011E+01	-*394055E-16	*468918E+00	*353746E-04
.	.	.	.	.	*356607E-04
.	.	.	.	.	.
0.	0.	0.	0.	0.	0.
*671945E+01	*100038E+01	*100000E-01	-*550546E+01	*810735E-04	*128846E-07
*856998E+01	*99929E+00	*100000E+01	-*735627E+01	-*250747E-04	*100000E+01
*109302E+02	*100027E+01	*100000E+01	-*971668E+01	*931878E-05	*100000E+01
*139403E+02	*99979E+00	*100000E+01	-*127272E+02	-*383535E-05	*100000E+01
*177795E+02	*100025E+01	*100000E+01	-*165668E+02	*167551E-05	*100000E+01
*226760E+02	*99993E+00	*100000E+01	-*214639E+02	-*758719E-06	*100000E+01
*289209E+02	*100024E+01	*100000E+01	-*277096E+02	*351242E-06	*100000E+01
*368857E+02	*99999E+00	*100000E+01	-*356753E+02	-*164868E-06	*100000E+01
*470441E+02	*100023E+01	*100000E+01	-*458348E+02	*780711E-07	*834572E-11
*600000E+02	*100000E+01	*100000E+01	-*587923E+02	0.	*100000E+01

CONVERGED SELF-SIMILAR SOLUTION REQUIRED 15 ITERATIONS.

INITIAL STATION PARAMETERS

MUE = .219000E-04 UE = .136191E+02 TE = .376908E+03 PE = .344704E+07 QSD = 0.  
 XAL = .489974E-03 XBE = 0. RE = .318707E+02

\*\*\*DIMENSIONAL OUTPUT QUANTITIES ARE IN S.I. UNITS\*\*\*

```

FREE STREAM VALUES-DIMENSIONAL
PT1 = .345000E+07 TT1 =
U1 = .46260E+01 AA1 =
REFERENCE VALUES-DIMENSIONAL
PREF = .702188E+03 TREF =

```

.6385 PROFILE

ETA	Y/YE	U/UE	T/T/E	TT/TTE	CRCDDO	PT/PTR	M/M/E	YPLUS	UPLUS	UDEF	VISEFF
0.	0.	0.	• 545E+01	• 911E+00	• 397E-13	• 191E-02	0.	0.	0.	• 100E+01	• 100E+01
• 450E-09	• 731E-10	• 342E-08	• 545E+01	• 911E+00	• 795E-13	• 191E-02	• 146E-08	• 773E-07	• 690E-07	• 202E+02	• 100E+01
• 102E-08	• 166E-09	• 777E-08	• 545E+01	• 911E+00	• 199E-12	• 191E-02	• 333E-08	• 176E-06	• 157E-06	• 202E+02	• 100E+01
• 176E-08	• 285E-09	• 133E-07	• 545E+01	• 911E+00	• 238E-12	• 191E-02	• 571E-08	• 302E-06	• 269E-06	• 202E+02	• 100E+01
• 269E-08	• 437E-09	• 204E-07	• 545E+01	• 911E+00	• 318E-12	• 191E-02	• 875E-08	• 462E-06	• 412E-06	• 202E+02	• 100E+01
• 386E-08	• 630E-09	• 295E-07	• 545E+01	• 911E+00	• 358E-12	• 191E-02	• 126E-07	• 667E-06	• 595E-06	• 202E+02	• 100E+01
• 540E-08	• 877E-09	• 410E-07	• 545E+01	• 911E+00	• 397E-12	• 191E-02	• 176E-07	• 928E-06	• 828E-06	• 202E+02	• 100E+01
• 734E-08	• 119E-08	• 557E-07	• 545E+01	• 911E+00	• 517E-12	• 191E-02	• 239E-07	• 172E-05	• 112E-05	• 202E+02	• 100E+01
• 981E-08	• 159E-08	• 744E-07	• 545E+01	• 911E+00	• 715E-12	• 191E-02	• 319E-07	• 169E-05	• 150E-05	• 202E+02	• 100E+01
• 130E-07	• 211E-08	• 984E-07	• 545E+01	• 911E+00	• 111E-11	• 191E-02	• 421E-07	• 223E-05	• 199E-05	• 202E+02	• 100E+01
• 672E+01	• 451E+00	• 934E+00	• 163E+01	• 998E+00	• 981E+00	• 337E-01	• 732E+00	• 395E+04	• 189E+02	• 133E+01	• 316E+03
• 857E+01	• 531E+00	• 952E+00	• 147E+01	• 100E+01	• 995E+00	• 387E-01	• 786E+00	• 577E+04	• 192E+02	• 971E+00	• 390E+03
• 109E+02	• 622E+00	• 967E+00	• 133E+01	• 100E+01	• 101E+01	• 441E-01	• 840E+00	• 835E+04	• 195E+02	• 664E+00	• 479E+03
• 139E+02	• 726E+00	• 979E+00	• 121E+01	• 100E+01	• 101E+01	• 494E-01	• 890E+00	• 1119E+05	• 198E+02	• 416E+00	• 579E+03
• 171E+02	• 846E+00	• 989E+00	• 112E+01	• 100E+01	• 100E+01	• 543E-01	• 934E+00	• 164E+05	• 200E+02	• 231E+00	• 681E+03
• 227E+02	• 987E+00	• 995E+00	• 106E+01	• 100E+01	• 101E+01	• 582E-01	• 967E+00	• 217E+05	• 201E+02	• 106E+00	• 768E+03
• 289E+02	• 116E+01	• 998E+00	• 102E+01	• 100E+01	• 101E+01	• 606E-01	• 988E+00	• 275E+05	• 202E+02	• 364E-01	• 828E+03
• 369E+02	• 136E+01	• 100E+01	• 101E+01	• 100E+01	• 100E+01	• 618E-01	• 997E+00	• 336E+05	• 202E+02	• 794E-02	• 856E+03

## APPENDIX D

*470E+02	*161E+01	*100E+01	*100E+01	*100E+01	*100E+01	*621E-01	*100E+01	*402E+05	*202E+02	*902E-03	*865E+03
*600E+02	*192E+01	*100E+01	*100E+01	*100E+01	*100E+01	*621E-01	*100E+01	*480E+05	*202E+02	*934E-09	*866E+03
S	-	*63853E+00	RETHET	*18342E+05	DPEDS	*-16386E+02	CFW	*49052E-02	ZSHK	-0.	YE
XI	-	*87087E+03	RES	*43890E+08	DTEDS	*-27090E+01	QSD	*0.	RSHK	-0.	UTAU
RMI	-	*52858E-01	PE	*65845E+04	DUEDS	*16007E-01	HD	*0.	ITRO	-0.	TRFC T
Z	-	*61534E+00	TE	*63009E+02	DLTAST	*29232E-02	NSTE	*0.	TW/TI1	*91061E+00	YMP
BETA	-	*16473E+00	RE	*36417E+00	THETA	*26684E-03	NSTH	*0.	RFTRUE	*89267E+00	P20
XAL	-	*99666E+01	UE	*79418E+03	FORM	*10955E+02	NUE	*0.	ROUSE	*15444E+05	OMEGA
RVWALD	0.	*0.	ME	*49917E+01	TAUD	*10339E+03	NUW	*0.	DSMXO	*-14305E+03	RVWAL
REDELT	-	*20093E+06	MUE	*42076E-05	CFE	*90030E-03	SWANG	*0.	VW	*0.	
NOITER	-	4	ERROR	*62741E-04							

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